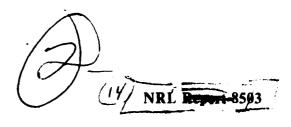
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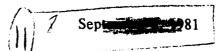
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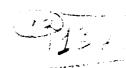
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# NRL 5-m<sup>3</sup> CHAMBER PRESSURIZATION EXPERIMENT: PRESSURANT CONCENTRATION HISTORIES

## INTRODUCTION

Carhart and Fielding [1] proposed suppression of unwanted, free-burning fires in pressurizable spaces by the injection of nitrogen gas. Preliminary tests have demonstrated their concept [2-5]. Liquid-fuel (class B) fires in 0.27- and 5-m³ chambers at one atmosphere are quickly controlled by addition of nitrogen; flames extinguish at oxygen concentrations of 12 to 14% by volume, yet partial pressure of oxygen is essentially unchanged. Thus, spaces remain habitable provided extinguishment is timely and excessive accumulation of toxic combustion products is avoided. Additional advantages of this suppression technique as compared to others include the inertness of nitrogen gas to machines, electronics, electrical wiring, and air-purification devices. Further, a space can easily be returned to normal condition following a suppression action.

This promising method, however, poses questions and problems that require exploration, some perhaps not yet defined. Since fire suppression by nitrogen pressurization may be a last-resort method used only after other methods have failed, well-developed-fire encounters are likely. Rapid extinguishment becomes imperative—seconds may count. Thus, knowledge of the mixing rates of pressurant and resident gases is essential, particularly at fire seats. Such conditions as extreme geometries, cluttered spaces, nozzle design and location, injection times, or combinations of these affect gas-mixing rates. As a result, it is conceivable that pockets of poorly mixed gas may in one case increase fire intensity or in the other reduce the quality of the atmosphere to support life.

To explore pressurant gas concentration profiles during injection and to implement scale modeling techniques, different sizes of enclosures with similar geometry are used. In this way, identity of controlling parameters allows inference of concentration profiles in other similar spaces and provides additional insight as to controlling mechanisms.

The Naval Research Laboratory (NRL) 5-m<sup>3</sup> chamber was one enclosure used in these studies. This set of experiments was with minimal clutter and no fire. Pressurant gas injection times varied from 8 to 30 s, depending upon nozzle size and configuration. Because of these short injection times, large experimental distances (approximately 8 m), the relatively slow response times of chemical detectors, and the need for information at several points in space simultaneously, we used fine-wire thermocouples to measure local temperature histories. By this indirect method, we exploited temperature differences between the pressurant gas stream and resident gas to infer local pressurant concentration histories [6].

In this report, we describe the analysis and the evaluation of previously reported temperature and pressure measurements.

## **DESCRIPTION OF EXPERIMENT**

We have described the experiment previously [7-11]. Briefly, we blew pressurant gas from a pressure tank at 6.5 atmospheres (659 kPa) via an actuated control valve, a 3-in. (7.62-cm) pipe, and one, two, or three nozzles into a 5-m<sup>3</sup> chamber, initially containing one atmosphere of ambient air. This is schematically shown in Fig. 1. We increased chamber pressures from one to two atmospheres (101.3)

Manuscript submitted June 9, 1981.

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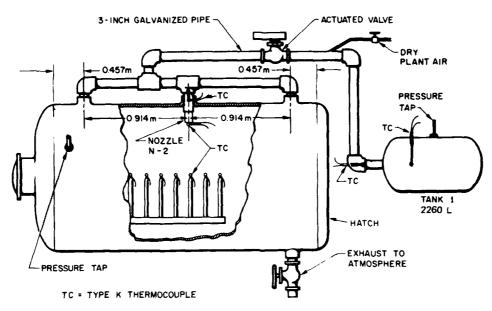


Fig. 1 - Schematic of apparatus

kPa to 202.6 kPa) while monitoring interior temperatures and pressures. To collect these data, we used two Doric Data Loggers, each coupled to a magnetic-tape device. Each system scanned ten channels with a scan time of about 0.5 s so that each thermocouple and pressure transducer output was recorded at 0.5-s intervals. The two systems produced data on two magnetic tapes with channels 60 to 69 on one and 70 to 79 on the other. We assured simultaneous operation of the two systems by use of a common control circuit.

We conducted gas-mixing experiments with minimal clutter. The parameters are summarized in Table 1. There are 12 sets of experiments: all sets but the first have three experiments each; the first has nine. To generate the 12 sets, we adjusted three variables: nozzle array, nozzle diameter, and thermocouple array. The three nozzle arrays included No. I, the center nozzle only; No. II, the center plus one end nozzle; and No. III, all three nozzles (see Fig. 1). We used two nozzle diameters (2.54 cm and 1.52 cm) and two thermocouple arrays. In thermocouple array I, we placed 13 thermocouples along the chamber axis in the airlock end of the chamber (see Fig. 1 and subtable in Table 2A). In array II, we shifted each thermocouple in array I by 0.457 m along radial lines, normal to the chamber axis and making 45° angles with the horizontal, when viewed from the hatch end of the chamber (see Fig. 2). Table 1 gives set numbers, designated run numbers, and NRL Memorandum Report numbers.

Our format for collecting data for each experiment was the same. With the pressure tank at 6.5 atmospheres and ambient temperature and the chamber at 1 atmosphere and ambient temperature, we collected data for 30 s, then opened the control valve and blew pressurant gas through the nozzles into the chamber until its pressure increased to 2 atmospheres. We then closed the control valve and continued collecting data for a total time of 4 min. We edited the two data tapes and copied the edited data onto a single tape with channels 60-69 preceeding 70-79 for each experimental run.

Table 1 - Summary of 41 Gas-Mixing Experiments with Minimal Clutter

Set Number	Nozzle Array	Nozzle Diameter (cm)	Thermo- Couple Array	Number of Runs	Run Numbers	NRL Memo. Rpt. No.	Ref. No.
1	l	2.54	I	9	23-31	3740	7
2	II	2.54	I	3	32-34	3776	8
3	III	2.54	I	3	35-37*	3776	8
4	III	1.52	I	3	39-41	3791	9
5	II	1.52	I	3	42-44	3791	9
6	I	1.52	I	3	45-47	3791	9
7	I	1.52	II II	3	48-50	3792	10
8	II	1.52	11	3	51-53	3792	10
9	111	1.52	II	3	54-56*	3792	10
10	III	2.54	II	3	58-60	3793	11
11	II	2.54	II	3	61-63	3793	11
12	I	2.54	II	3	64-66	3793	11

<sup>\*</sup>Runs 38 and 57 were deleted.

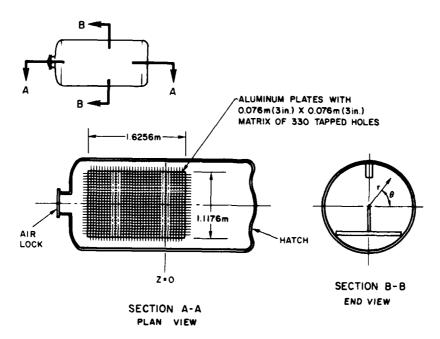


Fig. 2 — Plan and end views of Tank 2 showing cylindrical coordinates and matrix of 330 tapped holes

#### DESCRIPTION OF ANALYSIS

The pressurant gas may be air or nitrogen, but it is assumed to have the same specific heat ratio  $\gamma$ , one that remains constant over the temperature range of interest. The chamber volume is V and initial absolute temperature and pressure are  $T_0$  and  $P_0$ , respectively. The subscript zero denotes initial condition. The total chamber molar contents N and pressure P are considered to be known functions of time t, as is the total temperature  $T_s$  of the influent pressurant. The pressurant flow rate dN/dt is suddenly increased from zero at time t=0 and suddenly dropped to zero at time  $t=t_c$ , where  $t_c$  is time of valve closure. During the filling interval  $0 \le t \le t_c$ , dN/dt may be constant or may vary gradually. The chamber walls and any interior structure are considered isothermal at temperature  $T_0$ . At a set of t interior locations (index i), temperature histories  $T_c(t)$  are measured. The objective is to infer the pressurant mole fraction history  $X_c(t)$  corresponding to each  $T_c(t)$ .

This problem is not strictly determinant for two reasons. First, good experimental evidence indicates that the chamber contents are far from adiabatic. Gas-to-wall heat transfer from gas arriving at each interior point of interest undoubtedly varies from point to point. However, quantification of such spatial variation of heat-transfer effects on measured temperatures is a complex problem comparable to that of determining transient pressurant distribution, the solution of which was our original purpose. Thus, we make the modeling assumption that the molar gas-to-wall heat-transfer coefficient is independent of interior position; the validity of this assumption depends on the extent to which spatial variability averages out along fluid particle trajectories.

The second reason for indeterminacy is that after the pressurant enters the chamber its temperature  $T_p$  depends on age. "Old" pressurant is compressed in the chamber through a higher pressure ratio than "new" pressurant which is added later, hence old pressurant tends toward a higher temperature relative to its value at entrance. Here we make a second modeling assumption, that the pressurant age distribution is the same at every interior point.

Except for small volumes, at most a few diameters down-jet from each inlet nozzle, kinetic energy of the fluid is thermodynamically negligible and no distinction need be made between total and static temperatures within the chamber. Therefore, from the ideal gas law,

$$V = \int_{R} RTP^{-1} dN = RP^{-1} \int_{R} T dN = NR\overline{T}P^{-1}.$$
 (1)

where tc denotes that the integration is over the total chamber contents, R is the universal gas constant, and T is the molar mean temperature. The chamber content total internal energy U may be written

$$U = N\overline{u} = \int_{\kappa} u \ dN = N[u_0 + c_{\nu}(\overline{T} - T_0)] = N[u_0 + \frac{R}{\gamma - 1}(\overline{T} - T_0)], \tag{2}$$

where again u denotes that the integration is over the total chamber contents; u and  $\overline{u}$ , respectively, are local and mean specific internal energy;  $c_i$  is molar constant volume specific heat; and  $u_0$  corresponds to  $T_0$ . This thermodynamic description, which is not in question, and the two modeling assumptions render our problem fully determinate.

To describe gas-to-wall heat transfer, we characterize the molar heat-transfer coefficient by a dimensionless parameter  $\beta$ , such that the local heat flow per mole, from gas at local temperature T to the chamber wall at temperature  $T_0$ , is  $(\beta R/\theta) T - (T_0)$ . Here  $\theta$  is a characteristic time. Since turbulent convective heat transfer is nearly proportional to flow velocity, which in turn is roughly proportional to  $d\ln N/dt$  during filling, we take  $\theta = (d\ln N/dt)^{-1}$  for the filling interval  $0 \le t \le t_c$ . During this interval  $\beta$  should be nearly constant. After filling we take  $\theta$  as constant at its value just prior to the time  $t = t_c$ . For post-filling times,  $t > t_c$ ,  $\beta$  should decline to a much lower free-convection driven value as filling turbulence decays. The heat-removal rate Q from total chamber contents may be written

$$\dot{Q} = \beta R \theta^{-1} \int_{R} (T - T_0) dV = \beta N R \theta^{-1} (\overline{T} - T_0). \tag{3}$$

The temperature linearity exhibited by Eqs. (1) to (3) signifies that the temperature  $T_i$  at a point can be calculated as if resident air and pressurant were perfectly stratified and suddenly mixed adiabatically at constant pressure to pressurant fraction  $X_i$ . Further, our assumption of uniform pressurant age distribution means that the pressurant temperature for this calculation is the average temperature  $\overline{T}_p$  for all the pressurant in the chamber. Thus, if the mean resident air temperature  $\overline{T}_a$  is known in addition to the molar mean temperature  $\overline{T}$  of chamber contents from Eq. (1), an internal energy summation determines  $\overline{T}_p$ , i. e.,

$$N\bar{T} = (N - N_0)\bar{T}_p + N_0\bar{T}_q, \tag{4}$$

then

$$T_i = X_i \overline{T}_p + (1 - X_i) \overline{T}_a. \tag{5}$$

We have, finally, the pressurant mole fraction at any point,

$$X_{i} = \frac{\overline{T}_{a} - T_{i}}{\overline{T}_{a} - \overline{T}_{p}} = \left(1 - \frac{N_{0}}{N}\right) \left(\frac{\overline{T}_{a} - \overline{T}_{i}}{\overline{T}_{a} - \overline{T}}\right) = \overline{X} \left(\frac{\overline{T}_{a} - \overline{T}_{i}}{\overline{T}_{a} - \overline{T}}\right). \tag{6}$$

where  $\bar{X}$  is the molar average pressurant fraction for the entire chamber contents.

To derive  $\overline{T}_a$ , the first step is to determine  $\beta$  from experimental data. A control volume energy balance gives

$$h_s dN/dt = (u_s + RT_s) dN/dt = dU/dt + \dot{Q}, \tag{7}$$

where  $h_s$  is the pressurant specific enthalpy corresponding to its supply temperature  $T_s$ . Combined with Eqs. (1) to (3) and the previously assigned value for  $\theta$ , Eq. (7) yields for the filling interval

$$\beta = \frac{\gamma T_s - \overline{T} - d\overline{T}/d\ln N}{(\gamma - 1)(\overline{T} - T_0)} \qquad (0 \leqslant t \leqslant t_c)$$
(8)

and for the post-filling interval

$$\beta = -\frac{d\ln(T - T_0)/dt}{(\gamma - 1)/\theta_c} \qquad (t > t_c),$$
(9)

where subscript c denotes that  $\theta$  is evaluated just prior to time  $t = t_0$ 

And finally, with the resident gas and pressurant modeled as perfectly stratified, an energy balance on the resident gas is written as a system,

$$\frac{d(N_0\bar{u}_a)}{dt} + \frac{d(N_0R\bar{T}_a/P)}{dt}P + \frac{\beta RN_0}{\theta}(\bar{T}_a - T_0) = 0.$$
 (10)

By combining Eqs. (8) and (10), noting that  $\theta d \ln N/dt = 1$  and that  $d \ln P = d \ln N + d \ln T$ , one obtains

$$d\overline{T}_a = \frac{\gamma - 1}{\gamma} \overline{T}_a(d\ln P) - \mu [(T_s - \overline{T}/\gamma) d\ln P - \overline{T}_s d\ln \overline{T}], \tag{11}$$

where  $\mu = (\overline{T}_a - T_0)/(\overline{T} - T_0)$ .

An examination of the initial behavior of Eq. (11), i.e., with  $\overline{T}_a = T_0$ ,  $\overline{T} = T_0$ ,  $T_s = T_{s_0}$ , and  $P = P_0$  at the time the control valve is opened (t = 0), shows that

$$\mu_0 = \frac{(\gamma - 1)T_0}{\gamma (T_0 - T_{s_0})(d\ln \bar{T}/d\ln P)_0 + \gamma T_{s_0} - T_0} \approx 1.$$
 (12)

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Then, with Eq. (12) as a starting value of  $\mu$ , Eq. (11) is readily integrated numerically on the basis of measured  $\bar{T}$  and P data. This procedure, valid for both the filling and post-filling processes, gives values of  $\bar{T}_a$ . Pressurant mole-fraction concentrations  $X_i$  at any local point of interest are obtained from Eq. (6). Comparison of  $X_i$  and  $\bar{X}$  values at any time t indicates pressurant excess or deficiency.

From scale modeling considerations previously reported [12], an appropriate dimensionless time  $\tau$  was described for both pressurization ( $t < t_c$ ) and post-pressurization times ( $t > t_c$ ). The definition was

$$\tau = \bar{X}/\bar{X}. \quad (t < t_c) \tag{13a}$$

and

$$\tau = 1 - \frac{t - t_c}{\theta_c}$$
  $(t > t_c),$  (13b)

where

$$\theta_{i} = -\left[\frac{d\ln(1-\tilde{X})}{dt}\right]_{t \to t_{i} > t}.$$
(13c)

In addition, a working hypothesis for scale modeling was stated. Irrespective of pressure level or pressurization rate, for a given enclosure geometry and nozzle configuration, at homologous model and prototype points, dimensionless pressurant deviation

$$\xi = (X - \bar{X})/\bar{X}_c \tag{14}$$

is a unique function of  $\tau$ .

## **REDUCED DATA**

Data of each experimental run were collected into tables in which temperatures and pressures were averaged at 1-s intervals, Tables 2A-43A (the A tables). The time t=0 was arbitrarily taken at the instant the control valve began to open. Total time intervals over which each run was considered started at t=-5 s and continued long enough to include desired information. The captions give run number and nozzle configuration. In the upper-right-hand corner, a subtable gives the I locations of the 13 thermocouples and their cylindrical coordinates  $(r, \theta, z)$ . As shown in Fig. 2, r=0 is along the chamber axis, and the plane z=0 is normal to the axis and passes through the center nozzle with the positive direction toward the air-lock end. The first four columns of these tables give, respectively, time t, absolute pressure of the pressure tank (Tank 1 in Fig. 1) in atmospheres, total temperature  $T_s$  of inflowing pressurant in K, and absolute pressure P of the chamber in atmospheres. The next 13 columns, i.e., columns 5 through 17, give absolute temperatures in K for the 13 thermocouple locations. Notice that (J), when it follows an I location, indicates an inlet-jet centerline.

In the facing B tables (Tables 2B through 43B), we present the inferred values of pressurant mole fraction concentration  $X_I$ ; columns 8 through 20 give values for I locations 1 through 13, respectively. These I locations correspond to the thermocouple locations in the A tables. The first seven columns give the time t, the molar mean temperature  $\overline{T}$  in °C, the mean resident air temperature  $\overline{T}_p$  in °C, the dimensionless molar heat-transfer coefficient  $\beta$ , the ratio  $\beta/\theta$ , where  $\theta$  is the defined characteristic time, and the mean pressurant mole fraction  $\overline{X}$ . Notice that Tables 2A and 2B give data for a single experimental run and are on facing pages, as are all the A and B Tables.

Next, consider the sets of replicate runs as given in Table 1. Set 1 has nine such runs, while the remaining eleven sets have three each. Our purpose is to organize our data by set into a convenient form for comparison with other data according to our working hypothesis and to examine standard deviations within our data sets.

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For example, Set 1, Table C gives mean values for the nine replicate runs 23 through 31 presented in Tables 2A and 2B through 10A and 10B. The headings for this table are the same as those for the B tables. In addition, these mean values are at dimensionless times  $\tau$  taken arbitrarily at 0.05 intervals over the range 0.00 to 2.45, as interpolated from  $\tau$  values calculated by Eq. (13) and appropriate B tables. Set 1, Table D gives standard deviations of the mean local pressurant fractions, and Set 1. Table E gives the dimensionless pressurant deviations  $\xi$  for values of dimensionless time  $\tau$ .

Similar Tables C, D, and E follow for each of the remaining 11 sets. The zeros in these tables at higher  $\tau$  values are due to limiting the number of data scans processed by the computer. Thus, for the slower pressurant dumps, the calculation is turned off before  $\tau = 2.45$ .

## DISCUSSION

We present results from 12 sets of replicated sequences that include 41 experimental runs with minimal clutter in the NRL 5-m<sup>3</sup> chamber. Pressurant concentration deviations (from perfectly mixed mean values) for a range of dimensionless times are inferred from measured local temperature histories. We call this the *thermal method* and describe its thermodynamic analysis.

Standard deviations of local pressurant fractions show that the means of these values are statistically meaningful at dimensionless times  $\tau$  above 0.5 or 0.6, but below these values they are meaningless. We explain this condition as follows. First, the control valve is not instantaneous, but opens in about 2 s. Second, stagnant chamber gases require sufficient momentum transport to drive the turbulent, quasi-steady flow that the analysis assumes, and this process needs an interval of time to develop after the valve opens.

We see evidence of this flow regime through its effect on values of the dimensionless volumetric heat-transfer coefficient  $\beta$  in the C tables. As dimensionless time passes,  $\beta$  values tend to constancy. After the control valve is closed and momentum forces are overcome by viscous ones, turbulence decays. As a result,  $\beta$  values decrease to much lower values and data scatter increases.

Improved flow measurement, pressure-tank pressure regulation, increased number of local measurement points, and increased rates of data collection would improve data precision. Nevertheless, the E tables show that dimensionless pressurant deviations  $\xi$  sensitively indicate gas-mixing rates. Positive values of  $\xi$  signal a pressurant excess, negative values signal a deficiency, and values near zero signal thorough mixing. The data show thorough mixing by dimensionless time  $\tau=1.5$ .

Except for strong positive peaks under the inlet nozzles, data taken at stations along the chamber center line show a pressurant defect which declines as the end of the chamber is reached. There is no significant difference in this pattern for one-, two-, or three-nozzle cases. However, when observation stations are located along the vessel radii, 0.6 of the distance to the wall and in a plane rotated  $45^{\circ}$  to the horizontal, this is not true. At these locations, the single center nozzle configuration shows a pressurant deficiency in the center section that changes to an excess toward the chamber end. The two- and three-nozzle configurations show an opposite effect. Although not large, these concentration differences are statistically significant. By dimensionless time  $\tau=1.5$ , the data show thorough mixing. No significant effect of nozzle diameter, and hence filling rate (varied by a factor of 3.5), is seen. To exercise our model more severely, injection times can be extended and spaces made more cluttered.

Table 2A — Scaling Run 23, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]



Table 2B — Inferred Pressurant Distribution, Scaling Run 23, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

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at L		٠			-		~	,		•	m	60	0	٧.			۰	•		•	۰	•		~	•	m	~	٠	۰	_	00	•	•	'n	m	<u>~</u>	m	•	•
X (X)	•	9	0 3 S		- 1	7	-	-	20	5 6	23	2	316	E	32		E.	330		7	4.2	₩.	-	•	Ť	*	•	Ŧ	*	4	38	*	÷	7	÷	4 6 3	~	Ŧ	-
Pressurant Fractions (X) at Locations	~		8 8		7 6 7	90	7 -	183	166	182	233	278	310	317	326		340	330		• 0	420	<b>6 E </b>	430	7 6 2	•	₩ ₩	499	463	430	<b>2 2 \$</b>	490	9 9	* *	4 3 3	311	~	7.7	311	3 3 3
<b>Trant</b>	4	0	144		- "	8 9	9.6	8 2	99	82	5	8 ~	310	33	50		417	408		4	50	39	3.4	7	÷	P P	20	5.9	90	21	90	0 9	9 +	33	24	403	£ &	36	<b>5</b>
Press		•			-	•	•	-	-	-	~	~		~	•		•	•		•	*	•	*	•	•	*.	•	*	*	•	•	•	•	•	•	•	•	•	•
	363		293				890	825	8.78	912	874	168	914	926	.019		937	039		8 2 8	734	6.95	672	642	630	621	393	364	348	523	4 90	562	332	542	311		E ~ #	311	332
		0	633		13 3		5.5	29	•	20	:	50	336	=	38		619	_		~	5	*	*	22	33	22	9.9	5 9	9	23	9.0	0.9	9	33	57	4 8 3	7.3	3.6	e.
	7				•	Ť	~	m	•	'n	₹.	ñ		•	•		•	•		•	•				•	٠		•	•	•	٠		•	•	•				٠
		9	5		800	233	019	0 6 2	1.24	3.02	176	278	310	317	328		340	4 9 8		=	420	439	405	462	=	433	402	463	4 30	12.	490	9 6 0	4.46	4 33	4 5 7	20	¥ 2 3	136	4 3 9
		•	•		7	i	٠	·			·	·						•			·								·		•								
	Þ₹	9	0.24		106	172	. 222	267	303	338	366	392	414	434	433		469	***		482	4.85	485	.485	20 V	483	4.63	4.85	485	4.63	413	483		. 485	\$ <b>9</b> \$	4.03	n ₩	4 8 3		
		•			50	20	96	24	~	17	33	=	63	<u>.</u>	96		66	72		ij	20	9	30	7.	9	9.4	80	33	:	63	£ <b>+</b>	ê	10	8.9	2.2	•	:	•	~
	9/8		7 2734		3.71			9.2	6.0	. 8	•	9	5869	2.2	3490		485	5172		90	1930	90	7	03	11	0.3	80	80	0.00	80	0	000.0	60	0	•	00000	•	000	-
	_						80	~	~	٠	•	m	-	<b></b>	و.		•	0		~	•	<b>æ</b>	۸.		•	٠	æ	•	•	n	•		~.	•	•		0	•	0
	•	•	296		9	<b>9</b> 2				16	-	16	15 4	•	•		16	20		~	~	~	**	-	•	~	m	~	•	~	-	•	Les)	•		٥	~	•	•
	, Ç	186			19.8	17.1	2. 7	16.3	•	19.2	29.7	9.9	30.1		20.5	JR.E	30.7	30.		30.7	10.2	0.0	2 62	9 62	29.3	2 62	29.0	28.9		28.7	30.6	9 82	28.3	* * *	20.3		2 8 2	2 5	•
	_													•	'n	1081		<b></b>	ED							•	•	•	•	•	•	•	•	~	n	 P	m	_	•
	r.6	46 0P	2	_			37.1		:	Ţ	7	7	4.5	7	Ţ	LVE CLOSURE	Ç		2013	+ 17	5	41.7	40.9	40.7	•	<b>6</b> P	39	33	33	=	2	m	=	37	37	2.2	~	£	~
	٦	FVAL	26.5	11.14	29.9	32.6	35.0	36.4	17.1	4. 4	37.8	9. 7	17.9	37.7	37.6	EVAL	9. 42	17.3	11.1	37.2	36.3	96.0	13.4	35.3	34.8	34.7	34.4	34.1	34.1	33.0	33.6	33.6	11.3	33.2	33.0	0.66	32.9	12.9	35.6
	~3	COMMENCE VALVE		VALVE FI		•	•	•	•	•	•	•	•	•	•	THENC		•	VE FI	15.0 37.2	•	•	•	•	•	•	22.	_	_	25.0	•	•	•	•		•	•	27.0	•
	- 3	•		5	••	,,	•	41	_	,~	_	_	ž	Ξ	=		_	Ĭ	Ĭ	-1	Ξ	=	Ξ	Ξ	ž	~	ř	~	ř	~	ž	ñ	~	ž	ř	ñ	Ä	ä	Ř

Table 3A — Scaling Run 24, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

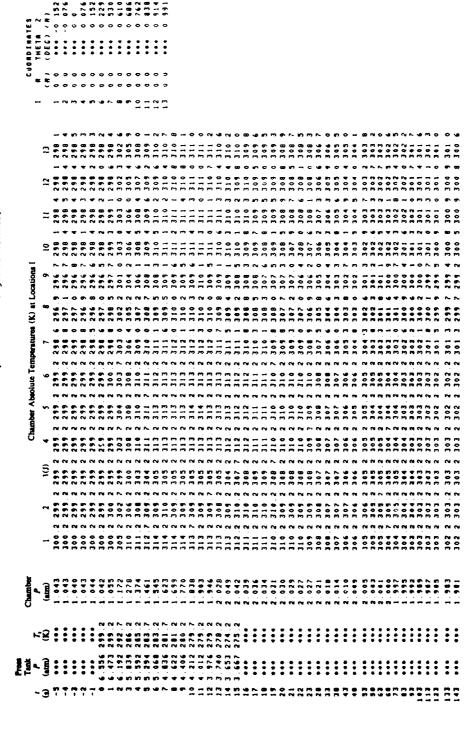


Table 3B — Inferred Pressurant Distribution, Scaling Run 24, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

										Promura	ınt Fracti	Pressurant Fractions (X) at Locations	t Locati	l suc					
-3	-6	<b>~</b> .6	۳۰Ĝ	•	B/0	P×	-	~	<b>3</b> (i)	•	<b>~</b>	•	7	••	•	0	=	12	2
		VE OPER	ING																
	29.3	25.3	7.96	-	0.00.0	0.00			0.00.0	•	000	0 000	900	0000		0.00	000	000	
_	52.9		76.1	\$62.8	5.8912	110	~	. 570-3	3.479-3	478-3	-	2-02	269	~	•		1 965	- 484-	2 269
` .	7.7			3.7 A	2 1610		. 516		:	•		4.7	436	316			•	=	76.0
	17.7		2.2	33.5	1.7461	191	. 19	365	=	=		-	7		173		7	213	2 2 2
_	33.4	7.7		23.2	1.7461	164	- 193		191	٠		7	143	-	173	083	1 43	219	1.58
_	13.1	37.1		17.4	1.1421	.217	•	299				0.0	148	170	245	139	170	245	213
_	16.4	39.2		16.0	. 9162	260	. 127	336		127		173	226	102	513	245	228	. 256	275
_	37.3	•		. S.	. 0012	. 299	. 127	163		. 127		211	253	253	321	270	295	137	295
_	37.7	#. #.		15.7	. 7530	331	. 200	Ξ		. 200		200	280	320	320	281	360	336	320
_	17.9	12.5		16.0	.7268	361	. 244	137		. 244		244	291	322	322	322	330	346	334
_	37.9	45.9		16.0	.6567	78.	. 277	203	* 6	. 277		277	115	338	362	346	338	17.7	362
_	E	<u>.</u>		13.7	2004	. 419	343	610	916	305		303	343	339	381	366	374	389	397
_	•	5		9.9	. 3363	. 429	•	621	913	124		324	347	313	362	392	<b>†</b> 13	107	415
ž,	74.	13 JA	366		•	,	į	:	;		:	;	:	;	•	;	;	;	;
			n .								7		= :			•		•	
		-	~	5	.7317	597	M -	~12	. 4	125	323	328	393	<b>4</b> 2 8	445	4.54	393	437	430
	17.7			31.6	2333	• 5 1	9		•	8			3.66	***	423	;		177	,
				- 22	1212					322	327		:					ì	
					770-	42.		225			. 72				72.		:		
	72		٠.	9	•	471			8		5-1	=	:	:	n n		=	7 2	4 2 2
	9.5		-	*	0771	47.	4.82	492	200	000	•	0	9 6 7	191	49.2	3.2	,,,	301	, ,
	3.4.6	50	٠.		1 2 0 3	124	224	439	109	439	6.0	=	•	139	•	9 7	2	:	:
	14.4	19.3	٠.	3 9	.0414	120	. 523	. 523	619	427	427	+37	404	136	456	•	436	456	436
•	24.2	70.7		•	0 4 2 2	120	***		6 0 2	404	404	401	9.7	60	69	3 3 3	4 4 4	9 9	4 4 5
•							7 1 2 2		245	7.	265	392	707	75	715	215		4 9 2	7
•	12.			• m		12.	2 20		342	• •			429				:	-	
•	13.4	37.	٠.		0 9 2 9	471	521	\$21	2.2	=		413	43.4	437	910	531	436	•	96+
•	11.2	37.6	٠.		0478	144	. 50.2	205	205	396	302	396	131	470	492	534	4 60	=	•
•	5		٠.		- 0946	14.	. 364	•	9	96.		=	439	430	•	34.3	419	•	1.6
•	0.	37.4			F # 13	124	340	32	5	435	435	132	E *	484	<b>9 8 7</b>	340	- - -	<b>40</b>	987
•	12.5	37.2		<b>*</b>	.0497	145	. 529	150	229	<b>6</b> 2	450	<b>4</b> %	432	131	496	262	;	529	475
•	32.7	M . 0	٦,	•	0.267	14	. 521	604	321	<b>6</b>		409	~	467	321	*55	-	<b>6</b>	* 2
•	32.6	36	27.9	•		~	200	395	209	395	395	3 6 2	129	209	303	245	209	931	. 6
•	72.6	36	٠.	•		1.4	4.98	383	498	382	131	3 6 5	<b>+ 9 +</b>	\$ 4 \$	803	277	<b>~ 0 ~</b>	÷	7.5
-	32.6	15	27 9	•	00000	451	* 5 *	3	;	**	• •	331	7.9	209	484	366	453	<b>6</b>	<b>4 B</b> 2
•	32.4	36.3	27.1	<b>5</b>	0528	471	260	443		\$ <b>†</b> †		317	<b>.</b>	302	205	525	8.5	<b>?</b>	8 9 4

Table 4A - Scaling Run 25, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

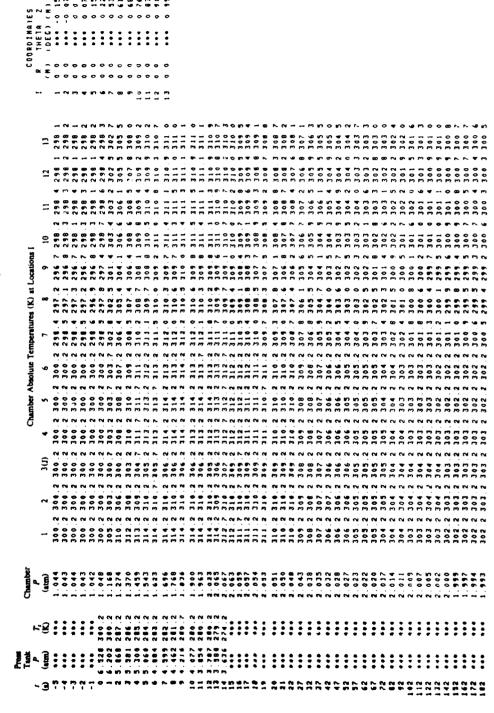


Table 4B — Inferred Pressurant Distribution, Scaling Run 25, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

Preservant Fractions (X) at Locations I	X 1 2 3(1) 4 5 6 7 8 9 10 11 12 13	).040 0.080 0.800 0.000 8.800 0.008 0.008 0.000 0.000 0.000 0.000 0.004 0.000 0.006 0.000		079 .156632	- 181 146 1.012 107 107 107 126 120 146 146 120 120 180	传中说: \$11世 · 多中年 · 31世 · 多的目 · 多的目 · 30章 · 0世年 · 60章 ·	064 446 902 187 187 290 204 280 106 269	, 通用的 · OTB · TOB · 的中国 · TOB · 数学说 · OTB · · · · · · · · · · · · · · · · · · ·	900 900 000 000 000 000 000 000 000 000	一年中四十八月四十二十四月 一日日日 一日日日 日日日日 日日日日 日日日日 日日日 日日日 日日日 日	281 603 926 281 281 281 313 378 394 386 386 386	.610 .933 .367 .286 .367 .335 .	428 64: 362 166 166 166 419 424 41: 427	200 200 200 200 200 200 200 200 200 200		200 C C C C C C C C C C C C C C C C C C	100 100 100 100 100 100 100 100 100 100	472 426 595 680 426 426 426 152 451 460 485 460 450 411	984 224 S64 S64 684 684 914 L04 L04 L04 929 888 184	461 350 640 461 461 371 389 452 470 514 461 461	424 526 619 434 434 434 397 452 499 508 462 489	418 512 603 418 463 418 409 456 502 530 456 484	ONE THE SAT SAT 198 MOT OLD DLY 025 025 025	THE PARTY AND ARCHIVE THE CONTROL OF THE PARTY PARTY AND THE PARTY AND T	0.94 CTD 0.95 0.04 0.04 0.05 0.05 0.05 0.05 0.05 0.0	164 174 100 110 110 110 110 110 100 100 100 10	, 的心的 《 CM 中, 如 CM 中, 的 CM 中, CM 中, 中级中, 中级中, 中级中, 中级中, 中级中, 中级中,	STOPP SOUN CONT ONE OF SOPP SOPP SOPP SOPP SOPP	429 429 634 429 634 429 409 458 634 429 634	COT INST OND BOD COT NIT NOT BOD BOT BOD INST BIRT	894 414 400 110 204 414 624 624 624 624 624 624	470 470 470 470 470 470 420 426 448 535 546 426 492	464 464 464 464 464 464 466 420 464 552 541 453	452 452 452 452 452 452 450 475 553 542 464 509	
tions (X) at		0.000.0		. 156 -	2 36	•	230	•	. 297	٠	•	•				. 382	00+	. 426	405	371	134	418	0.4	7	60	Ę	19	445	+29	. 403	6.2 <del>T</del>	420	• • • •	<b>*</b>	•
essurant Frac		•		•		- 2		•				•			•	•	•	•		•		•								•	•				
£		0 0 0		í	•	•	•	•	•	•	٠	•		•		•	•		•	•	•	٠				,	•	•		•	•	•	•	•	
	~	0-		6	-	2	7	4.	•	•						٠	•	٠	•		•	•	•	•	•	•	•	•	•	•	•	•	•	•	_
	<b>7</b>							•	•	•	•	•		•			٠	•	•	•	•		•	•	•	. ,		•	•	•	•	٠	•	٠	
	_	•		2170	7	7.1	8422	0000	72	1989	5931	0209	•	2643	•	3737	54	1264	1332		1078	0370	9520		7 0	•		34		•	. 1510	0457	. 2910	0475	0000
	9/B	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0		0		ĺ	•	16.4		•	13.9 .59			75		. 7 . 37	•	1.3 .12	•			•		1800	9900 9 0 0	•	1.3 .1258		0.00 0.0000	•	•	\$0. \$1	5		•
	. eG	186 60.0 29.1 105		<b>.</b>	=	-	_	30.3								m.					_												~		•
	 	14 69 EX 15 60 19							42.5 30	42.9 30	43.4 31	10.0 30.2 43.5 31.1			LOSED	43.6 31	11.0 31	43.2 31	42.3 30	41.9 30	41.3 30	41.1 30	40.7 30		40.1.30	39.9 29	19.1 29	39.0 29	39.0 29	39.0 29	30.6 29	38.4 29	38.2 29	38.0 29	
	۴ô	168 VALV 23.9 29.7	וווי	32.9	7.00	36.3	37.9	37.8	38.2	7.00	38.4	39.2	7		צורה כ	37.9	38.2	37.6	37.0	36.7	36.2	<b>36</b> . 1	2		2 17	25	34.7	34.5	34.5	34.5	34.2	14.1	33.9	33 · E	
	-3			•	•	•				•	•	•				-	•	•	•		•	•	•	•		-	•	•	•	•	•	-	-	•	•

Table 5A - Scaling Run 26, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

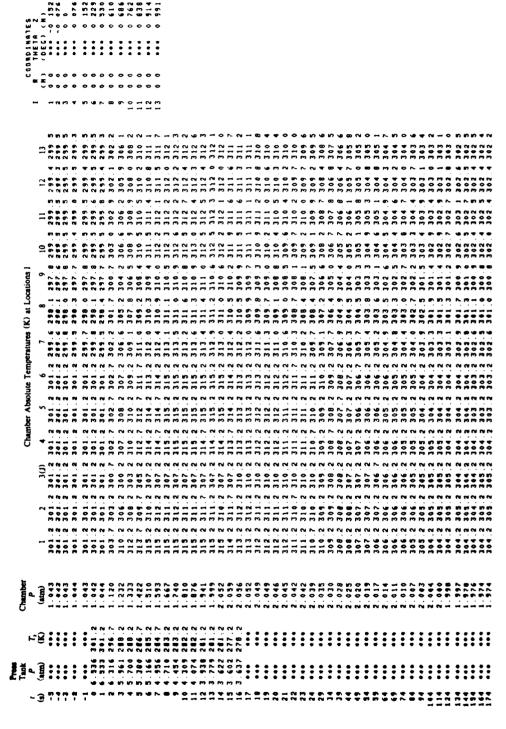


Table 5B — Inferred Pressurant Distribution, Scaling Run 26, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

										Testant	nt Fracti	Presentant Fractions (X) at Locations f	t Locatic	) <b>5</b> EC					
-3	<b>-</b> 6	<b>∵</b> ê	<b>r</b> .6	<b>60</b> .	₽/e	æ	-	~	36	•	<b>~</b>	•	^	•0	۰	9	=	13	13
	10. 30	VE 0.0	9114	•	•	9	•	9	•	•	•	•	•	6	•	•	•	•	
•				9	-22									2 0	9 6				
TATE	FILLY	. E .		:		:				•	•					•			
2.0	1.62	29.2	28.4	~	11.2327	. 063	- 243	400	3.625	1.045	1.043	1,045	116-1	. 664	- 761-	-1.406-	1.277	. 174	503
	13.0	33.7	28.3		2.9313	137	1.406	•	1.41	150	. 035	130	. 002	. 034	9 2 0	6	039	920	0 39
•	13.3	36.9	20.7		1.5466	196	- 118	•	961	. 126	126	2 48	680	0.0	163	0.08	089	187	163
•	17.2	3 6	29.7		9349	.242	0.26	•	843	. 126	. 126	. 227	157	167	217	1.87	187	207	207
•	7. 17	=	30.4		9988	E 8 3	0.29	309	279	. 149	-	239	221	221	273	246	2.2.2	302	275
<b>•</b>	39.0	<b>.</b> .	<b>9</b> . I	15.8	8114	319	163	•	838	202	203	. 247	281	264	315	281	590	332	315
-	79.3	9.7	31.3		. 7173	349	. 220		. 873	. 220	. 220	220	277	301	326	326	334	342	334
• •	39.8	7	31.2		.6717	376	. 264	304	. 903	. 264	264	264	588	352	336	344	376	366	360
	39.5		31.9		2969	00.	287	•	. 924	. 287	287	202	333	327	367	374	3.59	374	390
11.	39.8	-	32.2		5718	.421	313	٠	.946	313	313	313	329	376	384	360	00	40	384
12.0	39.5	55 4	32.4		. 5632	744	328	•	963	368	320	328	360	314	392	416	915	416	424
CORREA	ICE VAL	173 34	SUBE														•		
13.0	19.2	<b>.</b>	12		5330	487	326	. 647	969	406	326	326	398	398	422	+ 1	430	944	4 3 8
* * *	19.1	•	32.6	234 5	. 4682	.472	. 327	734	978	408	327	327	392	416	423	4.4	5	:	4.9
TALVE FULLY CLESED	FILLY	CL 88 E1																	
13.	~ =	•	75.4		1538	1474	378	•	96	450	378	378	=	428	428	436	194	433	*
16.	F .	7	15.1	63.0	0 9 7 8	121	. 449	. 935	902		449	+	423	415	*		4.19	994	4.75
17.	17.7	÷.	31.		1366	424	<b>484</b>	•	701	434	<b>†</b> 3 †	434	416	-	445	8 ~ 4	4 7 8	469	469
=	2.	+ 5	E .	6.8	.1076	<b>424</b>	ij	•	9.9	484	Ť	385	410	450	<b>#38</b>	436	4 38	436	456
19.	17.2	7.7	5 . E		0000.0	<b>424</b>	. 462	•	. 646	. 462	462	462	<b>9</b>	405	:	499	425	433	471
 	36.8	=	31.2		1125	+2+	. 13	•	633	119	++	+	430	++	•	468	439	B 9 F	439
23.	9.9	-			0386	<b>*2 *</b>	418	•	619	. 514	514	418	437	437	44	514	437	447	951
22.	7.97		9.00			**		•	386	487	~ <b>!</b> +.	2 E +	ZE# .	452	437	477	437	767	437
27.0	76.2		<b>6</b>		0000	*4.	<b>6</b>	•	268	6 9	469	469	459	439	439	208	439	+	439
24.0			9 00	9		424	6 T	•	145		7	4.38	*	404	9 7	48.9	405	# 9 •	4 38
					000	**	P	•	609	905	906	300	-	4 2 4	¥ F) ¥	486	<b>+</b> I <b>+</b> .	₩ ₩ .	† <del>.</del> †
					5640			•				*	23	0 1	3	000	390	33	4.32
	100	7					777	•		777				5 6		1 6 4	•		*
	7.87				•			•					7 4 7						
	1.80	39	30		0000	**	423		600	6 M	223		- E						
11.0	6.48	16.1	30.2		0463	474	312	•	312	512	312	312	433	405	4.5.7	3.23	380		
	9.	=	30.0		0 9 3 0	1474		•	296	484	18	ij	427	382	7.0	340	3 9 3	:	438
			2		0499	424	4.33	•	369	A 55	269	4.3	443	2 S E	515	\$ 3 3	397	000	0
			23.		e no	* 2 * .	į	•	0	. 492		÷	# •	6 B	327	- P	410	5	* 7

Table 6A - Scaling Run 27, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

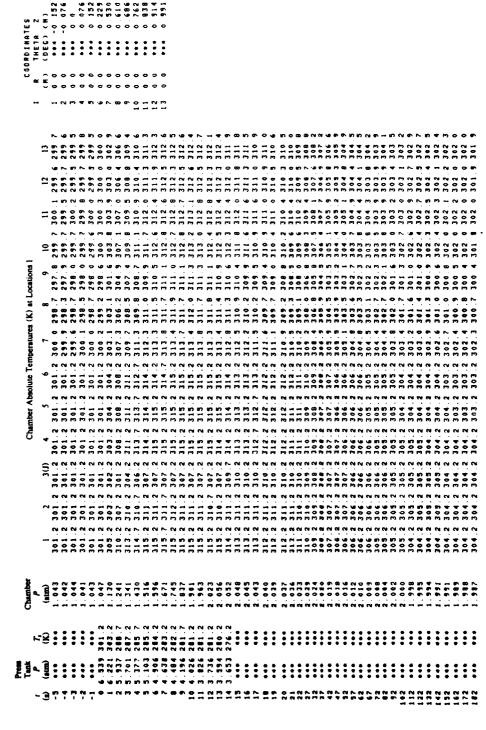


Table 6B — Inferred Pressurant Distribution, Scaling Run 27, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

1										Pressur	ant Fraci	Pressurant Fractions (X) at Locations	at Locati	i sto					
		_	<b>r</b> •6	92	9/8	₽≺	-	2	30	4	٠,	•	1	90	•	01	=	13	13
1.	BERCE	PALVE OP	ENTHE																
18			_	+.	0.000	0000	000.0	0.000	000	000	000	000	000	000	000	000	000		
				132.8	•	990	-3.915		624	111	402	402	- 1	363	405	709-	3.710	- 405	1 49
1.0   1.0	۳.	_																	
15.   15.	_		•	36.1	•	138	- 523	. 236	753	017	017	017	,	.017	160	000	0.59	133	<b>78</b> 0
10	_	_		17.7		961	1.37	•	946	088	880	880	149	174	233	137	1.86	233	1.62
10	37	•	30.2	. 92 . 36	. 9642	242	- 033	•	7.95	790	964	. 162	201	249	298	220	2 4 9	569	249
12		42.0		16.3	906	283	890	•	767	155	13.0	58.	234	260	304	286	5.69	è	304
10   10   10   10   10   10   10   10	-	_		16.0	7943	318	1.59		819	159	1.59	241	233	299	332	291	316	332	299
19.6   44.4   21.7   7240   24.9				13	7110	# P	•		937	220	220	239	251	339	339	331	355	339	331
19.5   6.4   9.6   12.   1.5				16.7	7230	375	2 49	•		243	249	249	312	331	375	367	367	303	7.00
10   10   10   10   10   10   10   10	5			16.7	9600	404	278		903	278	278	278	317	5 F F	39.5	387	403	393	387
The Value   The Case				16.0	5438	424	***	•	. 9 23	100	304	304	. 366	397	403	302	387	£14.	4 2 8
10	BESCH	TO BATAR	18 VRE																
199.5 4	1.0	T.81 9.		16.4	. 5262	# T	126	•	# <b>6</b>	. 32 £	321	331	152	437	422	¥ ;	437	437	4 2 2
10   10   10   10   10   10   10   10				7.9	. 5419	194	330	•	. 933	350	320	320	191	164.	<b>€ E +</b>	+63	627	455	124
1			_	,		•	,		;	-	;	:	;	;	;				
1				*	2078	470	216	•	9	B 6 7	6 T E	516	-	6 ·		•	29	5	7
10				<b>6</b> , (	129	470	. 363	•	962		m (	E .	9 :		9		80	9	7.4
1				P. 1	F 9 P T .			•			2 4	D 1				•	e c		
1				• -	107	200		•			704	0	2					2 .	
186. 4 11 2 11 4 12 2 11 4					95.	20	7		9			=		887	9	4 7 0	4 20		-
146.4 4 11 2 11 2 2 0 0 11 2 2 0 0 11 2 2 0 0 11 2 2 0 0 11 2 2 0 0 11 2 2 0 0 11 2 2 0 0 11 2 2 0 0 11 2 2 0 0 11 2 2 0 0 11 2 0 0 0 0				•	8680	0.4	4 2 3		6 13	4.2		£ 4	434	M 4	40.5	301	M W	P 4	E 9
15   15   15   15   15   15   15   15	_			1.2	.0613	470	400	•	<b>6</b> 04	409	404	409	438	306	487	308	497	477	4 3 8
135.8 40.4 10.6 0.0 0.0000 4.70 4.10 13.0 4.20 4.20 4.20 4.20 4.20 4.20 4.20 4.	_			•	0418	470	376	•	573	476	476	378	4.4	467	486	336	467	476	476
135   13   13   13   13   13   13   13				6.1	.1296	410	438	•	340	# T	43	438	438	8++	193	4.9.9	87	18	80
135.7 4 6 12 30 35 6 0 0 4 48 6 70 4 31 503 503 451 503 399 4 41 4 61 513 139 13 13 13 13 13 13 13 13 13 13 13 13 13	_					470	412	•	535	432	432	432	422	+6+	484	525	₩ W	163	443
135.5 4 60 0 10 55 7 0 0 15 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	13	~		•	0448	470	451	•	503	45.	503	399	441	7	513	534	430	482	.462
135. G 40 G 10 G 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	1.0 35	.5 40.0		~	0436	420	477	•	477	477	477	427	+ -	994	208	<b>8</b> 08	436	47.2	424
135.2 19 13 10 1 1 4 0917 470 413 423 1343 423 1343 423 425 423 423 133 142 13 13 13 13 13 13 13 13 13 13 13 13 13	33					470	994	٠	363	097	9.0	094	407	78+	49 2	533	09.	4 + 9	428
185 0 195 18 10 2	35			-	0937	420	415	•	543	433	543	435	435	436	521	532	424	467	4.56
135 0 195 M 10 2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	35			~	.0482	470	423	•	533	423	533	423	434	300	533	511	467	478	434
1 35.0 39.3 30.2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	23			•		470	443	•	300	300	300	. 443	412	489	200	511	456	445	412
134.7 28 9 20 6 1 4 0993 470 466 466 466 466 466 466 467 466 527 27. 28. 28. 28. 28. 28. 28. 28. 28. 28. 28	33			•		470	427	•	444	477	477	433	433	455	499	543	11	466	;
184 4 285 18 29 9 1.0 1.0 1.0 1.4 470 4.14 4.34 1010 4.34 1010 4.44 1010 4.44 4.0 10.7 10.1 10.1 10.1 10.1 10.1 10.1 10	÷	=	90	-	6990	470	466	٠	995	994	994	99+	£ + + .	991	534	534	451	125	£ # # .
144, 488, 154, 414, 050, 414, 050, 414, 050, 414, 050, 414, 050, 414, 050, 400, 400, 400, 400, 400, 400, 40		. A 310.5	29.9	<b>6</b>	1034	470	414		330	<b>P</b> P	530	į	<b>1</b>	684	527	515	457	480	410
24.4 288 5 29 9 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	ř	.4 31.5	29.4	•	0.000.0	0.45	. 530		230	+ -	\$3¢	414	402	495	519	553	4 4 9	449	-
	ï	4 38 5	29 .	•		0.4	498		4 9 8	161	÷	•	403	498	486	268	÷	428	417

Table 7A - Scaling Run 28, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

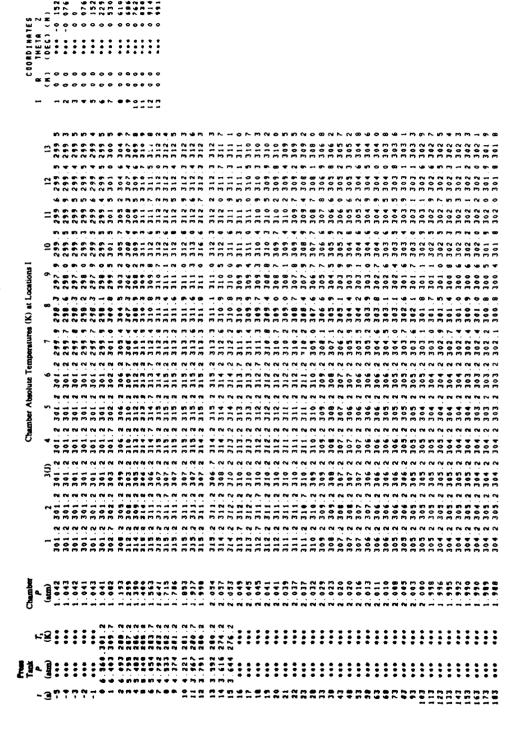


Table 7B — Inferred Pressurant Distribution, Scaling Run 28, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

										Press	Pressurant Fractions (X) at Locations I	tions (X)	at Locat	ions					
-3	<b>~</b> €	<b>~.</b> €	r.Ĉ	90	9/8	₽ĸţ	-	7	3(I)	•	~	•	1	•	۰	91	=	13	:
CORRECT	26.9 26.	40 34	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		0	•	•	•	•	•	•	0	0			_		9	
				2 8 8 . 9	4.6497	6.0	. 0 43		. 167		081	10.	0 3 3	318	:	1.67	1	1 10	960
	7 7 7	32.0		39.4	5.1275	.113	-1.06	•	~		0.53	. 0 3 3	- 226	7.28	0.50	- 612	393	. 003	1 70
-	93.0	9.0		20.0	100	177	202	•	2 1.000	•	063	132	132	0.38	196	9 2 0	920	212	172
•.	37.0	39.2		16.5	1.0539	. 226	- 06	•		M 0	135	1 15	186	1 36	216	196	. 227	. 327	.206
•	=	41.2		16.3	9618	.270	. 026	472	2 .829	113	204	204	240	31.	367	222	213	376	258
•		42.3		15.9	. 8311	307	Ē.	,		•	17	261	261	244	319	211	277	305	277
٠.٠	19.3	42.5		13.5	7346	6EE.	. 21	٠	•	•	210	513	297	274	313	289	303	129	313
:	39.9	. 4		13.5	6719	29E	<b>7</b>	٠	٠		261	. 261	307	315	330	330	346	153	346
•	39.5	44.7		1.91	.6501	393	7		•	•	289	513	342	327	330	342	- 3.5 ·	373	363
• .	39.3	÷.	31.	13.9	5833	.413	31		•	•	313	313	359	328	389	366	331	104	404
11.	39.6	¥ .	12.1	15.6	5276	484	33	•	•	•	337	337	159	374	389	374	397	-	•
	CORRECT VALVE CLOSURE	.VE CL	13 VRE																
12.1	19.7	43.4	32.3	14 9	2609	437	37		896. 0	•	371	371	917	394	9 7 7	=	423	191	1 6 1
13.	19.3		32.4	16.0	5563	.472	¥.	969' 6	-	. 426	349	349	395	426	456	;	Ŧ	=======================================	=
BATUA	FILLY	35873																	
14.	19.0			~	0927	6.43	÷	•	•	•	404	**	428	420	443	<b>7 7 9</b>	436	467	467
13.	=	7		~	1265	674.	<b>6</b> 27	•	•	•	393	393	:	417	473	6.9	413	•	206
. 91		1		e.	1352	473	•	•	•	•	=	•	=	Ę	437	£ 9 + .	•	8	4 90
17.		42.6		<u>ب</u>	. 1432	473	. 419	205	219 2	419	+ 1	419	463	437	472	463	4.53	205	490
		42.6		0	00000	.473	. 42	•	•		472	4 2 8	437	419	116	481	4 2 8	490	0 6 7
19.		41.7	30.8	<b>+</b> .	.1519	.473	+	•	٠	•	443	443	434	418	797	7.5	4 36	300	473
20.0		41.7	30 · B	0.0	00000	473	7	•	•	•	£ 9 .	433	451	445	460	206	45	497	4 7 8
21.	36.3	1.3	7.02	m. N	.0796	6.3	Ŧ	•	•		484	393	139	£0.	478	<b>6 6</b>	415	13	~
22.	36	6.0	5.0	4.	. 0822	674	7	•	٠	•	478	362	*	450	497	# B #	•	202	4 7 8
<b>3</b> 3.	9.	•	30 .	•	000000	473	•	•	•		433		456	426	465	313	4.55	213	÷
24·	36.0	40.9	30.5	0	0 0 0 0 0	673	7	•	·		111	111	=	415	470	25	Ę	=	518
25.	55.50	70	20.2	۸. W	1286	674	÷	•	•	•	463	413	433	313	503	513	423	543	513
<b>36.</b>	13.4	•	30.1	P.	.0444	473	6	•			494	393	434	<b>†</b> 0	203	494	434	328	÷
27.0	¥.	0.	30.1	0.0	00000	473	~	•	•	•	674.	4.3	453	423	÷	514	<b>463</b>	204	4 9 4
2. E	13 . 2	39.		1.3	.0432	473		•	•	•	437	437	~	90+	488	539	426	496	208
29.	7.	39.6		<b>1</b>	0460	473	7	•		•	442	442	. 9	390	313	346	=	. 336	236
		3.9		¥.	0469	.473	7	•			434	434	*	423	539	528	=	539	228
11.	- -	3.3		<b>4</b> . 1	0478	£ 4 5	<b>T</b>	•	•	•	521	<b>†</b>	9 7	9	310	242	8	521	210
32.	-	39.5		•	000000	473	7	•	•	•	482	4 2 8	439	4 28	485	3.4.5	•	303	514
33.	-	79.5	29.1	0.0	00000	473	9			•	462	462	Ŧ	<b>6</b> 0	464	550	419	256	237
74.	7.	-		~	100	.473	Į	•	•	•	-	=	4.0	*	528	3.5	426	245	247

Table 8A - Scaling Run 29, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

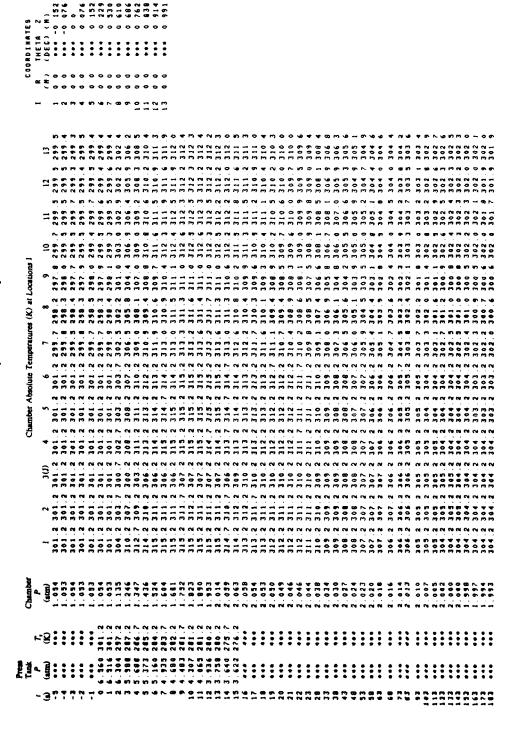


Table 8B — Inferred Pressurant Distribution, Scaling Run 29, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

											rresent	int rinci	fressurant Fractions (X) at Locations	r Location	1 <b>5</b> 1					
-3	<b>₽</b>	<b>~</b> :6	r.g	•		B/e	<b>~</b>	-	7	ğ	•	×	•	1	90	•	9.	=	12	<u> </u>
COUNTRICE VALVE OPENING	E VAL	340 3A	N I N G																	
•	26.9	26.9	162.0	•	•	0000	000	0 000 0	000	000	. 000	000	0 000'0	0	0000		000	0	000	
-	26.9	26.9	· *	31070.9	Ë	. 8821		0 48	, B00 · -		- 800	00	800	049	021	049	0	0.36	- 610	800
TALVE F	1114	BPEK																		
•	23.5	29.6	3.92	152.1	:	.1625		- 078	980	.072	517	251	910	- 210	374 -	144 -	210 -	. 177	012 -	078
-	13.2		27.9	32.7	~	.6471		. 298	189 1	324	920	.026	109	- 620	052	108 -	. 022	0.59	108	039
•	35.8	37.6	21.2	18.7	-	3013		- 013	. 290	930	. 077	. 077		.152	0.98	173	1 4 1	1.20	194	173
•	37.6		23 . 1	13.1		8797	.240	. 035	392	.749	125	. 125	. 214	. 196	205	223	196	214	232	214
•	3.5	41.9	23 . 7	1. 91	٠.	9130	.282	10.	411	. 821	. 166	991	. 248	. 231	223	564	248	. 236	289	256
•.~	19.0	<del>1</del> 7	26.3	13.0	_	2786	.316	. 169	482	874	169	209	248	. 224	273	287	.271	303	310	287
•	39.2	<b>1</b> .0	30.7	1.91		7451	.347	. 221	. \$27	909	. 221	. 221	. 297	. 274	282	282	312	305	335	328
•	39.3	B. T	7	15.3		6192	.373	. 268	. 530	998	. 268	.268	. 268	. 298	343	335	343	365	358	343
	39.9	•	7.	15.4	_	6244	795	. 298	320	169	. 298	.291	2 9 8	335	350	364	379	379	379	379
• . =	39.3	43.1 31.7	7	16.4	_	5965	419	313	612	910	313	313	313	321	387	381	368	410	₩03	388
ï	=	173 34	3116																	
	•	43.2	31.9	16.4	_	5421	438	327	. 626	926	364	327	327	. 364	372	394	454	409	911	416
111.0		+		-487		2010	433	340	. 641	942	416	340	340	348	416	408	453	446	431	423
	_	CT 88E0																		
	6.8	•	22			4511	468	357	1 199	800.	+34	337	337	373	96E	418	456	434	426	426
_	9.6	÷	32.3	119.6	•	.1226	894	96E .	343	192	99	394	394	402	431	9 * •	475	£84	453	194
16.0		=		-150.4		.1542	894.	£ 4 4 .	. 520	.675	. 443	=	. 443	404	438	E + +	466	12	439	121
17.	:	÷.	E	-127.4	_	1306	894	426	9 0 0	999	. 426	426	426	426	426	430	482	4.38	99	4 5 8
• .	• .	7		-32.5		0338	• • •	100	36.	643	. 482	10+	<b>.</b>	014.	418	430	199	. 442	482	412
19.4	37.6	43.2	31.2	-101.5		1041	. 468	430	533	617	. 430	<b>98</b> *	804	914	=======================================	450	483	438	997	438
_	17.4	13.0	1.	-34.8		.0357	894	435	513	<b>†</b> 0 <b>9</b> .	433	435	433	435	437	469	.511	433	6 9 1	469
_		~	. 0	B. 701-		.11.	<b>9 7</b> .	421		893	. 421	. 421	121	447	50	F .	208	E 2 4		433
22.0	17.0	75	6		•	0000	. 468	6 P	<b>7</b>	268	437	101	437	437	4.55	E 9 9	533	433	472	£ 9 +
	:					.0763	89.				*	•	* 2	. ·	929	6 8 9	9 1	9.	6	*
						***			. 24	070					. 90			*	•	:
	90	7	9	0 1	•	0000	89	917	900	306	900	900	914	423	10 ·	194	324	435	191	432
	N #			- 0						2 2 2	224	7.4.	724		164		0 F	413	8 9 9	8 7
2			0	14-		0422	4	1	17				· ·							7 KT
29.6	13.9		20	7	•	0423	894	436	9.0	531	9.6	531	9.0		9.0	9	531	133		*
M	15.8	<b>†</b>	30.2	-41		0423	894	£ 1.5	. 41.5	311	\$ J \ .	511	511		*34	694	540	434	501	302
11.	38.6	•	-	-42.0		0431	. 468	394	44%	164	. 49.1	+ 9.1			413	462	539	E 2 4	\$00	510
32.	23° G	7 9	ê	-42.7		0411	891	378	9.4	9.4	926	9 2 4 .	9.4		397	9.4	554	427	313	515
22	13.2		29.9	-12		000	468	75	462	462	762	462	462		402	472	553	415	215	522
	9. 19.	7.		T.		2 9 6 2	89.	-	=	<b>9</b>	•	-	4 0		397	499	370	4 2 0	0 10 10	020

Table 9A - Scaling Run 30, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

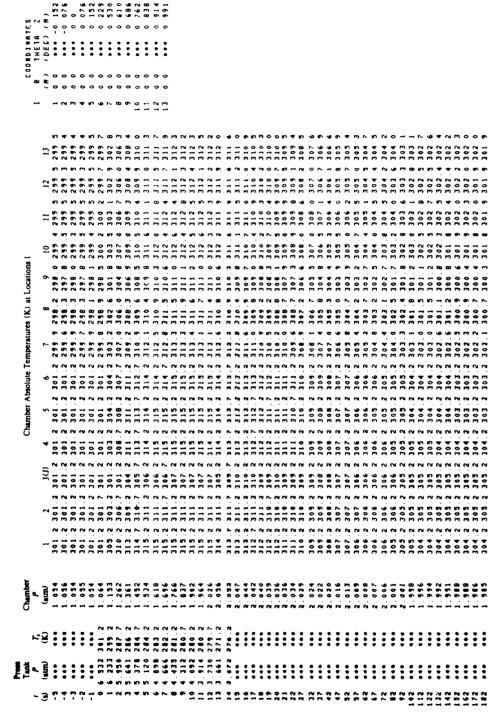


Table 9B — Inferred Pressurant Distribution, Scaling Run 30, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

										Pressur	Pressurant Fractions (X) at Locations I	ons (X) a	t Locatio	- su					
· (B)	<b>⊷</b> 0	<b>r</b> .6	<b>∵</b> Ô	93	9/8	×	~	7	36	•	<b>~</b>	•	,	••	۰	10	=	21	=
¥	VALVE	2 OPE	65.3	<b>a</b> ,	0.0000	000.0	000	900	0000	900	0 000 0		0 3 0	000	00	000	000	0	
TRY BATOR	2 A 1 18	* # W & .		٧	6160.01		B7 - 1 -	264	•		E .	- -		* 60	50		9000	08	306
	50.00	7,7	29.1	6 E	2.6715	139	966	196	1.389	- 101	.001	860	441	021	138	980	860	3 60	0 7 8
				9		242	980	2		950			7 5	222					7 6
•		6.2	29.9	1.6	9336	2 80	090	90	915	1	-		202	269	988	278	319	90.2	5 6 5
£		7	30.4	16.7	6998	317	140	499	9 2 8	140	7	220	244	299	318	319	331	313	299
7.0 31	1.1	-	10	16.0	. 7369	347	200	910	8 38	200	200	239	378	60E	347	340	340	3.33	340
	7.0	•	97.70	9. 9.	6367	E 4 E	2 4 4	4 B 5		243	7 7	# F	281	349	200	9 6	8 6 6	364	349
	9 10		7.7	9	36.40			629	60	7 6	2 6 2		323	0 T	- 6	• •	9 7		0 00 0 00 0 00
COUNTRICE	VALVE	ี	SEE.												;		:	;	
11.0	9.8	23.3	31.9	16 3	. 5238	964	310	9 9 9	206	310	310	310	362	399	422	4 2 9	437	4.2.9	399
12.4 39.W 43	M. 6	m .	32.		.5434	<b>*</b> 0 <b>*</b>	314	. 634	.919	330	314	314	367	457	427	4 3 8	₽ 2 8	457	427
12.0			31.1		8778	F 9 9	E 6	623	1.048	E 60	87 87	PT 25	36.	8.5	422	9	7	;	¥ 0 ¥
14.0	•	6	31.4	-	1346	463	566	366		5 F	# P	97 97		10 M			6.4	7	7
15.0 1		2,8		~	1791	£9.	399	-	£ 23	399	399	399	399	445	459	492	4 5 9	7	4.39
16.0	6.9	12.2	30.8	5.	1140	.463	¥86.	£09	919	384	384	***	401	471	434	513	4 8 9	*	4.5.4
17.6 30	9.9		30.6	7.	.0790	.463	397	376	. 621	397	397	332	454	431	487	513	469	469	460
10.0	¥ 10.9	11.4	30 · 4	-	0813	.463	402	339	.677	405	402	405	393	994	466	4 9 4	4 8 4	8 7	4 3 9
19.4	7.9	1.1	30.4	•	0418	.463	381	296	629	381	4.2	381	404	9 + 0	E & 4	520	4 5 5	446	4 4 6
20.0	4			<b>.</b>	. 1298	£9 <b>+</b>	6 <b>7</b> 8	390	342	•	•	4 4 6	404	4.35	484	513	4 7 4	9 4 6	417
21.0	S.7	60.5	4	0.	00000.0	£ 9 ¥	418	363	611	8.7	4 1 8	418	399	t- ₩	476	534	447	437	4 3.3
22.0	4	-	D :	~	0.964	463	400	348	398	100	430	000	450	450	319	529	0	439	0.5
2 4 4 6	 			•	50 G	M	916	. 23	\ <b>3 8 9</b>	986	9 7	9 .	967	9 .	9 0	, n	9 .	9 7	9 7
25.0				· m	9 50		4		7	9	, ,		7 7	7 -				7	
26.0	9.4	39.0		. P.	4660	F 9	424	47.7	9	454		4.24	424	92.4	0 10	) PO	2.5	427	4 4
27.0 34	6.63	39.0		0.	000000	463	4 18	471	524	418	9 7	418	204	492	213	4	8	7 2 7	439
28.0 30	1.6	39.0		0.	0 0 0 0 0	.463	¥0.	457	310	404	404	404	414	689	520	595	4 7 8	194	299
29.0	E. 5.	<b>1</b> . <b>1</b>		~	.0512	.463	378	. 539	984	378	486	378	0:4	453	205	593	453	475	4.75
31.1	<b>4</b> .3	9.		~	.0523	.463	333	317	.463	€ 9 <del>+</del>	<b>4</b> 6 3	353	419	Ĩ	528	5.83	452	206	473
31.0	0	=		 	.1080	463	<b>+</b>	497	=	-	4 4 1	4 4 1	39.	430	520	5 6 5	4 4 1	8005	452
32.6	ان ان ان	6.75	? 62	æ		463	431	488	431	431	431	431	396	404	545	268	4 5 4	511	445
23.6		6		0	0000.0	463	423	483	÷ 23	425	455	4.15	390	439	3.5	374	4 2 0	216	Ø <b>*</b> *
7	7	2.7	29 . 1	<b>3</b> 0	0.571	463	413	471	<b>4</b> 13	F -	£ 1 3	413	390	£.	553	265	4 93	2 <b>4</b> 5	₩ ₩

Fable 10A — Scaling Run 31, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

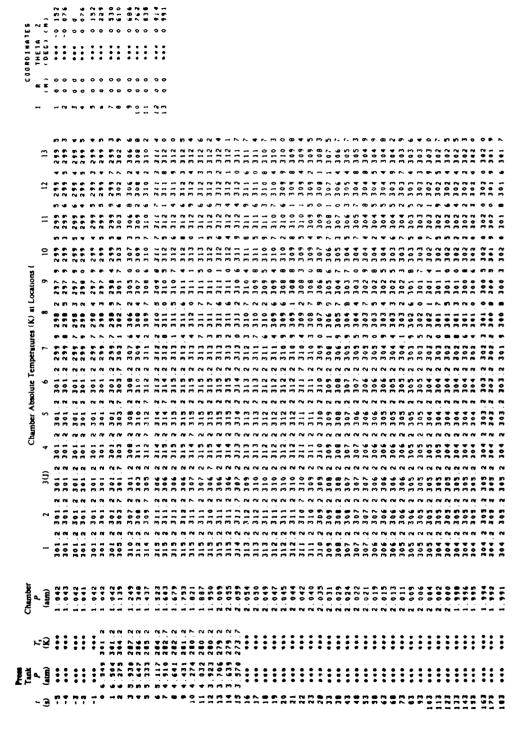


Table 10B — Inferred Pressurant Distribution, Scaling Run 31, Test Configuration 1: One 2.54-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

										ressur	Pressurant Fractions (A) at Locations I	ons (A) a	i Locatio	ıs ı					
-3	<b>~</b> §	<b>∽</b> ô	<b>~</b> .6	93.	9/8	124	-	~	3(1)	4	\$	•	~	00	٥	0	Ξ	13	13
	26.9	LVE 0P	EN 146 133.6	1	•	000.0	0.000	000.0	000	000	000	0 0 0 0	000		000	000	000	000.0	
1.0	27.0 FILLY	27.0	28 · 2	18260.2		000.	070	0 2 0	- 020		0 2 0	- 020 -		390	930		170	1.0	183
	•	•	29.6	129.7		920	-4.509	т	_	~		3 333-1			Ė	5 554-	20	- 849-	372
-	33.6		200	32.3	~	147	429			0.84	9 8 4	1 480	147 -	147	0.58	960 -	0 0 2	135	850
•	7.82		23.4	20.5	~	204	072			0.53	181	181	6 9 3	0 4 2	.68	0 9 3	0 9 3	181	1 4 3
•	37.4		23.6	13.8		249	• • • •			153	1.93	202	153	163	232	192	192	122	232
-	3.6		30.4	14.9	. 8133	289	087	434	869	173	173	260	212	.243	569	252	2 4 3	569	569
~	39.1		30.7	15.6		324	. 175		. 907	175	216	237	249	281	583	265	588	305	297
_	39.3		. IE	15.9		924	229		934	. 229	229	229	276	292	323	307	315	347	347
_	39.6		31.4	15.1		380	260	•	.962	280	280	280	305	233	317	340	348	363	355
_	39.6	450	31.6	15.6		***	70E	٠	906	348	307	307	330	330	367	352	352	382	390
_	9.6	45	=	13.6	•	454	331		924	331	331	331	331	375	360	364	398	413	398
=		1.0 E C.L																	
_	7.67	£3.3	2	17.3		£ 4 4	329	. 705	968	329	329	329	159	374	397	413	397	415	457
_	39.3	+ 2	75.7	-1248.8	4803	094	343	144	1.020	418	343	343	358	396	£04	4 1 8	<b>4</b> 33	433	4 2 6
	FILLY	CL OSE																	
_	39.3	43.3	2			. 472	349	632	1.029	425	349	349	387	405		4 4 0	4 3 3	-	4 33
_	39.9	£.3	2		,	472	101	188	912	44		401	379	<b>60</b>	453	452	60*	430	0.9
_	1.6	E .	2			472	457	. 334	. 7 62	457	425	4.24	415	457	<b>†</b>	445	457	4 4	442
_		44.5	Ξ		.1275	.472	443	523	189	F + -	++	£ 4 3	443	43.	121	4.5	4 36	475	451
_	38.3	7	ä			.472	*0*	264	++9	484	<b>+</b> 8 <b>+</b>	† B <b>†</b>	412	412	436	9 9 4	¢ 50	432	476
_	9.0	<b>1</b> 3	=			.472	£9 +	345	626	463	463	£ 9 \$	406	439	423	455	4 4 7	£ 9 ¥	480
_	37.7	43.4	=		1690	.472	447	. 530	613	44	~ • •	447	430	422	455	9.8	4 3 9	6 B Þ	489
_	37.6	43.2		-91.7	•	472	924	320	<b>6</b> 04	436	436	436	419	453	:	503	6.9	486	495
_	37.3	42.8	E			472	707	524	567	48	- 8 - 8 - 8	₹38	421	<b>*</b> 0 <b>*</b>	<b>*</b>	490	430	48	490
23.0	37.0	4.2	Ξ			.472	457	944	632	437	457	425	<b>†</b> 0 <b>†</b>	422	8 <b>*</b> *	<b>1</b> 2	<b>4 3</b> 7	<b>4</b> 2	4.5.7
24.4	37.0	4.2.4	ä		۰	472	4.88	535	6 20	;	=	÷	409	10	;	514	4.27	479	884
23.	36.3	41.7	ê	-300.5	1136	.472	501	101	595	501	201	Ξ		393	594	4 8 3	=	483	£ 0 ¥
26.	36.5		9	•	•	472	¥6.¥	¥6.	584	-	Ĭ	¥ 0 3	412	421	994	483	÷	476	994
27.0	36.5			•	•	472	478	478	369	478	8 / 4	4 2 8	904	433	4 4 2	513	442	69	694
21.	36.2			-208	•	472	450	331	331	138	. 4.3	4.28	431	403	468	523	415	987	4 2.7
23.	36.1					472	233	10 to	50.00	=======================================	-	141	423	413	488	207	435	# B #	9.9
=	7. 7			•	00000	472	213	. S E 3	513	513	513	÷14	401	4 38	991	* 6 *	<b>#</b> 38	997	4.48
3.	*			•	•	472	10 G	809	. S 0 3	P 0 0	203	4 0 9	414	437	•	331	7	9 9 9	• • •
33.	5.0		o E	-100.6	.0417	472		0	8.48		• 8 •	433	423	:	471	34.	-	<b>-</b>	
-		P.	e .	- 273 .	9880	472	m • • • • • • • • • • • • • • • • • • •	9 7	. 363	10 T		9 4	9~+	<b>+</b> 0 <b>4</b>	10	8 2	404	•	9
•	10 m		30	-114.2	0439	.472	. 347	+	547		:	•	<b>6</b> 0 <b>7</b>	4 2 9	308	347	4 2 9	<b>-</b>	• • •

Table 11A - Scaling Run 32, Test Configuration 2: Two 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

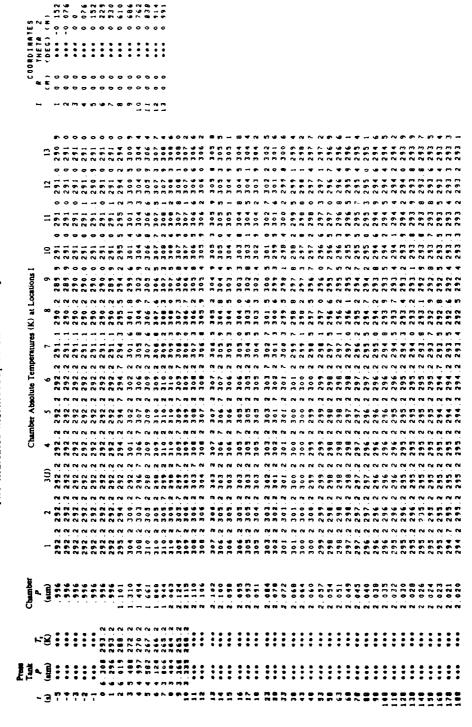


Table 12A - Scaling Run 33, Test Configuration 2: Two 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

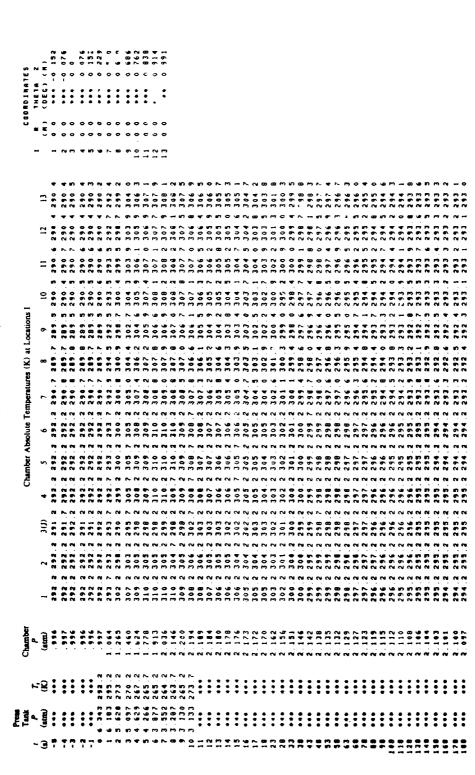


Table 11B — Inferred Pressurant Distribution, Scaling Run 32, Test Configuration 2: Two 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

2   3(1)   4   5   6   7   8   9   10   11				<b>₽</b> 2(5)	•	
1000   1000	p-c	¥ 0/8			9/8	B/6
11.2	0	0	0	1818G 182.7	FE DPERING 0 00000	FE DPERING 0 00000
12.2	600.	- 6624	. 0024	20.0 46.0 .0024	146.2 20.6 46.0 .0024	20.0 46.0 .0024
22.2		11.8392	121.9 11.8392	20.5 121.9 11.8392	21.3 20.5 131.9 11.8392	21.3 21.3 20.5 131.9 11.8392
### ### ### ### ### ### ### ### ### ##	•	W MM IN	A1 10 10 10 10 10 10 10 10 10 10 10 10 10	20 M M M M M M M M M M M M M M M M M M M	24. US 20. US 21. US	A 100 M 100
### ### ### ### ### ### ### ### ### ##	•	•				
### ### ### ### ### ### ### ### ### ##	67.6	014. BOYE. W	90.C. M. W			
### 22   2892   2892   2894				W 6200		一日 とうしん にしのかなが
### ### ### ### ### ### ### ### ### ##	•	. 6083	9.6 .6083	22.6 8.6 .6083	45.0 22.6 8.6 .6083	34.7 45.0 22.6 8.6 .6083
### 1994   242   243   244   243   244   245   2	•	4060	******* 1.50F41	28. 9 10782.1 S704	46.0 28.9 10702.1 .5704	
10.00   10.0	10 an	3320	•	22.6 6293.6 3324	46 0 22 0 4243 6 3324	46 0 22 0 4243 6 3324
### ### ### ### ### ### ### ### ### ##			1467 7 2004	22 4 1467 7 DOGS	A	11 1 4 6 6 6 16 17 17 17 17 17 17 17 17 17 17 17 17 17
### ### ### ### ### ### ### ### ### ##		1248	2030 3 .1248	22.1 2338.3 .1248	42.9 22.1 2338.3 .1248	32.4 42.9 22.1 2358.3 .1248
10.2   60.5   40.5	•	. 1043	1978.7 1048	21.0 1975.7 1045	42.0 21.8 1975.7 .1045	31.8 42.0 21.8 1975.7 1045
18	•	1090	2061.3 1090	21. 5 2061. 3 . 1090	41.1 21.5 2061.3 1090	31.2 41.1 21.3 2061.3 1090
### ### ### ### ### ### ### ### ### ##	50 50		1965.7 .0564	21.4 1065.7 .0564	44.7 21.4 1065.7 .0564	20.9 40.7 21.4 1065.7 .0564
### ### #### #### #### #### #### #### ####	•		1030 B 0601	741.3 1090.3 .0577		30.6 40.2 21.3 1090.3 G.0577
### ### ### #### #### #### #### #### ####	•		1680	21.1 1644.3 .0891	39.5 21.1 1684.3 .0891	30.2 39.5 21.1 1644.3 .0891
943         600         487         487         469         482         927         948           931         987         474         474         474         482         953         965           938         987         969         909         480         487         474         832         955           946         987         969         909         480         487         487         853         965           494         987         494         478         476         482         967         978         967           496         987         494         478         472         482         967	•	•	1156.8 .0612	20.9 1156.8 .0612	39.1 20.9 1136.8 .0612	29.9 39.1 20.9 1136.8 .0612
#### #################################	508	•	1186.1 .0627	20.8 1186.1 .0627	38.6 20.8 1186.1 .0627	29.6 38.6 20.8 1186.1 .0627
#13 #371 #313 #314 446 468 #91 #42 #371 #313 #314 #315 #315 #315 #315 #315 #315 #315 #315	•	•	642.9 .0319	20.6 643.9 .0319 .	38.4 20.6 642.9 .0319	29.5 38.4 20.6 642.9 .0319
### 1959   1969	•	. 0324	612.2 .0324	20.7 612.2 .0324	39.2 20.7 612.2 .0324	29.3 38.2 20.7 612.2 .0324
427 386 436 476 477 488 462 474 483 365 476 476 470 482 365 365 476 476 470 482 361 365 476 470 482 361 365 476 470 482 361 362 476 470 482 361 362 476 470 482 361 362 470 482 361 362 470 470 470 470 470 470 470 470 470 470		. 0661	1249.0 .0661	20.6 1249.0 .0661	37.7 20.6 1249.0 .0661	29.1 37.7 20.6 1249.0 .0661
494 0567 0566 1506 470 482 0512 0567 0569 0569 0569 0569 0569 0569 0569 0569	•	.0337	637.0 .0337	20.5 637.0 .0337	37.5 20.5 637.0 .0337	28.9 37.5 20.5 637.0 .0337
494 6858 494 494 494 476 482 561 579 540 550 550 550 550 550 550 550 550 550 55	•	05. 8890. 7	1299.7 .0618	20.4 1299.7 .0618	37.0 20.4 1299.7 .0688	28.6 37.0 20.4 1299.7 .0688
140   140   141   144   142   142   153   1564   142   153   1564   143   153   1564   143   153   1564   143   153   1564   1564   15	•	•		20.3 664.1 .0351	36.8 20.3 664.1 .0331	28.5 36.8 20.3 664.1 .0331
820 520 520 520 520 689 464 477 546 556 556 556 556 556 556 556 556 556			1336.5 0718	20.2 1356.5 .0718	36.3 20.2 1356.5 .0718	28.2 36.3 20.2 1356.5 .0718
404 568 405 405 505 473 473 543 574 574 575 574 575 575 575 575 575 575	•	.0367	693.0 0367	20.1 693.0 .0367	36.1 20.1 693.0 .0367	28.0 36.1 20.1 693.0 .0367
495 559 495 527 495 462 469 546 591 478 542 542 542 478 478 478 578 549 568 496 559 559 464 477 477 549 661 516 516 516 516 449 476 482 556 661 499 499 499 499 499 465 486 662 491 491 491 491 491 481 561 568			743.1 0372	20.1 703.1 0372	35.9 20.1 703.1 0372	27.9 35.9 20.1 703.1 0372
478 542 542 542 478 478 478 549 588 588 586 586 586 586 586 587 547 547 549 661 516 516 516 449 470 477 558 661 570 577 578 588 661 578 578 588 578 57			713.7 .0378	20.0 713.7 .0378	35.6 20.0 713.7 .0378	27.8 35.6 20.0 713.7 .0378
496 529 529 464 477 477 549 601 516 516 516 449 476 482 556 603 507 507 507 419 480 487 568 602 499 499 499 499 469 465 466 479 568 491 491 491 491 491 481 484 561 568		9 0383 .505	724.9 0383	20.0 724.9 0383	35.4 20.0 724.9 0383	27.6 35.4 20.0 724.9 0383
516 516 516 516 449 476 482 556 603 507 507 507 507 449 480 568 602 499 499 499 499 499 469 465 486 479 568 609 491 491 491 491 491 481 684 561 568	502		736.2 0389	19.9 736.2 .0389	35.2 19.9 736.2 .0389	27.5 35.2 19.9 736.2 .0389
307 307 3507 5507 439 480 487 568 602 499 499 499 4599 465 486 479 568 609 491 491 491 491 491 484 561 568			1508 0 0798	19 8 1508 0 0798	34.7 19.8 1508.0 0798	27.2 34.7 19.8 1508 0 0798
499 499 499 499 465 486 479 568 609 491 491 491 491 481 581	•	7 .0408 .50	771.7 .0408	19.7 771.7 .0408	34.5 19.7 771.7 .0408	27.0 34.5 19.7 771.7 .0408
185 195 484 484 164 164 164 164 164 164 1	•	•	765.5 0416	19.7 745.5 0416	34.2 19.7 785.5 0416	26.9 34.2 19.7 765.5 .0416
	303	1 .0422 .50	798.1 .0422	19.6 798.1 .0422	34.0 19.6 798.1 .0422	26.7 34.0 19.6 798.1 .0422

Table 12B — Inferred Pressurant Distribution, Scaling Run 33, Test Configuration 2: Two 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

Table 13A - Scaling Run 34, Test Configuration 2: Two 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

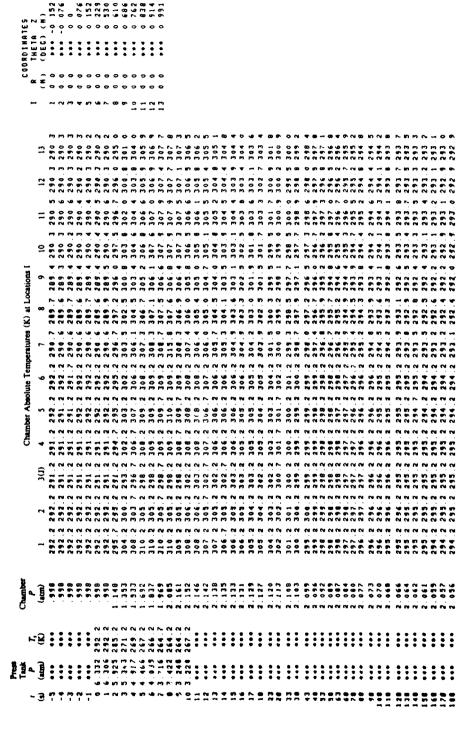


Table 13B — Inferred Pressurant Distribution, Scaling Run 34, Test Configuration 2: Two 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

										Pressun	Pressurant Fractions (X) at Locations	ions (X)	it Locatio	I suc					
~ 3	<b>⊷</b> ĝ	<b>ન</b> .ઈ	<b>*</b> ,5	90.	9/8	lbę	-	2	3(7)	•	~	vo	1	90	۰	02	=	2	2
COMMEN	CE VAL	4E 0PE	EN ING																
•	17.7	17.7		0	0.0040		00.	000	000	000	000	000	0 000	000	000	000		000 0	
• :	17.0	17.	•	44339.3	-7.0292	000 -	- 026		- 970'-	- 950 -	- 950	026 -	0.56	139	029	- 026	029	. 029	0.26
VALVE	-	= .	;							;					;				
~	4. 22	55.6	20	79.1	9.8291	•	*69		2.315	.634	. 891	- 168	581-1	- 593	-818	_	- 628	. A 38	034
•	<b>58</b> .3	30.7	*. 00	16.3	2.3547	•	060		•	195	195	. 291	. 61.1	0.11		- 038	146	533	214
•	-	36.3	20.3	10.0	1.1446	•	. 172	453	<b>6</b> 27	. 20 B	.234	297	. 203	234	297	- 584	303	322	309
•.	33.2	9.0	21.2	<b>9</b> .	7943	379	. 249	208	818	301	301	7.33	1117	2 96	363	335	348	368	368
4 0 MM 4 9	33.8	42.8 21.	21.8	<b>•</b>	7562	•	333	. \$73	. 629	333	363	263	.349	939	397	373	407	397	392
	34 2	֓֞֞֜֜֜֝֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֡֓֓֓֓֡֓֓֓֓֡֓֓֡֓֡֓֡֓֡֓	22 ,	•	****	797	300		• • •	3.66	• 1 •	;	24.2	-	6 2 3	;	£ 2.3	4.1.2	;
																	, ,		
		•		6.000		•	76.		2				:	7.		,	•	,	•
•	33.8		22.7	-3246.6	.5147	513	. 472	648	. 913	430	4.30	472	111	438	472	9 / *	472	476	467
	12.5		<b></b>	9.9061-	2072			. 993	\$E 2	E 6 + .	300	300	.462	4 8 1	4 8 1	4.94	6.6.4	486	4 8 6
11.	7 10	42.1	21.7	-935.6	E0 + 1	513	900	383	ī • •	437	98+	911	£ 9 3	4.93	303	313	503	303	486
12.0	1.15	£1.3	7. 7	E. 9E9-	1040	. 51	900	376	229	92	523	005	480	08+	4.0	313	300	•	£ 80 £
13.	30.5	•	2.1.2	-614.0	7001		ELV.	878	. 682	473	523	52.5	894	479	134	305	469	* 6 *	6 . 4
• .	10.1	39.7	9 . 7	-533.9	.0846	.51	. 483	. 363	.643	458	311	511	424	485	301	338	211	301	479
• •	50	6.0	20.	-366.3	1000	5	964	50 C	209	*	-	867	485	498	7	5 5	E 0 0	-	2
				0.01	6660	ē.							7 6	7	9 6			7 -	B 4
	2 2		0 0	- R. P.	0.52	7 6				2 2	7	9		4 4 5	7 (B)	7 kg	) M		4 7 55
13.0	7	37.7	20	-200.6	0318	15	467	323	283	467	5.5	4.96	6.24	06.	245	\$ 6.5	06.	325	4 7 9
<b>3.</b> .	28.5	37.3	20.3	0.604-	064	. 31	202	203	364	446	303	500	493	511	346	599	4 9 3	523	470
- 7	38		70	-419.9	9990	5	-	410	***	434		=	9 .	350	9	909	964	356	472
2 2 2		9.95	~ <	-214.3	0.75	S	9 1	326	226			3	705	5 1 4 5 1 5		9 7	4 4	3 5 5	472
	27.7			. 644	700		90.	967		7.		•	32.1	2 2 2	8 8 4				2
	27 4	er:	- 61	E 950-	0723	5	299	530	0	467	530	299	9.5	0.5	569	6.13	4.86	£0.0	4.0
	27.4	en En			0000	•	4 8 6	2.0	518	434	510	9	530	524	283	209	98 -	498	9 5
	27 . 1	0 5	19.6		.0745	5.	510	910	210	. 45	510	310	336	330	369	601	184	497	4 5 2
	27.0	34.		-240.4	0381	16.	764.	. 497	0.00	7 9 7	930	26.0	336	523	583	589	471	<b>49</b>	4.3.1
	26.9	34 3		-244.1	0387	5	•	244	247	084	247	0	950	514	267	287	467	0 8 7	447
	26.7	34.3		247 8	0393	51	. 473	340	340	679	.540	473	533	520	295	591	473	£ 6 3	459
	9.92	7		-251 9	0399	. 51	. 522	322	522	434	556	525	525	208	556	577	4 7 4	481	447
	56.4	33.8		-235 9	0496		510	. 310	510	310	578	٠, د د	217	310	33.	579	462	476	4 4 2
	26.3	33.6		-260.3	.0413	3.	503	203	303	303	573	303	533	512	334	368	£ 9 #	<b>4</b> 8 <b>4</b>	6 7 4
34.0	26.0	33.5		_	0846	,513	493	96	493	E 6 +	364	493	529	205	550	264	471	984	457
××																			

Table 14A - Scaling Run 35, Test Configuration 3: Three 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

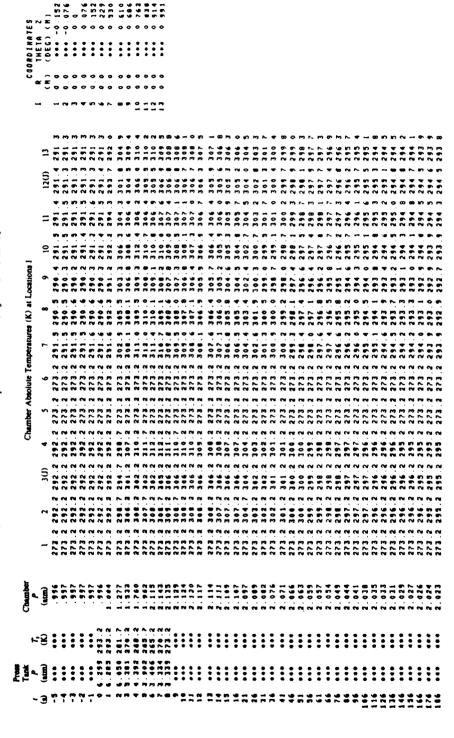
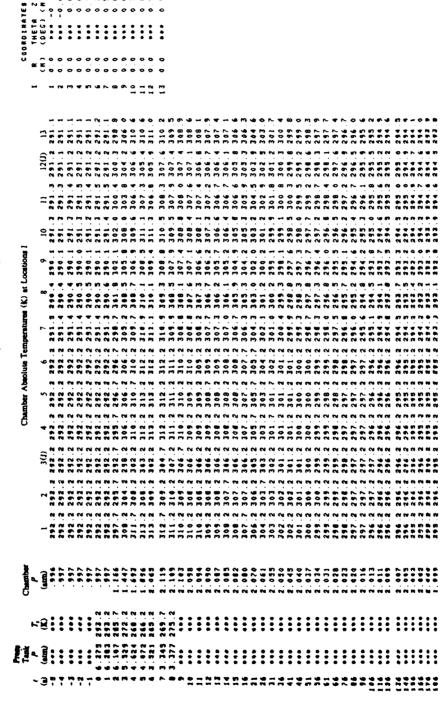


Table 14B — Inferred Pressurant Distribution, Scaling Run 35, Test Configuration 3: Three 2.54-cm Nozzles {(J) indicates thermocouples on an inlet jet centerline}

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- 3	<b>~</b> ₽	⊷ĝ	κĝ	•	<b>9/</b> 0	*	-	7	30	•	~	•	7	••	•	2	=	12(1)	13
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1111	FILLY	<b>IPE</b> K																	
	25.2	22.6	20.8	42.7	9.1527	198	4.72	-	m		•	٠	3-1.937-	m	-2.53	-3	~	ï	ď
-	15.7	26.4	20.3	M 74	2.9458	324	1.76	٠		•	1,765	_	765 - 271	1 - 395	•	1321	1 - 062		i
	27.2	32	70.7	4 E1	1.7776	408	1.515		6 .672		-	-	5 - 12	•	1			82 1	- 095
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	. ~	7	707	1.821	9893	205	1.459	8017	8 739	950	-			_	660		358	***	
34146	FRLLY	CL 88E9					1												
~	27 4	34.6	20.6	28.2	1367	514	1.468	•		•	994	1.468				0 13			
-	26.3	33.0	19 9	39.8	.2196	314	1.512	•	_		1.512	1.512	2 123		169	9 169		٠	
•	25.4	7	7.61	32.1	1784	514	1.54		•	•	-	-	•						
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7	73	21.1	18.1	20.0	1110	314	1.613	,			-	1 613				9 216			
7.	22.9	20.2	17.9	20.9	. 1161	514	1.622		•		-	1.622						4 . 253	
11.	3. 6	27.8	17.7	14.5	0803	314	1.620				***	~			700				
16.0	22.3	27.4	17.3	15.0	.0832	514	1.633	3 .117	7 .218	. 117	1.633	_	3 127		•	•	9 208	•	148
17.0	15.1	27.0	17.4	15.5	0980	\$14	1.62		•		-	1.626							
-	21.0	26.6	17.2	16.0	0892	514	1.630	·	•		-	_	1111	1 132	196		1 185		
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36.0	19.4	4.1.4	B . A	11.7	2496	\$14	7 531	E .	•	í	2 53	~		í			82 - 9	ı	,
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31.0		19.7	0 87	13.0	0723	\$14	€ 659	ì	656 - 6	959	+ 959	4.859	9 - 784	006 - 1	ď			ï	
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33.0			10.0	14.2	.0791	\$14	906	082-2.63	631-2.631-	~	9 082	80 6	082-2 16	162-2.162	-	,	405-2.397	7-2 045-	1-2 279

Table 15A — Scaling Run 36, Test Configuration 3: Three 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]



Commerce Value (Compared Compared Compa		12(1)	,	0 F	•	31	111	439	612	623				340	4.4	15.0	328	334	933	986	9 60	320	521	217	220	30.9		8	191	2 6			
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CO   CO   CO   CO   E   Main   F   1   2   3(J)   4   5   6   7   8   9   10		_	:	0 6	2	318	397	÷	4 4 2	::	6	, ,		33.	9 6	3 6	213	308	217	9 6	905	203	504	4 6 4	96		~	7	472	2	4 7 4		
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CO		•					141	=	930	:	416		•	490	000	200	31.0	323	533	200	2,4	366	368	376	4 / 5	0 .	2 7 3	795	26.0	237	975	,	,
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THE CO. (C)				9 1	•	7		7	•	•	•		, <b>.</b> ,	•		, 61		•	•	*		•	•7	•*	•,	•		• ?				•	
THE CO. (C)				0 "	2	38	9.1	5	19	29	•	, ,		:	2.	• •	: ;	14	72	<b>5</b>			25	63	<b>:</b>	47	9	30	E -	٤;	• •	. 7	
THE COLOR OF THE C		9/	;	0 V		5.72	2.40	1.17		•			) P	=		- 6	0	•	0	9	9	6	0	90	90.	E 0	. 0	0.	8	3	0 6		
(C)		•						•	•	•	•	• •	•	•	•		•	~	•	<u>-</u> :	v 0	•	•	<b>.</b>	-	•	PO -	<b>.</b>	en e		<b>»</b> "		
(C)						÷	Ξ	_		36.28			90	-643	200	200	-203	-316	-2161	-221	7 6	360	-123	-251	-2363	-131	-269	-277	= :	-	234		
(C)			٠	- :		^	•	•		-			. ~	-		•	•	^		٠,	• ^	•	_	-	~	•	_	_		٠,			
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Table 16A - Scaling Run 37, Test Configuration 3: Three 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

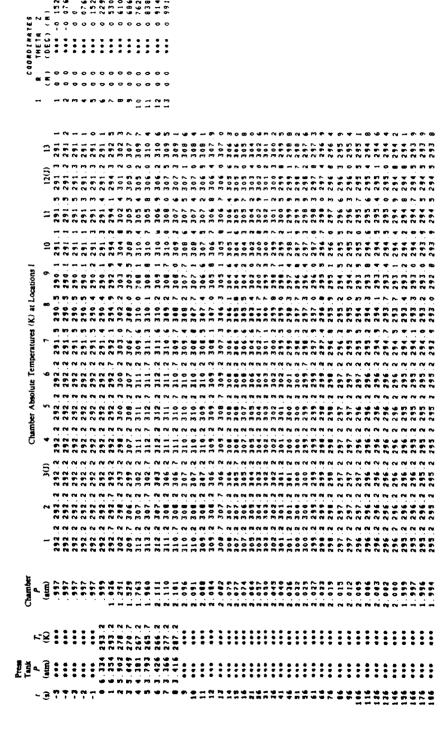


Table 16B - Inferred Pressurant Distribution, Scaling Run 37, Test Configuration 3: Three 2.54-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

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18 CL 81	LESURE															;	
<b>4</b> 7.0	23.8	• ·	. 8269	664	329	996	. 711	350	350	393	376	382	458	398	613	396	÷ 0 5
<b>1</b>	24.5	29.3	.6362	497	416		. 788	•	416	416	408	425	458	434	602	623	m <b>*</b>
08E9																	
~	24.1	•	.0203	264	164		.639	•	451	451	£ 4 3	094	9.	464	3.5	364	476
7.9	23.5	8	. 1915	497	424	•	9.	•	4.54	<b>†</b>	463	463	481	481	5.55	260	476
12.1	23.1	2	.1131	497	460	•	965	094	094	9.9	460	694	478	492	546	23.5	4 8
0	22		1118	497	054	•	183.	•	450	4 30	478	483	497	492	344	554	4
4	22.6	M	.0739	497	1	926	925	٠	4 8 0	432	475	087	504	519	5.38	543	4 80
42.3	22.3	4	1020	497	4.53		603	•	455	4.55	0 2 1	475	519	534	534	544	46
2	22.1	4	. 0326	497	436	•	•	•	456	ĩ.	486	984	532	557	516	5 4 5	9 ₹
~	22.0	<b>P</b>	0811	497	434	306	. 558	434	454	4 5 4	480	420	532	268	206	537	495
7 0	22.5	9.8	0535	264	164	٠	,		434	434	462	4.8	230	285	519	547	496
=	23.4	Ф. 177	.0817	497	737	•	•	•	194	407	452	438	521	591	309	240	4.8
~	23.0	2.7	. 0588	497	. 481	•	•	•	8 7 7	415	. 461	4 4 8	240	286	205	553	4 6
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32.3	24.0	₩. M	.0735	497	487	487	487	487	427	367	487	499	296	999	487	533	4 3
9	24.0	1 . 7	.0376	764.	474		474		4 2 4	350	487	424	637	289	462	337	9
~	24.0	8. 1	.0382	497	4.38	٠	438		4 5 8	328	5 2 5	509	639	<b>8 2 8</b>	473	8 + 5	4 8 4
*	24.0	1 8	03.88	497	424	•	164	•	424	454	532	4 7 8	9 2 9	089	451	332	4 9
	54.0	9	.0794	497	386	386	532		386	386	576	488	649	8 2 9	0 7	\$35	503
	24.0	6	0407	497	370	•	. 522		370	320	5.8.3	92+	629	069	4 4 6	553	53,
	7	•	0413	497	473		477		423	212	8.75	6.0	. 1.2	6 7 9	4 0 4	4 2 3	
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Table 17A - Scaling Run 39, Test Configuration 3: Three 1.52-cm Nozzles [(1) indicates thermocouples on an inlet jet centerline]

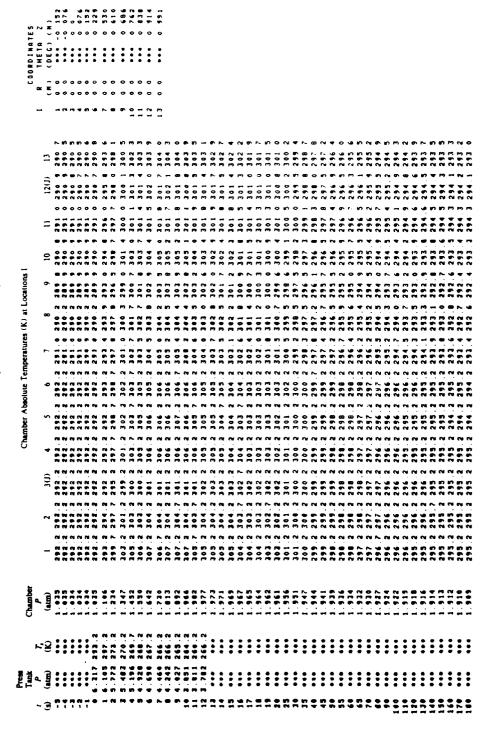


Table 17B — Inferred Pressurant Distribution, Scaling Run 39, Test Configuration 3: Three 1.52-cm Nozzles {(J) indicates thermocouples on an inlet jet centerline}

	::	:	E 0	230	316	326	377	424	436	,	2 4 4	45.5	436	<b>*</b>	7	27		£ 4 3	9 7 4	, 4 , 10	0 FF +	432	4 18	4 2 3	4.25	414	420	423	4 18		4 2 8
	12(1)	922		9 6 Z	380	487	¥ 6 ¥	5 4 5	009			\$ 2 8	<b>5.2.8</b>		200	8 4	474	£ 9 3	0 10	7 9 9	436	432	4.2.5	4.00	417	459	412	413	0 <b>:</b>	7	•
	=	0000	901	323	398	492	531	260	0 0 9	**	9 7	2	528	213	205	¥ 8 4	4 7 4	E 9 9	# <b>4</b>	9 6	4 4 5	432	418	4 2 3	405	399	397	404	405	398	412
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S on an mer jer centering	· '	100	980	223	300	319	345	366	377	•		4 2 6	426	0 M T	4 ·	7 7	:	9.6	* *		*	432	•	* ID *	4.0	431	4.58	9.4	E /-	6	7
II mile	9	9 0 0 0	146	536	328	319	9 30	361	393	478	=	80.	396	7.	4 .	7	4 2 9			-	421	366	***	*	4 2 3	<b>1</b>	4 > 3	<b>;</b>	÷	9 :	**
2 00 8	۶	0 000	146	236	272	319	3	335	393	,		0 0	426	964	-	4 4	4.2.4	4 7 6	7	=	451	194	<b>+ 3</b>	~	-	į	473	461	-	1	9. +
ordno	•	1.382	4	33.0	272	319	326	387	393	3.7.8	-	804	396	9.7	-	4 4	420	-		=	451	. 467	434		<b>†</b>	- 48	473	197	-	7	**
	3(3)	985		89			622		6.38	243	286	323	316	•	000			•			•	•	₩.	• • •	8	÷	473	194	÷	9 ;	9.
alcs u	7	0.000.0	•	2.0		-			499		9		٠	•		4 4 5	•	•			•	•	•		•	•		٠			436
	-	0 000	660	13.	. 181	292	303	333	340	507	411	408	396		413	327	138	•		-	4 2 1	194	***	~ *	423	=	397	383	+	977	4 16
THECT 1.22-VIII INCERTED (13) INCHREGO MECHIOCOUPIES ON AN INIET JEL CENTERINE.	Pet	000.0	143	9 9 9	302	375	₹ 03	428	0 12 0	55.7	4	80 <b>4</b>	4.55	5.0	P 1		80 ¥		n en	884	80 T	684	10 T	664	60 T	¥ 22	453	455	5.5	10 I	DR V
1.32-20.1	9/8	0.0000	3.2064	666	6320	6512	5778	5195	.5551	65.6	1574	1333	0695	. 0719	91.0	0 3 6 6	88.20	0467	0 4 2 1	£ 9 8 0	0443	00000		0000	0 4 68	0477		00000	1002	0516	0 0 0 0
	•	7 8 7		6.21				12.3		•		7. 7.	7. 7.	~	~ :	•	PO .	۰. ۱		-	~	0	<b>.</b>	0	•	<b>60</b>	•	0	-	•	0
	<b>~</b> .6	N ING 61.3 22.0	20.4	181	19.1	19.6	20.02	9 5 20 5			30		19.9	-		13	1.4	6:		1.61	19.1	19.1	19.0	67	18.9	#. @_	-	10.0	2 9 5		• ·
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	<b>₽</b> ĝ	2 '	24.7	. E	30.0	= 1				FULLY 340.7		29.3	29.0	7.0	7 .		37.6	27.1	27.2	26.9	26.7	<b>26</b> . 7				<b>56</b> . 1	92	56.0	~ i	500	7.67
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Table 18A — Scaling Run 40, Test Configuration 3: Three 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

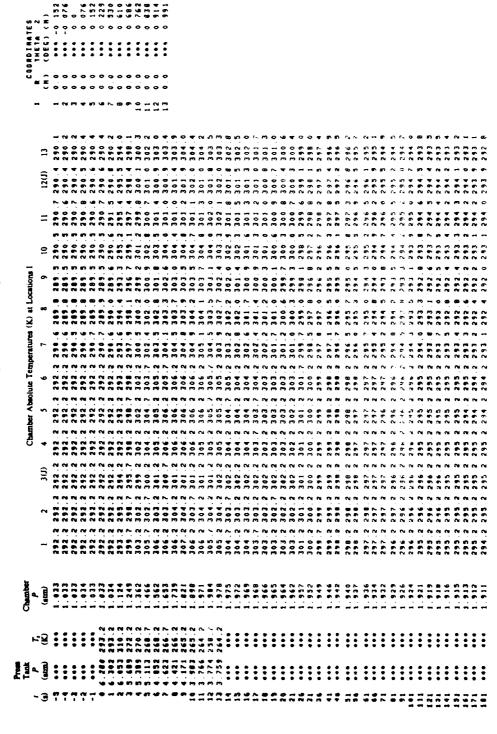


 Table 18B — Inferred Pressurant Distribution, Scaling Run 40, Test Configuration 3:

 Three 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

	13	1 4 3	162	294		281	319	3 4 2	378		9	0	;	4	4 2 9	432	425	4 4	447	451	459	471	466	473	4 2 6	4 80	<b>*</b> 8 <b>*</b>	4 7 6	483	4 20	485	4 7 8	697	472	4	* *
	12(J)	000	320	348		426	478	167	304			F 80 F	,	9	978	503	433	200	505	496	492	492	493	486	483	4.6	¥ 8 ¥	 ₩ ₩	484	425	474	478	924	472	<b>-</b>	99
	=	0 000	296	230	,	-	478	322	547		3 2	3 7 8	į	23	313	515	505	205	4 9 8	0 6 4	984	422	4 6 6	452	455	4 2 2	4 2 6	4.54	4.5.4	07	436	4 4 7	4 38	433	=======================================	4 2 6
	01	0000	296	783	7 7 7	2 0	583	319	340		36.	3 / 8	:	-	433	4 3 2	450	475	4 8 6	422	492	497	4 9 3	205	511	537	252	519	532	537	550	244	539	551	245	80 80 80
	•	0 0 0 0	187	- 622	777	000	313	3 4 2	326		372	383	:	<b>4</b> 0	459	426	437	456	4 1	457	459	471	479	473	483	485	<b>+</b> 8 <b>+</b>	9.4	491	482	488	309	492	496	464	<b>4</b> 9 0
tions 1	40	0000	2.2	366	·	262	295	325	336		361	2 <b>2</b> 2		50	433	38	52	3.5	35	25	420	37	445	45	448	459	<del>-</del>	439	9 +	8 •	:	447	4.5	457	33	42
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<b>X</b> (X)	1	0000	0	- 022	717	7 6 8	293	31.9	23		367	~		66	Ť	÷	7	45	5	. 412	433	4.5	438	4.	4.	459	45	447	<b>¥</b>	Ť	4.5	Ť	<b>4</b>	45	9	<b>*</b>
Fraction	٠	0000	193	630	261	2 2	289	313	336		378	<b>*</b> 6 E		Ŧ	423	396	431	418	403	•	433	417	397	4 4 5	. 427	416	398	0.7	432	403	429	4 3 3	438	433	413	4 6 5
Pressurant Fractions (X) at Locations I	~	0 M	153	356	261	25.5	260	313	356		378	394		<del>-</del>	£ 5 H	4 2 6	431	<b>4</b> 1 8	435	; ;	433	417	99+	445	427	<b>4</b> 16	4 7 0	244	432	.422	467	4.5	4 3 8	433	+ 3+	4 8 2
£	•	0 F 0 F 0 F	- 422	630	192	2 2 2	96	313	326		376	=		438	423	455	431	418	433	:	433	417	994	4 4 3	457	416	470	~++	432	47.2	467	455	438	433	455	485
	<b>9</b> 0	0 6 F	32 -	686	2 5			396	659		619			. 25	396	574	554	545	330	509	199	184	994	445	. 261	487	470	447	432	477	294	435	<b>438</b>	<b>433</b>		704
		•	ı,	-	•	•						•		•	•		•		•	٠	•				٠			•		•	•	•			_	~
	7	0 M	•	138		2.00			7		213				401		492		462					•	427	•			432	٠	391	•	. 43		•	9
	-	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	- 153	103	0.0	* * *	2 60	313	301		378	394		411	4 2 3	426	431	418	433	111	433	417	397	443	. 427	416	398	442	432	403	391	378	438	433	415	4 0 2
	₽ĸ	000	.072	1.53	216		. A.	30	Z 0 V		164	4.33		~ P +	<b>~ 12</b>	497	437	4.3.4	457	437	454	4.57	457	457	457	437	437	4.57	457	457	437	437	457	457	484	.457
	9/6	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	1.6253	3.1978	4068	D 4 0 4	7.20	6143	5474		5431	5005		1395	1863	0880	1039	1084	0372	.0761	0390	9660	0811	0413	0423	0640	0438	0445	0453	0461	0450	0479	0413	0498	00000	0.00
	•	- N		•			, o		2.1		3.1	710.1		98.3	267.6	8	2 2		5.9		53.4	10	M	6	7.0	-	62.2	63 2	•	9.5		-	8	8 02	•	5.3
		4	-																																	
	r.6	H IN C		23.3						<b>BSURE</b>		20.8	_																					1.8		
	r.Ĉ	VE OPE 18.0	2 E X	28.2	29.9	7		2	3.8	_	39 0	39.3	CLOSEI	39.0	37.7	37.0	36	33	35.4	34.9	34	4	34.0	33.7	33	33	33	32.8	32.6	32	32.1	31.9	316	31.4	31.4	31.1
	<b>~</b> €	18 VAL.	#LLY 20.8	24.9	2.7 B	29.4		9 0	31.1		910		HLLY																					15.6		
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Table 19A - Scaling Run 41, Test Configuration 3: Three 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

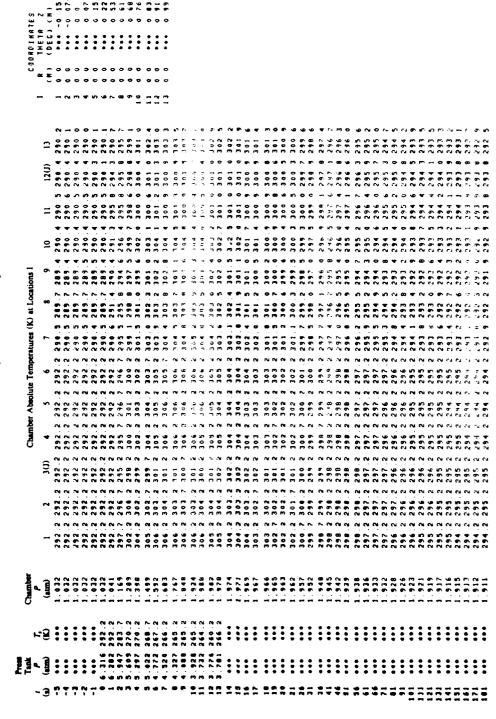


Table 19B — Inferred Pressurant Distribution, Scaling Run 41, Test Configuration 3: Three 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

	•	•								Ē	seurant P	Preseurant Fractions (X) at Locations	X # Z	cations l					
-3	-6	. <u>6</u>	r.Ō	92.	9/8	æ	-	7	30	•	~	•	7	••	•	9	=	12(1)	=
CONMENCE VALV	E VAL	9	3 :			•		3									:		
•		-		- 638	90000		430-	- 0 E F	100°0 000°0	929		- 019		9 9 9		0000	0 000 0	000	913
VALVE F	711	IPEN		!		:		:		• • • •	•	•	:	:			•	•	
~	22.0	23.2	5	19.1	6.0618	102	E90'-	240	694	545	240	240	- 880	245	-	. 215		- 124	0.93
•.	26.3	28.0	=	18.4	1.5768	921	010	223	4 2 8	223	120	. 223	161	110	212	680	212	121	1 20
•	26.3	31.6	7	13.8	1.0302	.235	120	. 26 J	477	. 263	192	. 263	. 192	170	249	149	. 291	242	192
•	29.4	33.9	=	13.3	.8749	.284	191	34	. 536	. 254	. 223	282	. 223	216	279	210	373	123	235
•	30.3	33.9		11.8	6229	.324	. 233	403	.520	290	290	. 290	. 267	. 261	302	. 250	423	193	290
~	30.7	37 2	19.0	12.4	6748	360	294	E 0 7	268	294	294	321	. 299	288	327	294	491	469	338
•	30 7	30.0	13	13.1	6329	390	328	484	596	328	328	328	322	328	344	322	505	200	355
•	30.8	38.7	13	12.5	.5575	. 417	361	131	.652	36.1	361	3.6.1	343	356	351	340	5 \$ 2	499	382
COBRENC	EVAL	13 3	BSURE																
0 0 7	70.7	330	20.2	13.6	. 5532	440	378	538	. 644	378	378	378	341	367	383	378	296	559	399
0	30	39.0	2		. 4827	438	<b>98</b>	192	. 708	438	384	384	167	394	00	405	009	583	4 2 1
VALVE F	4110	CL 0SED																	
12.0	30.2	3 6	20.	•	.0249	437	422	477	614	422	423	422	383	4 0 5	452	4 3 3	5 2 9	531	433
13.0	29.6	37.6	2	25.1	.1271	487	407	197	. 378	. 407	+ 9 +	405	405	419	430	447	550	527	4 4
0.4.	29.0	36.7	:	26.35	.1339	437	439	5	.558	.439	439	439	<b>10</b>	86.0	428	434	5 2 8	505	4 3 4
.3	28.5	9.9	5	20.8	E801	784	0 7	491	.552	430	430	430	114	417	4 8	454	515	497	442
16.0	28.2	35.6	2	14.4	.0728	437	. 416	4 7 B	240	416	4 7 8	416	422	4 2 8	0 4 4	459	515	490	4.4
17.0	27.9	35.1	5	14.8	.0750	457	453	482	517	453	453	£ 2 3	415	4.2.1	447	453	4 9 1	466	434
• =	27.8	34.9		9. 2	<b>986</b> 0.	<b>₹</b>	438	E 0 5	267	438	438	438	419	419	451	471	477	458	426
÷.	37.6	34.6	2	7 7	0389	484	. 433	486	331	453	<b>486</b>	421	421	421	447	453	473	453	427
20.0	27.3	34 2	19.2	15 8	2620	427	. 468	168	532	. 468	468	89+	421	<b>4</b> 0 8	455	8 <del>9 4</del>	7 6 1	=	4 15
21.	27.2	. G	5,	<b>4</b> .	.0409		438	. 191	523	438	458	85 +	417	424	131	471	4 5 8	431	454
22.	27.0	~ ·	2	<b>8</b>	. 0413	<b>LB+</b>	0 2 4	# F	518	430	450	430	. 423	416	464	0 1.0	4 6 4	7	4 2 9
53.	56.9	m (	£ :	<b>T</b>	. 0422	484	446		513	9	4 4 6	446	425	425	459	<b>4 8</b> 0	4 5 9	•	4 3 9
	2.92		= :	er (	0410	- E -	7 6 7	2	4			4 5 5	429	4 15	9		£ 4 3	4 3 6	4 3 5
2		9	-		0437	/E+	-	<b>e</b>		481	 	2	8 7	<b>4</b> 1 4	439	-	÷	7 7 7	4 1 2
2 .	97					~ P	9 ( 7 ;	25	20.0	9 6	9 0		9 2	<b>1</b>	# T	4 8	415	0 0	
	, ,	, C		•	7				9 9				,	7 .			865		8 .
	6	7		N	0470	- No.									,		•	7 0	2
34.0	25.8	3.1.8	=	6	0479	487	467	2	245	467	294	29.	=	4.21	4 9 9	215	90	391	96 +
71.0	33.6	3 1 6	=	۸. •	• • • •	<b>4</b> 8 4	944	+18	41.0	¥ 187	.514	<b>₩</b>	437	904	8 9 7	66+	1 6 E	376	399
32.0	32.6	31.6	=	0	0.00.0	437	664	499	499	489	.499	422	438	413	468	~ o s	666	384	4
23.e	73 m	17.1	=	19.9	9001	764.	+ 40	130	490	64.	4 9 0	¥ 3	. + + 3	419	4 2 4	306	3 9 3	193	
7.	25.3	31.1	5.5	• •	0.000.0	487	•	480	•	480	480	•	=	4.25	884	304	-0	193	409
R X																			

Table 20A — Scaling Run 42, Test Configuration 2: Two 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

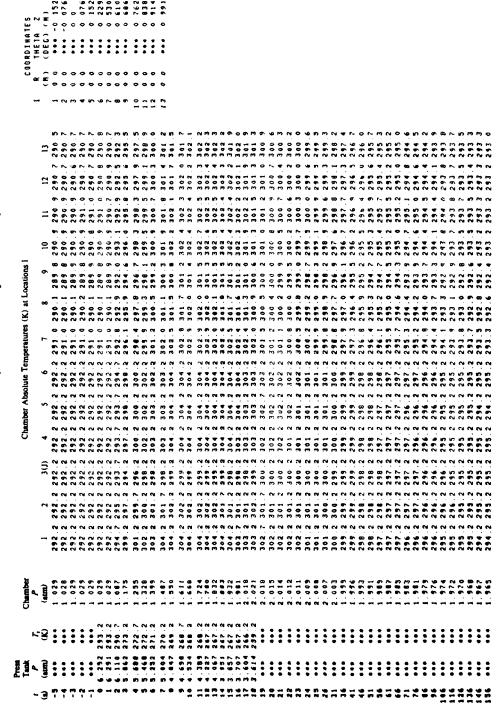


Table 20B — Inferred Pressurant Distribution, Scaling Run 42, Test Configuration 2: Two 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

			0	:	528	157	98	<b>4</b> 6	7.	9	24	<b>£</b> 3	20	29	e e	95	413		437	3.		128	191	291	:	478	0	897		7.	7.7	63	33	•	2	•	~ .	C
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	2	90	000		725	157	180	238	. 257	. 273	318	332	350	367	380	399	-		423	431		435	467	467	:	4.			4 2 2	487	493	<b>~</b>	477	. <b>48</b>	-			2
			• •	•		187	_	m	243	•	305	~	•	~	•	399	419		423	•		8.8	291	~	* 9 *	٠.	7	0 5		_	•	2	<b>\$</b>	<b>.</b>	984	<u>.</u>	٠.	-
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	2	•		•	7	-	_	~	~							-	•					•			•	Τ.							•	•		17 6	,,	
	•	9	:		3	141	=	231	237	280	305	313	331	348	380	386	393		397	417		<del>+</del> 5	440	-	436	4 3 4	-			-	909	-	-	<b>÷</b>	000	2 4	9	2
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3 F					93-	109	23	192	~	7	2.9	=	=	7	•	23	406		410	454		:	Þ E Þ	•	n * *	111	-		; ;	45.5	•	÷	433		436		3 :	ě
X)	1	9			•	٠	-	_	~	~	~	Ξ.	-		7	_	•					•		,		•	٠	•					•					
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Pressurant Fractions (X) at Locations	•	9	000		. 52	037	60		-	~	~	~	311	E.	M	37	F.		304	2		*	434	Ŧ	434	. 4.9	-			=		7		7	7	-	9	•
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	33	•	000		528	610	460	==	363	31	369	.600	628	653	673	693	. 705		.780	730		790	704	629	100	394	2		E	318	369	319	348	333	355	7		
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	à				5	2.5794	1.0926	. 1630	~	Ī	5	3	. 5374	.51	5125	. 4463	4718		4566	. 4628		3902	1039	1039	E	. 0372	0 7 6 1		0 7 0	0416	. 0 4 2 3	•	.0437	. 0 4 46		. 0 4 2 3		
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	6	1			~	•	~	٠	<b>-</b>	-	•	٠	<del>-</del> .	•	~	•	•	13	•	•	8 6 1																	
		W .		PER				29.6				34	3.5	33	Ë	36	7	34.	8	8	3	~	36	8	Ħ	<u>*</u>	~	3		2	33	33	2	32	77.5	ã i	= :	7
	ğa	NCE VA		FELLY		~	3.5	6.9	6.21	9.6	19.1	19.3	*	•	4.6	3.5	19.3	1 W.R.	19.2	9.6	11.1		19.2	2.		=				7	6.9	9.	•	6.9	56.3			•
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	-3	3000	-	VALVE	~	-	÷	•	•	~	-	•	=	Ξ	7	=		C		9	4164	- 2	=	19.0	÷	=	27			5 6	2	=	=			2 6		
		_		-														-																				

Table 21A - Scaling Run 43, Test Configuration 2: Two 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

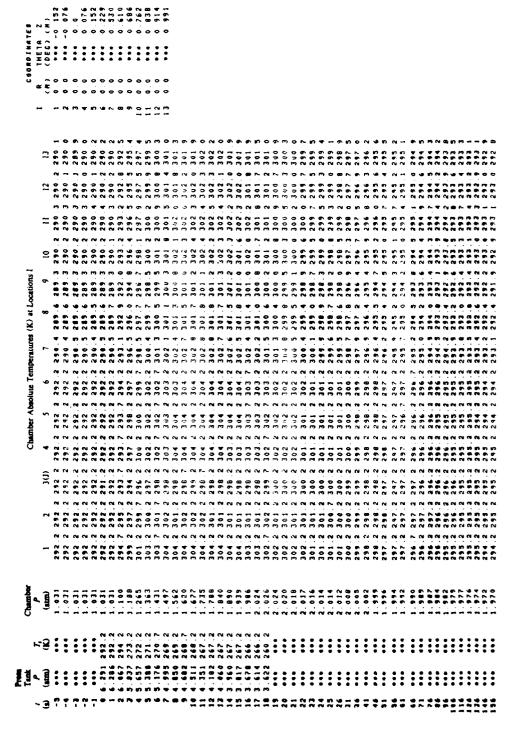


Table 21B — Inferred Pressurant Distribution, Scaling Run 43, Test Configuration 2: Two 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

۴.	<b>L</b> 2							•					,				
n	ē	<b>80</b> .	B/0	Pr.	-	7	33	*	S	•	1	<b>00</b>	•	2	=	13	=
-	EN 186	•					•	•	;	;		;		:		:	
	7. 6.7 6.7	2. B188	-7.0229	0	. 0 . 0		0 W		9 7	0 .	. 0 4 1	0.0	9 4 0	001	000	0 0	100-
•	;				•		,			,	;		;	1		:	
			36.44	9 -													- 2
		7	10146	•	E 70			15	1 2 1		121	1 1 2			121		
~	•	13.6	1.0624	213		. 329	479	. 179	179	179	. 187	172	232	6 2 1	194	202	232
2	17.3	13.4	7096	234		_	100	239	239	239	. 2 1 0	211	25.9	204	. 239	232	.266
	17.1	13.1	6313	206	. 209	٠	. 338	. 279	273	273	233	242	275	242	268	261	281
	18.2	13.6	6493	318	. 237		. 578	. 257	237	321	. 26 J	276	289	263	283	283	315
•	18.7	14.4	5073	339	303	. 429	386	303	303	303	291	303	352	303	328	303	322
	13.1	13.4	5273	361	331	٠	585	331	331	331	313	325	336	319	338	344	330
•	19.4	15.7	5331	382	332	•	6.33	352	352	332	333	346	363	340	332	352	359
	19.7	16.3	4944	10+	365	354	.681	363	363	363	346	332	371	363	338	358	365
13.7	20.		.4630	414	37	•	269	97E.	379	379	366	372	383	372	379	3.8.5	391
2 2	20.3	16.9	100	433	363	1990	7.09	450	369	8 8	9 - E	392	392	379	398	398	404
173	LVE CLESURE																
35.8	20.6	•	. 4222	448	396	293	.724	•	396	396	396	383	41.5	433	405	409	415
2		-1832.0	4324	194	463		731	£94	4 2 9	429	405	409	9 7 0	409	409	423	4 16
CLORED	-																
	20.8	-1559.1	3705	.472	4 58	•	. 732	438	438	4.28	410	454	424	454	111	424	437
	21.0	286.4	- 0681	472	477		611	477	477	443	443	443	450	4 4	4.27	443	457
87 87	20.8	-286.4	.0681	472	486	. 554	554	486	486	486	431	131	431	445	455	452	4 38
÷	20.6	-597.5	.1420	.472	468	•	539	468	468	4.6	9 + +	434	446	461	424	461	461
1.1	20.4	-312.0	.0741	472	424	•	. 327	434	4.54	4 3 4	454	462	469	469	469	469	469
-	20.4	-139.6	.0379	472	¥.	•	. 507	- 305	205	434	441	448	463	A 7 B	463	124	1 2 1
-	20 3	-162.1	0385	.472	. 4	•	487	487	<b>48</b>	487	445	457	457	+9+	46.4	464	464
33.3	20.1	-331.6	0788	472	477	·	477	477	477	477	447	454	437	4 8 5	469	477	462
33	20 . 1	0	00000	472	. 463	•	•	. 463	465	465	457	457	472	495	472	68	472
32.8	20.0	-342.4	.0814	472	434	•		454	404	*	454	40	4 7 8	509	4.50	984	478
32.8	20.0	0	•	.472	436		436	436	514	436	644	451	475	523	483	86₹	4 90
32.6	19.9	-175.5	.0417	472	453	•	+ 1 +	493	493	493	438	438	469	509	4.69	493	477
12.4	19.9	-178.5	.0424	472	. 42	475	475	475	475	475	7	4.35	467	515	459	483	483
2.2	19.6	7.181-	.0432	.472	100		+9+	494	+ 9 +	+ 9 +	447	439	472	528	08+	961	488
6.	19. 7	-184.7	0419	.472	4 3 6	•	456	456	456	456	440	4	684	530	489	497	513
7	19.7	-108.1	.0447	.472	443	•	. 443	. 443	526	443	. 443	432	484	534	484	501	509
	19.7	0.	0.000.0	.472	434	•	<b>†</b> E <b>†</b> .	476	517	<b>4</b> 3 <b>4</b>	451	<b>#</b> 9 <b>#</b>	* & *	550	<b>▼</b> 8 <b>▼</b>	200	500
-	•	7	****	422		707	•	•					,				

Table 22A — Scaling Run 44, Test Configuration 2: Two 1.52-cm Nozzles [(1) indicates thermocouples on an inlet jet centerline]

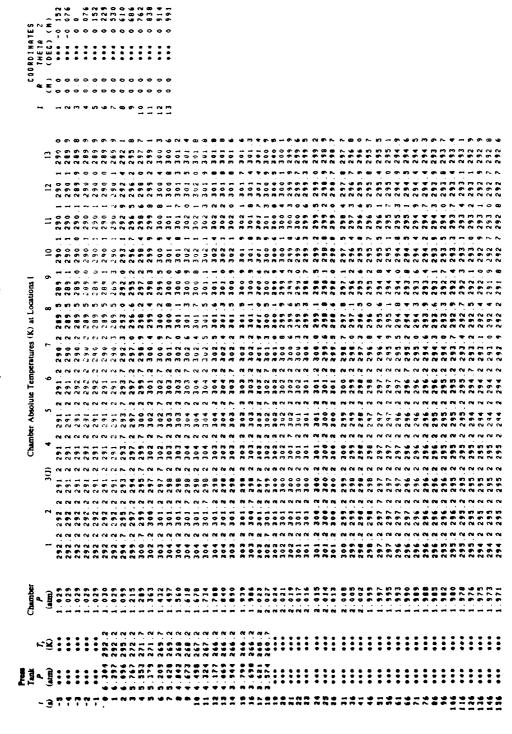


Table 22B — Inferred Pressurant Distribution, Scaling Run 44, Test Configuration 2: Two 1.52-cm Nozzles [(J) indicates thermocouples on an inlet jet centerline]

-3	<b>⊷</b> و	r.Ĉ	۳۰Ĝ	<b>0</b> 2.	9/8	be	-	~	3(I)	₹	essurant S	Pressurant Fractions (X) at Locations 5 6 7 8	(X) at L	ocations	٠	01	=	21	13
CONNENCE	CE VAL	VALVE OPEHING	E# 1 M G																
•	7. 6	17.4	26.6	23806.6	0.0000	000	000	000	000		000.0	0 8 0 0	0.000.0	9 800° 0	000	000	0 000 0	0000	800
VALVE	FILLY	-			ı														
~	7.02	20	20.5	136.7	7.7710	<b>450</b>	272		272			1-275		896	8 4 3	8 4 3	. 86E	720 -	943
• .	23.4	2 . 2	19.	37.8	7916.5		- 062	131	723	133	133	133		=		017	9 2 0	=======================================	174
•	23.4	27.2	17.3	16.0	8446	•	1.28	780	4 12 13	128	077	128	108	108	169	-	1 2 8	189	199
	26.9	29.6	17.2	14.8		.220	177	338	498	. 097	0 9 7	177	161	185	241	193	201	548	241
•	27.8	31.4	17	14.7			. 211	334	533	175	173	173	232	232	254	225	232	261	254
7.	20 3	32.6	17 7	15.2	6480		210	413	548	210	210	210	244	2 2 8	278	258	278	305	298
-	9 82	33.4	18.	13.5	•		238	+3+	584	328	258	238	271	284	290	277	284	310	303
9.6	29.0	34	18	13.8	4847		308	997	624	243	. 245	276	283	327	321	308	314	340	340
10.0	29.0	34 8	18	15.2	•		337	323	630	273	273	. 275	325	325	326	337	337	343	343
11.0	53	33	19.2	13.0	•	•	362	- 312	673	300	300	360	137	356	362	362	356	324	368
12.0	29.0	7.7	19.4	16.0	4977		374	282	289	374	312	315	355	368	374	353	368	393	380
13.0	28.9		19.7	15.7	4544	•	387	376	701	387	324	324	375	004	387	387	3 8.1	900	400
14.	2.0	33.3	19.9		6994	+8+	484	585	709	390	328	338	390	390	403	390	346	409	409
CORRE	CE VAL	LVE CL!	18 URE																
13.0	28.7	33.6	20.1	16	•	448	E94	592	722	398	396	3 \$ 8	398	398	~	4	398	454	<b>+</b> 1
16.0	28 5	3.5	20 3	-391.2	•	797	467	631	7.30	10	401	101	104	427	<b>†</b> [ <b>†</b>	421	4 2 1	447	440
VALVE FULLY CLOSED	FULLY	CL 05E	-																
17.0	29 4	33	20.5	•	3245		470	603	803	E 0 T	£ 0 <b>♦</b>	£ 0 ¥	453	430	436	443	4 30	130	436
16.0	29.0	36.3	20		1323		482	578	6 42	÷	417	<del>-</del>	4	449	443	462	437	462	449
19.0	38	33.7	50.6				. 500	366	266	434	¥ 3 4	<b>4</b> 3 4	74.7	094	<b>?</b>	467	<b>4</b> 3 <b>4</b>	467	097
30°	28 L		20.3	E. 56.			984	334	334	418	4 1 8	418	445	454	466	486	466	9 0 \$	4-13
22.0	27.8		20.7	-63.8			476	343	543		904	904	4 4 8	69	469	4 9 2	462	6 \$	476
22.0	27.5	4.2	20.1	-67.7			324	324	. 524	H 13 H	m m	315	433	453	460	<b>4</b> 8 <b>9</b>	460	- R - W	4 7 4
<b>5</b>	7. 4	33.9	2	9. 46-			. 510	210	2.0	438	434	438	438	432	467	493	4 7 4	495	467
7	2	7.1	6.6	10 ( 10 ( 10 ( 10 ( 10 ( 10 ( 10 ( 10 (			A .	0 L	A 6	80 I	P 1	50	686	T :	9 !	6	89 ·	•	9 / 4
	7	7		- 100 ·			E 2 T		9.4	M ( )		•	:						7
	76.9	* 0 * 12 * 12		N 45	95.0							7 7	• •		9 4	4 4 0	B 9		7
7	36	7	1.9	- 17			600	606	600	. <b>4</b> 3 3	4.3	433	7	4 3 6	471	501	98.	301	6 2 4
5.2	56 5	32	13.6	-38.0			3.0	101	304	457	457	427	43.4	437	481	304	437	496	<b>88</b>
3.0	5 e	32.4	19.5	- 38 -			* * *	•	4 9 4	417	4 3 3	÷17	433	4 5 2	479	51.8	463	205	~
J 1. •	26.2	32.2	13.5	-39.3	.0423	472	478	336	478	399	424	399	438	4.34	8 4	525	4 5 4	301	4.93
32.	36.2	32.2		• •	000000	472	e e	833	# G # .	# S # .	433	•	429	4.43	163	30	4 3 3	005	4 8 5
17.	26.0	31.9	19.4	0.01	0431	.472	519	319	440	440	440	0 7	432	4 4 8	7 9 7	519	164	\$ 0 <b>4</b>	204
•	23 9	317		- 40.7	.0430	472	916	314	+2+	***	T P	* 2 4	₩.	4 4 5	<b>7</b>	9 2 9	99+	¥ 16.	e T

Table 23A — Scaling Run 45, Test Configuration 1: One 1.52-cm Nozzle [(1) indicates thermocouple on an inlet jet centerline]

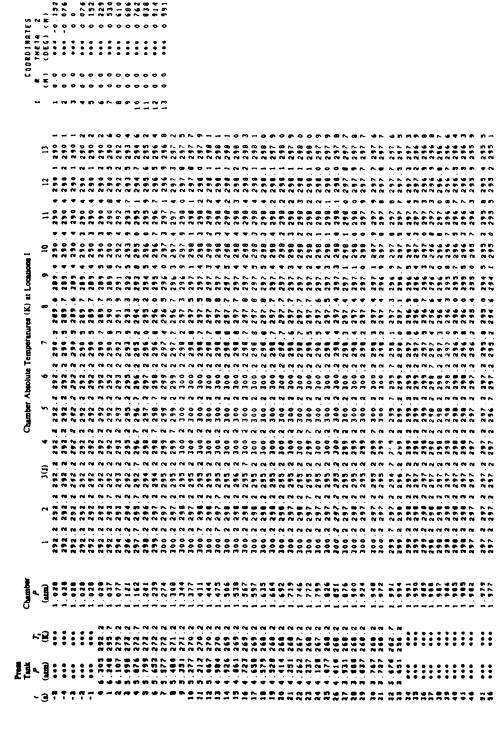


Table 23B — Inferred Pressurant Distribution, Scaling Run 45, Test Configuration 1: One 1.52-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

. 346 . 706 . 948 . 344 . 710 . 947 . 344 . 696 . 999 . 444 . 470 . 992	775 P. 44 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4

Table 24A — Scaling Run 46, Test Configuration 1: One 1.52-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

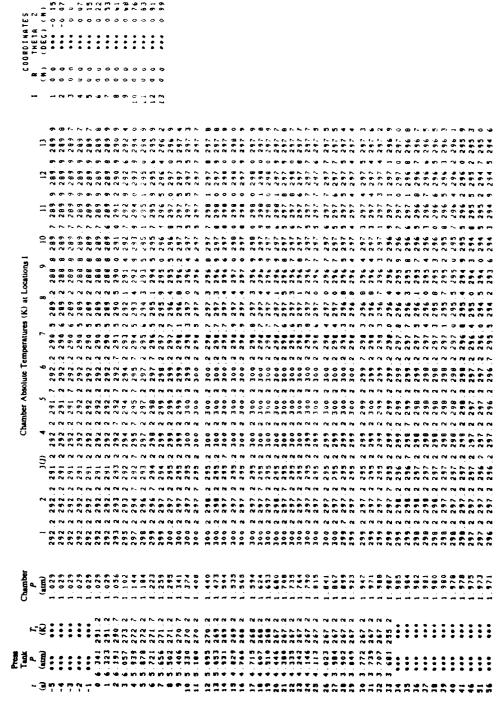


Table 24B — Inferred Pressurant Distribution, Scaling Run 46, Test Configuration 1: One 1.52-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

		13		;	•			025	022	080	093	=	8	153	200	203	222	242	<b>548</b>	247	5 ë 6	278	301	598	329	334	3 3 8	342	¥ 1	0 r	2 2	3.0	3.84		386	364		395	124	413
		71			535		239		057	060	136	14.	157	8 Z R	500	220	539	247	24B	5 9 2	584	287	301	307	359	334	328	362	9 9 9	- I	7 7	397	901		986	÷		395	451	426
		=	,	000	~ 000 -		- 700	- 095 -	0.45	080	111	133	157	161	200	220	213	558	2 4 8	265	275	2 7 8	292	307	309	4	3 4 8	372	4 6 4	D !	0	K 6 M	90		9 6 M	410		419	42	4 3 8
		01	;	000					0 3 3	0 6 1	111	1.24	157	170	183	212	230	238	248	247	275	528	262	307	338	344	346	345	7 9 1 9 1	9 6	2 6	3.7	384		3.9.6	396		<b>~ 0 </b>	453	431
		•			000 -		- 387	- 001	045	128	138	167	190	178	200	220	230	238	275	256	566	282	301	307	319	334	346	182	* 10 10		3.6	386	395		986	398		395	197	438
	Location	••			000			- 072	033	0 6 0	150	124	1 48	170	1.83	203	. 222	242	240	5 2 6	566	287	292	598	338	308	3 2 8	335	41	\ r r	3 2 6	397	393		386	398		395	421	456
	Pressurant Fractions (X) at Locations	1			- 232		239-	- 001		٠	•	133			•		. 222	•		٠	. 257			107		334	338	342	323	- 1		397	393		n	398		383	397	4.38
,	it Fractio	•		•	000		1 804	140	115	0 6 6	155	183		٠				•		•						334		345	•	•	•				•	468		4.53	445	+37
	Pressurar	~	•		000		_					099					•		257														•			392			14	
		4			000			•	•	660	•	•	•		•	•	•	٠		٠	•		•	•		•	. 330		Į:	2	197	-	*		٠	19			. 44	
		30	•		000		ż	_	٠	388	376	•	,	•	•	•	0.25	•	٠	·	649	٠	•	·	•	_	_	. 748				_			•	916		•	909.	•
		7	•		000 0			37	. 23	3 . 191	•	•		٠	•		. 400	•	•	•	. 558	•		•	٠	•	•		•	•	•				•			•	9 . 626	•
		-	•	000	000		5	- 095		003	60	0.09	0.82	7.	9.	7	2 30	7.	52	. 2	. 284	. 29	. 31	31	ČV.	¥66.	7	342	P	7	9 17		•		10 P	468		Ţ	443	<b>P</b>
		₽ĸ	•	000	B10.		. 022	0.59	680	116	145	. 165	187	. 214	.233	230	. 267	. 283	. 298	.312	325	338	330	361	372	362	3 \$ 2	405		619		*	452		664	463		0.4	0.4	024
		B/8		00.0	.0043			3.8593		9049	. 8057	7116	. 6434	9259	. 5856	5691	.5437	5894	•	.5141	·	4639	4637	4712	4010	4330	4240	1136	N 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2	50.00	0 0 0	3661		\$16 B	3099		3036	1880	. 1139
		æ	•	0	169.0			100 8	38.1	29.5	27.2	26.3		27.3	24.9	24.0	24 7	26.0	9.92	25	•	23.4	•	26.4	24 9	76.1	26.3	9.0	27.1	5.0		78	26.6		0	11729.4		11366.7	2014 9	4312.4
	*	.ĝ	HING	324	• .		18.3	15.9	13.5	13.2	13.5	13.9	14.5	15.2	15.6	1.91	16.5	16.9	17.2	17.5	17.7	9.0	18.2	18.4	9.	18.7		0.61				19.7	13	8 C 3 E		20 0			19.9	19.7
	4	ō	CORRESCE VALVE OPENING	17.6 324.1	9	S E	18	20.2	22.1	53 6	24 8	25.7	26.6	27.1	27.5	28.0	28.3	28.4	28.5	28 6	28.7	28 8	28.9	28.9	53.0	9,0	29.0	52	2	2		5		VE CLO	20.5	38.6	CL 88E0	58 4	26.2	2 · B
	*	. <u>Ç</u>	ICE VAL	2		•	18.6	19.9	21.3	22.4	23.2	8. E	24.3	24.5	24.8	25.0	25.1	25.1	25.1	25.1	25.1	23.1	33	23.1	25.1	73	23.0	0				2 4 7	24.7	CE 49				7.4.4	24 3	0 7 7
	•	3	CORRE	•	-	VALVE	۰. د	0. 0.	0.4	2.0	•	0.	3. B	9.0	10.0	11.4	12.0	13.0	14.0	15.0	26.0	7.0	9.9	19.4	3 ¢ .	21.	22.0	23.0		2 2		78.	29.4		9.0	71.	***	32.0	33.0	• •

Table 25A - Scaling Run 47, Test Configuration 1: One 1.52-cm Nozzle [(J) indicates thermocouple on an inlet jet centerline]

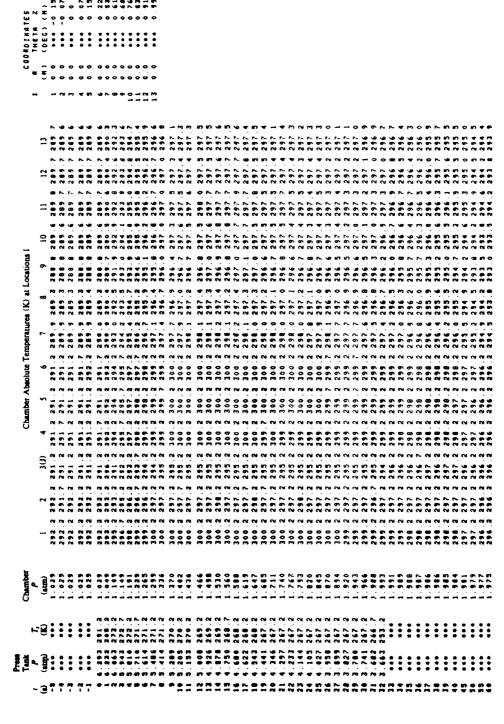


Table 25B — Inferred Pressurant Distribution, Scaling Run 47, Test Configuration 1: One 1.52-cm Nozzle [(J)indicates thermocouple on an inlet jet centerline]

· 9	<b>~</b> €	<b>™</b> .6	90	9/8	p.	_	7	3(1)	•	8 1 4 5	·		œ	•	9	Ξ	17(1	2
INDENCE AND	9	4			•				-	,	,		•	•	2	=		2
!	12.3	17.3 195.9	5.4	0.00.0	000.0	0.00	0.000	0.000.0		0 000 0	0 000	000	0000	0000	0000	000	000	
1.0 10.6		25.1	1.00	2.7107	.015		620			020		936			0 3			- 082
•																		
2.4 19.9	. 9	19.7	113.9	5.8157		-1.875	=	_	336-1			1.875-	- 239-	2.317	-3.201	-2 317-	_	548
7. 0 21. 2	3 7	13.6	33.6	1 . 1 0 3 0			. 234	336	- E70	100	6.0	0 0	0 0 0	•	,			0 7 3
4.0 22.4	23.5	14.4	37 6	87.8	121	. 017	. 23		. 072	410	. 072	180	•	117	۰	0 9 3	128	117
5.0 23.1	3.4	. + .	27.3	. 7003	146	010	272	797	0.70	0.20	127	107	136	7.		***	771	77.
6.0 23 5	23.4	14.0	28.9	7934	169	0.93	37.2		•	50	=	155	1 32	159				
7.4 24.1	5 e	14.9	22.3	. 5447	119	•	342	3.2	120	980	128		291	12.2		-		
1 1 21 4	26.	13.3	26.3	.7164	211	1 29	390	427	172		2 2 2		-			•		
9.0 24.8	27	15.7	22.7	5425	230	-	436	321	138	60	3	300	2 2	213				
10,0 24.9	<b>5</b>	16.1	2 4 2	2885	247	. 210	. 423	331	167	124	167	218	227	218				
11.4 24.9	6 ~	16.4	8 92	. 6424	. 265	. 223	<b>~ = 7</b>	374	102	138	7 15	212	234	234			23.1	2 3 1
	5	16.	24.8	5039	280	. 247	116	. 3 9 8	203	160	2 0 3	236	2 38	256			236	2 3 6
	~	17.		. 56.29	292	. 261	. 324	617	. 216	172	. 216	232	3.61	243			3.7.9	2 2 0
		-	24.0	4977	0 H	. 2 8	191	•	. 240	193	2 40	267	276	276			294	285
		37.6		. 5367	. 323	9.50	36.	989.	. 242	196	2 4 2	27.9	2 9 8	388	270		286	2.98
75.0	7		24.4	4292	333	50 E	28.	675	259	.212	239	386	596	586			305	305
_	~		23 0	111	9 P P	316	(4) (5) (6)	693	. 271	224	. 271	309	318	290		318	309	337
0 22 0	-			4276	658	9 20	616	.709	. 282	233	213	350	330	31.1	339	330	8 <b>4</b> E	339
19.4 24.9 28.7 18.5	2 2		2	6338	373	329	. 373	7.19	329	232	280	319	339	349	339	349	349	3.4.9
0. 0. 24. 0	21 7	9.		4027	383	9.34	631	.729	. 285	236	2 8 5	334	354	9 4 6	344	334	364	384
	28.7	7 . 9	7	•	R6E	928	•	. 741	067	239	5 6 3	339	370	349	349	339	370	339
24.	<b>~ 8</b>	-	~	***	. 403	348	630	. 752	396	243	294	343	363	365	363	363	373	375
1.4 24.6	26.9	19.1		. 3362	17	. 362	366	.720	. 413	.260	311	362	372	372	382	372	403	403
4.0 24.7	20	19.2		4228	4 20	. 139	. 672	776	411	253	367	380	380	359	391	391	391	391
3. 4. 24. 8	~	19.3		3433	420	996	:	7.89	. 421	263	316	379	389	379	389	3.69	0	00
9. 4. 6. 6	<u>~</u>	19.4	29.4	• • • •	436	339	683	791	. 413	303	339	348	4 0 5	380	391	4.02	413	4.2.3
7. 0 24.5		19.5	3.02	37.26	P++	3.9.5	<b>)</b>	.796	410	333	410	380	3.88	388	377	88	410	•
1.12 1.1	=	19.6	29.4	4110	431	194	3	900	403	34	403	382	3.94	382	3.0		9	5 9
INNENCE VAL	.VE CL!	15 URE													•	;		,
19.0 24.5	20.5	19.7	23.2	. 2999	483	474	707	. 813	417	303	360	394	900	383	429	417	417	424
10.0	7 T	19.		3649	+9+	891	701	817	410	3.3	410		4 10	18.7				
FOLVE FULLY	CL 88 E	_							:				•		:	;		,
_	20.3	-	22.0	3337	04.	166	. 762	. 822	407	341	407	407	•	407	407	407		
_	29	20 2	- 16.0	-, 2548	470	437	67.	260	402	347	402	-						
33.0 24.7	21.9	30.7		6160	470	462		889	9	3 4 9			428	•		7 7 7		
_	21 3	10	•	1029	0.4	439	673	6.73		2 2 2		, m		) # 			7 7	70
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Test Configuration 4: One 1.52-cm Nozzle Scaling Run 48, 1 Table 26A ジェジェゥらの くりらか とっらの じょう ちゃまとうゆう きょかにから しゅいょ からかまさう ちゃか かんとく ここちをし こくご こご こご こご こご ここしょう うしょくし

Table 26B - Inferred Pressurant Distribution, Scaling Run 48, Test Configuration 4: One 1.52-cm Nozzle

13		. 012	017	178	=	0.64	111	139	89 1	174	218	213	230	245	272	295	131	333	333	347	378	<b>8</b>			2 2		0.0	395	,		<u>;</u>	405
11		- 210	9 0 0	219	5.0	240	124	126	7.0	306	230	137	230	237	290	800	122	335	360	360	378	398		,			0	11	, ,		;	422
=	0	•	0 42	219	013 -	. 047	111	151	0 .	3 1 6	230	241	279	294	305	321	9 6	9 17	374	374	392	8		*		; ;	387	428	;	:	,	422
9	•	~	6.50	261	072	047	111	101	- -	7.00	230	249	243	237	265	569	960	1 15	333	360	364		390			,		399	•		:	422
•	9	•	Ċ	٠	110		_	Ċ			194			232	222	285		101	333	678	230	370	36.			384	387	379				405
ations I			•	•	•	•			•	9 6		•	•	•		230			344		•	•		•				529				125 1
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tions (X	•	,	2 . 042		•		١									244									7	•		*		7		
int Frac 6	÷		. 0 12	•	020	•	•	. 018	•	. 691			,	802	•	. 238	•		250	•	•	•	•		2 2	•		. 214			•	371
Pressura S	•		0.0	٠	20	٠	.097		-	. 69		17.	13	.201	.2	- 5			250		563	~	.27	7	2/2	7	30	379				371
•	•	412	013	134		11.	. 197	131	. 168	210	130	. 177	194	308	. 214	. 218	243	25.2	. 250	. 264	565	270	. 275		280	-	387	. 179			•	171
~		012	. 013	134	0 2 0	-	.097	121	9	2.5	85	.177	134	. 208	214	2.5		2	250	. 264	263	270	. 275	2	0 0 0		387	379			•	3 2 E
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		012 -	. 0 32	261	214	010	- 043	=	7	160	138	. 177	194	. 208	- 214	. 218	24.2	7 2 2 3	. 2 30	. 264	. 263	5.5	273	0.0	77.		- 1	379	;		:	371
•	•	:	0.20	063	0.34			178	661	219	23.4	.271	.287	.302	316	6. F	- K	4.5	375	58 E	338	404				747	***	.461			•	• • • •
9/6					3837	9250	9298	1229	.7163	7362	.6001	9169	. 6 3 3 S	.6241	6119	.5910	90 50	3121	. 5173	+834	.6319	4521	. 4434	1706	8694	, M	4360	.4266		700		4524
•	-	53562.0 -7	-	135.8 5	42.0	34 0 1	32.5	30.7	27.7	29.9	5.6	90.00	29.6	29.7	9 0	o r		29.5	31.2	29.1	9.00	30.1	0.00			37.2	6.48	2 10	;	2261		-3436.6
<b>™</b> Ĉ	32126	~	• " =	33.6	13 6		Ť.	3 .	= :			20.0	20 . 2	70.	2	20 · F		71.7	21.4	21.5	9. 12	71.7				22	22.0	22.1		22 2	:	22.2
<b>~</b> .6		100	1 . 1	23.2	23.1	24 5	23.5	26.3	2 5	27.6	28.5	24.3	<b>31.</b>	28.5	20	5.5	2 2	2 2	28 7	28.7	28.7	28.7	7 1 2			21.	7	28.1	. כנים: יים			28 6
~£	E VALVE	18.9		21.4	22.8	23.0	24.5	23.1	53.6	25. 46 25. 46	36.0	1.92	1. 92	1. 92	56.0	97	26.0	26.0	23.9	16.0	23.9		5.0			25.5	23.4	23.3			_	23.2
	=	•	-	_	_		_		•			_	13.0	_	_					_	_	_					_					•

One 1.52-cm Nozzle Test Configuration 4: Run 49, Scaling I ١ Table 27A 

Table 27B — Inferred Pressurant Distribution, Scaling Run 49, Test Configuration 4: One 1.52-cm Nozzle

13	091	104	225	200	7 6 6 F	9 8 8	n e o	1275	0 4 4 4 K	505	4 95
12	0.000		243						2 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5		2 2 2 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4
=	0 100	104	2002	2000	2 P P P P P P P P P P P P P P P P P P P	N 9 10 10 10 10 10 10 10 10 10 10 10 10 10	376	225	4444 M	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	4 9 6 9 5 9 5 9 5 9 5 9 5 9 5 9 5 9 5 9 5
9	0000	017	1000	52.2	2	1 M M	307	444	40404	8 9 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	4 6 6
٠	0 000 0	130	253	222	- N - N - N - N - N - N - N - N - N - N	2 4	4 4 4 4 6 4 4 6 4 4 6 4 4 4 4 4 4 4 4 4	******	7777	4 C C C C C C C C C C C C C C C C C C C	80 8 4 5 9 6 4 10
cations I	0.000	M 60 0	137	2.4	237	N 4	376	M 0 0 W	2444	833 831 831	5 9 6 6 5 10
X) at Lo	.213	1000	123	222	222	200	200	25 25 25 25 75 77		2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	4 4 6 6 4 9 5 6 6 9 5 6 6 9 5 6
Pressurant Fractions (X) at Locations 5 6 7 8	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	113	202	222	2	,	0 4 E	0000 0000 0000		22 22	4 9 4 4 9 6 4 9 5
murant F	1,000	5.55	- F - F - F - F - F - F - F - F - F - F	700	224	7 0	315	, , , , , , , , , , , , , , , , , , ,	11000	37.0	4 4 8 2 2 3 2 3 5 2 5
£	. 216		128 178 178	750	22.		115	10000 10000	11000	371	123
~		9115	173	555	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	, , , , , , , , , , , , , , , , , , ,	118.	22.44	5555	37.0	3 A A A
7	. 216	510		200	22.5	0 0	115	2244	132	12. 12.	123
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*	000	064 095 122	134	0 M M	2	1 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	263	7 0 N 9 17 1 0 N 0 17		75 42	476 476 476
	•	-, -, ,						,			
<b>%</b>	6.1496	2.4835 1.1166 .8629	1.0398 7321 3979	3.00 3.00 3.00 3.00 3.00 3.00 3.00 3.00	M & W   W   W   W   W   W   W   W   W   W	# C # S .	1271	2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	### K	3 2 2 3 3 3 3 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	1090
•	202.4	2 3 3 6	22.7.2		7 2 3 0	5 6 6	26.1			7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	0 B N
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<b>₽</b> .Ĝ	20.6 22.2	22.5 23.5 27.8	200						n 1 1 n 1		CL 868
<b>~</b> §	20.6 20.6 22.1	_	5 2 2 6		n n n		22.5				27.6 27.6 27.9
-3	COUNTRICE VALVE OPENING 0.0 20.6 20.6 141. 1.0 22.1 22.2 20.									29.0 29.0 20.0 21.0	7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7

Scaling Run 50, Test Configuration 4: One 1.52-cm Nozzle ١ Table 28A りょうてん ちおくりにかどごとり ちゅくからかになっ りゅり くからか とごじ りらちょうかんきん アンことにととにことにこと とごぞこここご ここしょうしょうしょうしょうしょうしょ

Table 28B — Inferred Pressurant Distribution, Scaling Run 50, Test Configuration 4: One 1.52-cm Nozzle

	2		0.38	697	1 22	142	188	200	211	234																						497			300	511	4 7 8
	13	0.000	B 0 0 1	. 072	111	172	186	210	221	243	. 261	304	321	330	341	365	391	366	37.1	380	398	396	1.1	. 121	4.50	=	462	<b>4</b> 2	4.04	491		<b>49</b>	499		532	21.	~
	=	1 016-	919	<b>9</b>	143	1 7 2	179	191	2 2 1	. 262	. 299	323	331	3.50	341	365	380	366	360	402	3.67	421	11	433	<b>4</b> 3 8	4 7 8	4.9	<b>8</b>	- B +	517		497	240		300	579	<b>6</b>
	01	000		097	100	145	<b>9</b> 8 7	237	249	262	289	304	(Y () (F)	340	341	3.5	380	366	£ 0 4	391	432	410	446	454	£ 9 ¥	4 7	<b>★</b>	214	4.9	204		511	513		346	252	1.4
_	•	0 0 0	090	110	111	162	198	191	221	223	251	576	292	340	341	334	391	366	360	369	387	387	422	409	# 3 B	-	4 J	20	481	<b>4</b> 5		484	472		876	484	478
ocations	800	000	.026	9 4 0	1 00	1 45	170	191	-51	243	270	304	315	340	330	# # P	320 3	336	360	380	398	398	399	421	-	478	437	₩ 8	 	504			513		3.28	525	<b>8</b> ∠ <b>▼</b>
(X) # L	7	216-1	. 800	039	. 079	123	151	163	174	. 206	222	276	. 264	111	300	. 324	349	134	316	33.0	333	352	399	382	• •	£04	•	<u>-</u>	455	438		421	4 38		491	497	•
ractions	•	0 1	213 -	122	134	132	142	. 200	239	201	261	. 237	273	291	280	303	319	326	403	424	375	433	434	443	4 30	433	7	£ 9 9	89	4 7 8		=	413		424	420	4.8
Pressurant Fractions (X) at Locations	٠	9 4 9 8 9 8	233	186	134	152	142	200	239	281	261	237	273	291	381	303	319	404	E 0 T	424	432	433	434	443	430	433	462	163	194	121		184	483		417	470	249
£	•	9	233	106	134	202	233	200	239	. 291	309	. 257	321	. 291	381	354	319	409	403	454	432	£ 2 4 .	434	.445	430	123	79	. 463	168	478		187	183		477	470	349
	~	0.4	517	0.59	134	103	1 42	. 200	*	187	213	237	273	194	280	303	319	305	294	313	319	318	316	326	328	328	336	334	337	346		331	330		341	334	80 7
	7				2 * *		~	108	9	187	<b>.</b> .	61	۲2	;	178	25	<b>5</b>	0.2	3.4	E1.	13	=	16	56	3.6	2.	36	4	37	9 +		3	330		<del>.</del>	134	<b>.</b>
	7	0.1-1	•	•	•	•		٠	•	•	•	•	٠	•	•	•	•	•	•	•	•	•	٠	•	•	•	•	•	<u> </u>	T.		•	•		•	•	
	-	1.0		. 0 59	1.14	. 13	143	. 20	. 239	7	. 2 11	. 257	. 23	5.0	2 80	e E	31	90	0	313	37		Ť	. 443	Ť	. 43	-	•	•	4.7		Ĭ	. 483		. 42	4.0	Š
	124	0.000		660	. 122	1.	170	. 192	.212	.237	15 E	178.	287	301	.316	329	341	10 E 10 C	6 9 E	375	383	362	*0*	. 413	424	. 432	0	244	434	094		467	473		477	477	.427
	9/8	0.0000	100.0	1.1417	9290	8483	.6412	.7099	.6918	.87.00	6149	.5176	2608	8378	6119	47.42	. 4745	. 3948	5404	4095	.4661	1694	.4633	8+0+	2343	1200	3792	.3877	3680	.3313		3370	.3512		.2613	000000	.1102
	•	***	21.2	9. 4	20.1	7. 7.	24.5	26.3	27.3	1 22	27.0	23.2	26.3	25.8	30.5	24.0	23.8	31.3	30	3. E	8.75	29.5	29.5	9.75	29.0	29.4	20.1	29.8	29.0	27.8			1.0		2.	0.	ш 80
	٠.		•	•	•	•	-	-	Ξ.	٠,	٠,	<b>.</b>	•	۲.	21.6		m.	*	•	•	•	•			<b>*</b> .	•	~	-	•		<b>.</b>		-				•
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*	Ş	MEE VALUE 20.9 2	23.7	33	26.2	27.0	37.6	28.0	29.5	23.4	20.5	28.0	28.8	20.0	28.6	28.7	28.7	28.5	28.3	28.4	28 . 3	20.3	28.2	28.2	1. 1.	2 F . I	<b>7</b> 7.	28.1	28.0	28.1	CE VAL	28.1	28.0	אווי	27.9	37.9	37.6
	- 3		4 BATOA	•	• .	•	•	7.0	•	•					14.0								22.0							29.0							0 X X X

Two 1.52-cm Nozzles Scaling Run 51, Test Configuration 5: ١ Table 29A 

Table 29B — Inferred Pressurant Distribution, Scaling Run 51, Test Configuration 5: Two 1.52-cm Nozzles

=		-	361		0.75	0.8	164	218	260	292	323	340	367	397	4 1 2	437	419	4.5		471	7 6.4		4 6 4	490	488	498	500	508	514	1 B 4	485	487	492	<b>₹8</b>	504	512	469	489	<b>4 9</b> 0
21	!		- 020		0 6 0	613	119	195	238	263	310	327	360	390	431	124	436	438		471	<b>4</b> 21		502	513	196	498	900	5 o 8	497	481	4 6 B	487	183	478	485	464	091	470	161
		0	- 19		. 82	٠				272			•							191	93		16	13	519	8.6	60	80	14	25	85	0.5	92	14	• •	*8	. 62	. 09+	7.
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9	!	0.00	350		- 230	- 023	0.7	163	210	258	289	320	333	397	417	432	4 8 3	458		90 +	9		316	303	486	300	300	316	306	481	4 8 5	8 / 4	501	96 +	50.0	521	479	470	4 9 0
- 6			99		109	038	119	210	212	282	596	320	333	377	454	431	436	465		9	<b>78</b>		479	497	472	465	484	491	497	481	468	469	483	478	555	503	460	4 8 9	
cations 8		000	3 <b>4</b>		128	075	523	210	238	299	316	340	380	403	454	438	476	458		479	479		509	497	96+	498	509	508	523	489	503	514	501	533	522	515	497	86+	209
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Pressurant Fractions (X) at Locations I		000	9		. 027		173	218	260	272	316	360	334	337	376	391	402	472		.479	471		454	505	084	463	459	++	116	684	477	691	465	094	* + 5	436	+ 8 1	479	8
£.		•			112	376	263	295	295	340	916	960	399	337	378	161	405	403		6 2 0			137	427	480	463	139	6 4 9	9 ;	<b>4</b> 03	477	469	163	9 9 9	8+	438	488	624	084
		000.0.000.0.000			631	•	•	•		272	•	•	•	337	•	•	•	472		. 62	٠		437	27	084		439	449	•	. 68	. 22		465	. 091	<b>4</b>	:	. 88		400
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		0.000	9		. 027	1 30	128	1 +0	. 224	. 272	316	. 294	334	337	328	391	. 4.82			=	17.		437	427	100	. 465	413	449	116	119	427	169	163	9	=	438	4 8 8	. 429	2
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13-4		0.00	•		•	=	-	~	~	~	m	7.	m.	7	•	•	•	₹,		₹.	•		₹.	•	•	•	₹.	₹.	•	₹.	•	•	*	•	▼.	•	•	•	₹.
9/8		•••			9192	678	505	365	• • • •	6989	016		383	438	999	5043	1940	4559		4719	4219		2062	125	0382	111	0406	0834	427	415	0442	431	000	9260	944	0.0	9110	0495	•
od.	•	•	٠		•	~		·	•	•	ĺ	•		•	•	•	•			•	•			•	•		•			•	ĺ		•	•		•			•
90		•	066.1		114	13.9	18	16.5	13.1	13.2	16.7	13	15.2	16.1	16.0	16.6	16.0	11.0		17.7	72.2		35.4	31.3	<b>.</b>	20.3	°.	14.3	7.3	~	<b>9</b> . <b>6</b>	۷. ۲	•	15.9	~	0			0.0
	<u>u</u>	•	•		<b>.</b>	•	~	~	•	~				٠	•		•		<b>¥</b>	•	=				9.						<u>.</u>	-	٠.		٠.	Ξ,		=	
€.0	1	4 142			<u>.</u>	=		2	2 2	2 2	1 23	1 22	3 23	8 23	7	2	3	2 24	1881		33		9	3	ž	5	, ,	24	ž	3	3 3	1 23	1 2	53	4	4	2 23	0 23	~
<b>~</b> .6	- W	2	~	OPER	24.3		000			36	~	14	=		39	33	33	39.2	VE C	39	=	CL 8S	3	37	37.3 24.	3 6	9	3	P	E	33	33	33	3	Ħ	34	7	ř	<del>-</del>
<b>~</b> 0	3.	21.4	21 2	FULLY	7.	3.6.6	21.9	100	1.3	32.2	32.5	32.7	33.0	33.0	13.0	33.0	12.9	32.7	CE VAL	32.6	12.3	FILLY	32	31.3	31.2	30.7	9.0	m		•	•	23.7	29.7	29.4	? <b>?</b>		29.1	28.9	28.9
~ 3	CORRECT VALVE OPERIE	•	•	****	•	•	•	• .	• :	<b>.</b> .	•	•	10.0	•	12.0	13.0			_	• •	• · <u>· ·</u>	VALVE		<b>1</b>	76	<b>3</b> . •	22.0	23.0	24.0	23.4	<b>5</b> . •	27.4	<b>3</b> .	29.4	• •	11.	32.0	77	-

Table 30A - Scaling Run 52, Test Configuration 5: Two 1.52-cm Nozzles

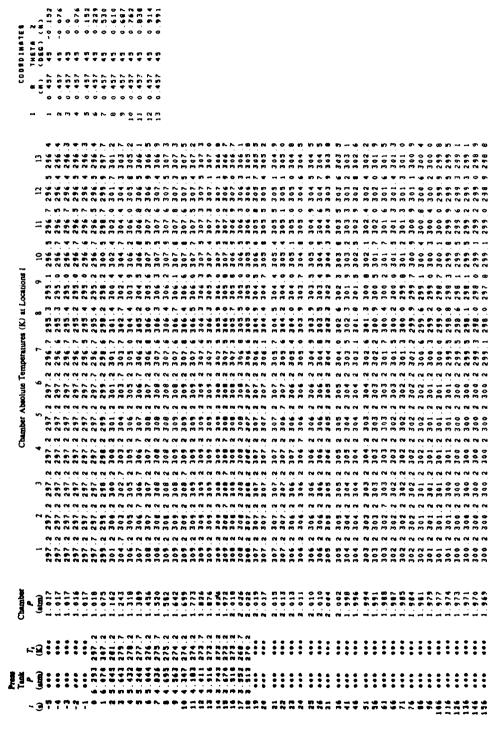


Table 30B — Inferred Pressurant Distribution, Scaling Run 52, Test Configuration 5: Two 1.52-cm Nozzles

	=			2 2 3		091	-	189	241	293	335	340	380	399	4	451	481	4 6 5		505	201		\$ 2.8	5 2 2	518	534	-	0 E 6	255	\$ 2.4	511		8 7	7 1	9 C	515	0 0	9 F	9 7
	12			+1+		- 305 -	020	142	516	270	E 0 E	333	187	405	434	445	481	4.82		499	496		320	306	3.5	ç	٠:	. 6	j 0 4	124	521	<b>T</b>	on 1			315	000	2 F	202
	=		0000	679		- 459	0 3 8	123	192	247	589	356	353	399	4 2 8	458	467	06.		8 7 8	4 9 3		520	214	502	•;	•	ř	'n	8 B •	493	51.4	600			493	6 4 4		3 6
	2		9000	226		- 264	. 0 2 5	123	208	240	310	319	367	399	4 2 8	4 5 8	4.4	468		492	808		\$ 2 0	330	205	e.		r.	513	524	205	010	9 7	,	r	203	66	* F	2.10
	•		000 0	300	:	- 302	127	198	273	270	588	333	380	378	-	438	424	468		485	4. 4.		215	0 6	493	4 3	:	010	468	4 8 8	205	000	- * - *	· ·		n n	\$ 0 T	0 °	98
Location	•		0000	**	;	- 722	-	1 20	233	255	303	333	353	405	4 2 1	4.51	09+	490		4 8 5	201		497	908	4 B S	517	499	313	4.93	4 8 9	7 7	<b>T</b>	D 4		, ,	203	479	4 7 4	200
R (X) EC	7		0000	=	:	- 196	152	23.3	257	293	303	3+0	380	399	434	131	467	468		0 - 9	478		497	48.5	483	483	307	906	486	906	11.	7 (	25		y (	493	499		9
Pressurant Fractions (X) at Locations	•		0000			292	. 279	310	. 298	338	332	368	408	372	393	0 I <b>+</b>	419	06.4		492	98+		294	314	485	473	7 6 4	PB V	400		4	9.4			7 6	355	010		9 4
Pressuran	\$		0000		;	329	152	170	216	223	362	333	305	338	359	376	384	383		456	=		420	4 2 4	;	433	4.2.1	m st t	460	4 4 2	~ 7		~		> -	3 / 1	***		
	•		. 000			000	. 279	563	257	300	. 296	. 333	303	33.8	339	376	384	383		420	**		428	134	:	F 7 3 3	. 421	. 40	371	3 6 6	~				) ·	5.2	B 5 7		
	8		0.000		•	000	343	263	•	•	296	,	•	•	•	٠	٠	•		•	•		428	¥ 6 7 .	•	433	421	804	460	4	~						113		
	7		0.00			•	٠	•	•	•	. 296	•	•	•	•	·	•	٠		•	4 4 8		. 428	474	•	E .		•	7	•	₩.					•	•		
	-		0.000	77.	•	. 332	. 152	. 217	. 297	. 263	312	. 298	. 3 3 9	372	393	4.10	419	418		420	98+		. 467	111	483	. 473	79.	453	900			2.4				225	0 0 0 0 0 0		
	×		000.0	•	:	==	. 162	502	243	277	306	EEE.	357	378	<b>404</b>	. 421	437	. 452		463	478		084	•	087	•	•	•	•	•							•		
	8/8		0000		•	4.2429	1.2446	.9193	. 8299	.7502	.6402	9029	.5746	. 5265	.7265	.4919	4750	. 4985		.4463	1004		.1321	. 1513	1198	. 0832	.0861		00000	0 9 2 4	645						1961		0000
	<b>40</b> .		•		•		21 . 1	17.3	16.9	16.7	13.5	17.0	13.0	13. 7	17.0	16.7	17.4	18 · 51		18.5	6.6		7.7	~	en ev	1.7	-	• .	0	-	~	0 4	- 0			0	~ -		0
*	Ç	HING	72.	•		7	23.9	23 . E	23.9	24.3	24.7	25.0	23.4	23.	26.2	26.5	26.7	26.9	8 UR E	27.	27.2		27.4	26.7	26.3	26.3	26.2	3.6	26.0	e .	9.0						2 E		20
g.,		340 3A	2 5 2 5 5 5				7 11	34.4	36.2	37.3	38.7	23°	•	n •	•	÷	12.0	•	VE CL1	<b>8</b> .	s .	CL 68E0	7.5	7.7	3.0		-	P	M .	9 1		•				0 1	io er	) (F	9.0
•	ĝ,	CE VAL	23.5		֚֓֡֝֝֝֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓		5	12.2	13.2	13.9	7.7	34.5	34		7	34.9	31.8	34.6	CE VAL	34.4		FULLY	93.9	£.	32.8	22	12 2	31	5	9 1 1		= =	2 -				0 C		7.00
	(2) (2) (3) (9	CORPER	•		֓֞֝֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֡֓֓֓֓֓֓֓֡֓֡֓		-	•	9.	•	~	•	•	• .		12.	13.0	• · • ·	COBBE	- 1	16.0	VALVE	17.0		13.	9.0	21.0	5 5	23		2 3						22.4		7

Two 1.52-cm Nozzles <u>ج</u> Test Configuration ਤੇ Run 53, Scaling NAME OF THE PROPERTY PRODUCTION OF THE PROPERTY i Table 31A Change of the control  $= \frac{1}{2} \cdot \frac{1}{1} \cdot \frac{$ 

Table 31B — Inferred Pressurant Distribution, Scaling Run 53, Test Configuration 5: Two 1 52-cm Nozzles

			i			Two 1.52-cm Nozzles	Two 1	.52-cr	Two 1.52-cm Nozzles	zles									
- 3	<b>~</b> ₽	<b>~</b> 0	r.ô	•	9/8	×		~		Æ →	Segurant S	Pressurant Fractions (X) at Locations I  5 6 7 8	(X) # [	ocations 8	~	2	=	13	=
	CE VA	COURENCE VALVE OPEN	9#1#8	,					;	;									
• -	25.5	N 00	2 2	135.3	0.00	000	. 131		- - - - - - - - - - - -		6 4 4	000	0 0 0 0 0 0 0 0	9 9	9 0	0 0 0 0	0 000 0	0 0	•
	FULLY 28.7		23.3	• •	2.8073	114	PO.	. 136	3 62	136	136	136	252	. O .	119	. 0 3 0	0 1	6 9 0	-
	12.9		22.1	19.6	1.1343	164	130	197	256	. 197	103	130	216	1.78	186	0.00	122	100	- ~
•	2.2		22.	16.7	1	246	234	254	188	25.	217	. 291	3.6	210	254	193	217	539	~
•	33.9	27.9	23 . 48 24 . 48	9.62		27.0	. 271	105	60 6 F	E 0 6	236	271	305	271	278	2 3 0	264	283	~ ~
		200		2.0		10 10 10 10 10 10 10 10 10 10 10 10 10 1	33	P		1 PS	3.33	999	3 4 6	3 13	333	312	3 3 3	9	'n
	76.		23.	91		5	7 O	- ~ - ~	347	746	~ ~ ~ ~ ~ ~	0 0 7 P	# 9 00 F	406	- F - ▼	6 E E	- E	41.3	m <del>e</del>
=	6		50	9	123	10 C	396	763	363	. 363	363	966	9 F	25	4	75	4 2 9	429	* *
			7 9 7	12.3		97.4	121	200	7 10	307	387	4 2 4	F 60 7 ♥	4.5	46.8	7 50		7 to	• •
14.0 34.6 41.1 26			26.7			. 432	. 421	ê	205	785	987	0 4 4 0	470	477	F. 60 +	470	497	Ę	•
	, .			,	;	;	•	•	:	,	ì	;	•	;	;	•	;	;	•
			27.	-	45.22	4 7 8	7.7	# W	6 M	7						4 9 6	2 4 5	96	• •
ATTA	FULLY	CL 88E1	:	•	!			:							•	•			
17.0	32.9	2.00	26.9	~	1197	646	.467	459	429	. 429	429	294	304	684	0 0	516	511	334	<b>8</b> 0 (
= :	M 6	6 P	36.6 26.6	~ -	1512	6.4	?			393	471	910	4 / 4 4 / 4	0 10	505	4 10 6 0	0 10	0 m	en en
	32.5		76		1237	629	6.24	437	437	6.37	437	479	526	28.9	303	503	 	320	•
2.0	12.4		26.1		0426	479	471	429	429	429	429	+	200	513	961	513	529	521	4
22.0	12.2		26 . 1	•	0434	624	452	410	410	410	452	161	528	503	203	537	E ⊃ S	520	<b>W</b> D
23.4	£1.9		25.9	7.7	1680	624	497	434	424	424	434	497	6 B 7	<b>463</b>	264	484	497	905	4
~ ;		4 · ·	53	•	0000	479	-		8 4	9 9	-	16	6 9	000	483	4 9 1	517	005	4 4
	: :			-	86.40				, ,	7 7			, ,	9 9			7 6 7		, 4
2.0		36.5	52.6	•	40	624	¥.	5 5	429	429	429	4 25	. 60	203	523	203	521	523	•
2	7.1	36.3	23.3	•	.0494	624.	. 467	421	. 421	. 421	421	467	204	535	504	523	523	\$ 1.4	3
29.0	31.1	36.3	25.5	0.0	0.000.0	624	. 493	116	116	400	446	446	205	205	493	521	205	521	5
3.	9.	9.5	25 . 4	6.	1018	624	518	470	420	375	470	423	499	4 2 0	209	4 9 0	209	526	•
-	9.00	9.0	25.4	0	0000.0	479	497	•	6 + 6	449	449	7 9 7	487	¥ 8 4	<b>8</b> 2 <b>9</b>	497	497	7 6 <del>4</del>	•
9.5	000	# W	25.5	0 0 7	1061	624			•	-	•	* *	* °	* 0	4 6	# G	4 6	 	• •
• · · · · · · · · · · · · · · · · · · ·	0	35.2	23.2	8		624	7.5	435	. 432	435	432	4 6 5	522	492	205	522	492	\$12	•

Table 32A - Scaling Run 54, Test Configuration 6: Three 1.52-cm Nozzles

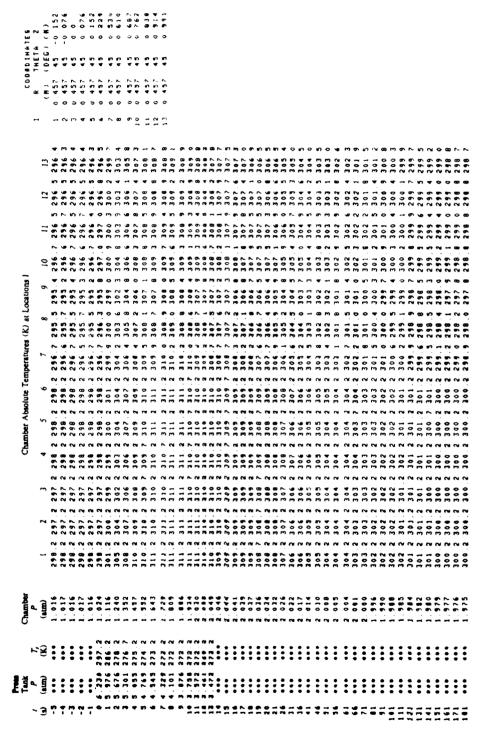


Table 32B — Inferred Pressurant Distribution, Scaling Run 54, Test Configuration 6: Three 1.52-cm Nozzles

2	2		- 032			0 60	334	369	408	431	460		439	<b>+8+</b>		197	516	514	505	506	521	524	332	512	491	503	510	503	4.95	513	504	301	208	489	490	1	4 7 5	4 7 8
:	71	9	- 104			300	134	381	420	442	460		485	205		508	310	521	512	306	\$14	133	218	512	306	. 51	910	527	111	330	315	215	323	•	490	987	B / T	<b>484</b>
=	=	0	0 12			2 6 6	3 4 6	392	4 0 8	445	4 9 4		9.4	+ 0 +		520	533	527	519	306	205	5.24	3 0 3	497	206	503	515	511	519	513	512	301	308	524	=	9	30	961
9	2		284		7 6	28.0	322	364	988	431	466		482	484		508	491	514	4 9 9	4 8 3	200	884	496	473	4 8 3	511	212	519	519	513	4 9 3	309	4 9 9	<b>.</b>	111	7.0	•	• • •
٠	•	9	032	. 7 .	3	2 2 8 7 2	3 2	381	-	425	6 4 9		434	496		483	304	501	472	492	486	88	481	468	483	496	510	311	495	303	493	301	208	-	E 4 9	304	•	2
Pressurant Fractions (X) at Locations I	•		212	222	- 4		322	80 F	392	425	4 55		470	478		497	523	508	512	499	200	512	503	505	. 521	519	549	343	533	513	250	. 526	525	535	.316	304	-	523
(X) at 1	-	900		4		23.5	7 6 3	313	333	361	399		414	+61		455	472	. 463	43.9	451	451	445	467	438	476	488	478	495	. 471	. 472	434	467	. 463	. 435	4.0	430	439	. 431
Fractions	0	999	0	316		277	310	324	369	409	. 427		433	3 0 2		-	472	694	472	492	914	11	160	438	. 191	<b>0</b>	421	453	£ 1.	423	ij	*	415	•	447	415	31	. 50
essurant	n	900	0	316		277	310	324	369	604	427		439	205			472	. 463	472	492	186	481	496	512	491	480	471	455	519	303	193	¥ 8 ¥	.482	<b>19</b>	.534	322	=======================================	5 9
Ē.	•	909	761	133		277	340	387	397	409	. 427		439	. 502		485	472	163	472	. 492	486	481	460	. 512	.491	480	47.	433	7.3	. 423	19	<b>+8+</b>	. 482	7.	. 447	322	=	B 0 8
•	•	999		133		277	287	324	369	334	.372		604	=		425	409	398	439	424	417	410	424	438	415	£04.	393	373	159	. 423	413	101	396	378	447	. 432	2	413
•	7	000	•	•			251	324	314	134	. 172		375	386		425	403	39	439	7.	417	410	. 424	<b>438</b>	413	. <b>1</b> 03	393	. 413	. 139	. 423	. 413	- 60	. 196	<b>79</b>	44	432	- 43	. 419
-	-	999	9	:		2 .	01E	324	369	600	. 427		124			+	472	. 327	565	492	917	=	496	. 512	164	•	1.4	. 493	\$19	363	. 433	:	412	230	. 514	. 332	. 312	. 30
cq	<b>×</b>	9	670	761		22.7	314	05.8	362	409	+64.		. 448	14.		100	14.	184	186	1	184	1	1	1	<b>1</b>	111	=======================================	~ ·	=	=	<b>19</b> + .	=	104	<b>I</b>	=	1	100	<b>!</b>
ć	» /a	9900	9.3910	4743 6	1231	050	8090	7104	67.42	.5762	. 5970		3936	. 7425		.2772	. 1946	. 1033	.0713	1110	0.0768	.0792	.0406	.0112	1980	.0442	0440	. 0924	0.00.0	0939	0.00.0	.0494	. 1019	0000.	. 0528	1065	•••••	••••
q	Q.	•	1.23.1				7	12.9	13.4	12.9	14.2		13.3	•		un Pe	2.5	F. 1	•	<b>+</b>	-	<b>•</b>	ņ	- 0	-	•	ب	7	•	- 5	0	•	P9.	•	~	-	•	•
المرة	5	1116	24.3	3.66		23.6	24.4			26.2	26.7	3	26.9	27.4		27.3	26.9	26.7	26.3	26.3	26.2	26.1	26.1	25.9	25.7	25.7	25.6	23 . 3	25.5	25.4	25.4	25.3	23.2	<b>2</b> 2 . 2	25 . 1	25.0	23.4	3. e
w. §	2	3	7												_																					1.9		
ام و	5	H VALV	26.9	. בין היין			13.9	36.3	36.8	17.0	36.9	EVAL	36.7	36.5	: פרוא נ	36.0																						
~ 3	5	CBREE						_	_	_	_	2			-										_	_		_	_	_		_	_	_	-	72.	•	• .

Test Configuration 6: Three 1.52-cm Nozzles Scaling Run 55, ١ Table 33A 

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Table 33B - Inferred Pressurant Distribution, Scaling Run 55, Test Configuration 6: Three 1.52-cm Nozzles

	13			.083	•	0.48	161	23.5	291	369	200	403	430	897		<b>?</b>	315		919	310		50			005	200	308	305	. 319	411	412	. 113	. 4.93	. 504	300	513	917	503	<b>?</b>
	21		000.0	. 683		610	152	257	70	33.7	199	7	<b>43</b>	490		900	115	;		324	+ - 6	~ ·	000			200	16	916	919	499	489	304	309	312	316	913	415	194	=
	=		0.000.0	078		-	191	0.33	317	9 7	410	Ţ	991	+		200	5.2.5		+ 2 G ·	. 5 20	4		0 10	276		P P	933	33	326	9.29	. 512	520	. 532	220	. 512	537	. 32	503	. 512
	2		000.0	986		980 -	0.34	+8-	259	322	360	+ 1	4 2 8	473		£	<b>J J J</b> ·	•		=	-				9	7.	503	•	497	477		•	302	515	300	303	523	<b>!</b>	47.
=	6		000.0	405		1	152	272	317	357	38	419	439	. 473		. 183	499	•	436	215	•				473	F 6 7	469	•	475	•	467	483	478	473	192	-	<b>F 9</b> 3	486	470
Locations	•		0000.0	1.050		1.153	6 9 3	-	259	322	360	403	433	437		436	. <b>48</b> 3		. 204	200	320	-	.00	9		2.0	491	•	497	:	497	.489	. 4 9 3	436	. 300	. 513	. 309	9	Z#+.
Pressurant Fractions (X) at Locations I	1		•	562		•	113	213	246	916	343	170	401	. 401		. 436	. 477	!	6.4	134	• 0 .	7	***			•	-	•	. 482	•	424	187	7.4	496	. 432	496	908	191	470
Fraction	•		0.00.0	. 244	1	0.93	202	191	317	276	316	339	390	=		. 423	92 P	;									169	•	. 432	. 162	. 412	673	470	. 463	99.	436	. 432	419	
Pressuran	S		000.0	562		•					316	•	•	٠		. 423		;									•		452	•	•	٠	•	•	• • •	436	. 4 3	. 303	<b>**</b>
	•			- 562		•					171	•	•	•			. 426										. 469		. 452		482	•	•	٠	•	٠	•	٠	•
	•			562		•					371	•	•	٠		<b>2</b>	٠										•		. 452	•	482	•	•	•	•	•		•	•
	7		•	162			•	•			316	•	•	•		430	•		•	•	٠	•	•	•	•	-	٠	•	. 526	•	. 412	•	•	٠	• • •	•	٠	. 303	•
	-		0 0 0	. 244	1	- 131	103	134		22	316	. 3 S	390	=		. 423	=		2.4							2.4	•	Ē	. 432		. 412	473	.470	. 463	9	436	. 433	208	
	×		000.0	600		=	891	229	200	322		313	413	664.		97.	. 478	•	2	507		10 ( W	P (			5	<b>8</b>		£ .	B9+.		\$0.	. + 63	. 483	. + 83	. 485		\$0 *	B 7
	9/9		• • • • •	9.5296		6.0637	2,2453	1.0738	8720	2096	6999	. 6209	.5907	. 5938		2005	. 5026		22.2	1034	910	700	26.90	21.20	9374	68.7	• • • • • •	***	. 0 4 1 1		.0426	. 0 6 7 3	•••••	. 0449	. 0457	.0465	. 0474	9260.	•••••
	٩		•	1108.0		72.9	24.3	14.1	12.9	11.0	12.3	12.7	13.0	16.3		•	r. <b>8</b>	;		7.7	=	9.4	• •			+ · R1	•.	M.	•	• •	6.4	10.1	•	3.5	re en	¥.8	<b>89</b>	11.3	•
•	÷Ĝ	# 1 H G	97.	24.1		23.0	21.9	22.	23.3	24.1	2	23	25.4	26.2													25.3		25.1	. <b>82</b>	24.9	24.	24.8	24.7	24.7	34.6	24.2	<b>34</b> . 4	<b>1.</b> 1
•	G	14E 0PE	23.	23.4	BPEN		12.1	1.92	7.	41.2	43.7	5			110 311	44.7	-				~	<b>9</b> .	N.	•		7.	13.2		30.7	-	31.2	37.7	1.76	37.5	17.3	17.1		7 7	¥.
•	ĝ	ICE VAL	<b>33.0</b>	23.4	FRLLY						76.3			16.3	ICE 491	7.97	-			* ·		7	2:	2		22	32.5	32.2											
•	-3		-	-	VALVE	~	•	•		•	~	-	•			11.	~ ~			•	-	-				-	2.0	83.	34.0		36.	27.0	 	29.0		11.0		7.	

Three 1.52-cm Nozzles Test Configuration 6: PROPERTY AND THE WAR AND THE PROPERTY OF THE PROPERTY AND 56, Scaling Run ł Fable 34A TE TO THE PROPERTY OF THE PROP 

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Table 34B — Inferred Pressurant Distribution, Scaling Run 56, Test Configuration 6: Three 1.52-cm Nozzles

	2			•	0.0	228	2 8 2	33	374	00	4 3 8	. 463	4.67	9		512	<b>48</b>	508	497	4 > 7	- B	486	164	479	0 8 4	<b>8 8</b> 9	8 / 1	<b>4 8</b> 5	486	969	501	505	88	4 B 7	489	1.64	487	4 8 9
	2			T - Z	. 70	228	27.8	M	360	900	469	428	294	100	:	512	303	313	90	1.6	4 9 1	300	491	493	194	495	€ 6 9	4.05	505	503	501	505	505	495	. e <b>+</b>	497	478	481
	-		۰	۴	•	_		•				•					<u>.</u>				n	•	80	6	_	<u>.</u>	90	~		9	'n	۰	0	~		~	۰	
	Ξ			2 . 6 9 7	•		~			Ť	**	Ŧ	478	*		200	493	*	10	Ŧ	473	479	4	+	'n	•	•	~	4	4	₩	4	Ŧ	Ŧ	•	462	+	435
	9		000	. 4 7 6 4	0.43	237	5 6 6	374	36	423	4 . 9	E 9 #	4 9 0	507		529	499	4 9 3	317	497	4 9 3	493	512	507	509	525	309	515	518	511	517	529	513	503	522	51.4	495	513
_	•		0 000	- 9.4	128	290	36.2	374	0 7	41.2	Ī	452	194	102		306	487	305	497	181	894	493	484	493	484	493	301	477	4 6 4	503	493	497	497	487	464	488	<b>8 ~ 4</b>	463
cations	•		. 000		0 2 9	219	278	200	274	000	92+	4 3 8	430	501		517	303	505	523	497	205	200	526	515	531	525	516	523	518	527	540	521	513	319	514	197	504	524
Presentant Fractions (X) at Locations	7		0.000			2		5	*	34	37.9		431	111		468		470	•	7.1	461	472	20	98	80	9.8								•			٠	•
tions ()			0.00		i				•	•	282	•	•			•	•	4.004								•		•	٠				,	•	•	٠	٠	
nt Frac	•		000.0				•		•	•	•	•	190			•	٠		•	•	# T		•	450	•	•	•	٠	471	•		Ŧ	₹.	421	-	Ŧ	•	. 433
ressure	~		0.00		244	22		29	18.	371	397	0 P +	461	467		439	487	4.70	797	304	104	479	470	450	4.4	429	486	.477	471	191	. 462	-	431	503	4.89	484	. 4 6 2	455
_	•				426	316	130	293	987	000	197	430	191	467		439	-	470	797	471	88	479	470	430	443	429	014	477	47	79	462	<b>8</b> 7 7 .	431	421	489	8	. 461	. 433
	۳,		:		212	316	320	326	7.0	:	197	, <del>1</del> 30	194	467	,	4 2 9	<b>2</b>	470	**	304	81.	479	0.4	÷ 20	. A 43	503	91.	427	141	<b>+9+</b>	.462	448	513	503	489	<b>.</b>	194.	433
	7		100		171	124	200	293	987	:	13.7		16.1	46.7		489	-	470	1.5	304	÷	479	470	122	916	203	486	477	47.1	151	462	8.8	513	303	489	100	346	341
			•	•			•		•	~		٠.	•	~		•	٠		•	•				~	•	·			_	•	N				•		•	
	-				•	-	2	2	=	ř	76E.	•	•	467		7	Ŧ	*	Ť	•	Ŧ	479	÷	25	5	'n	7	7	+	<b>*</b>	7	Ŧ	S		Ŧ	7		Ŧ.
	×		000.		174	235	2.0	. 3.25	36.	162	417	<b>*</b>	462	479		ij	<b>:</b>	**	*	ij	Ŧ	ij	=	**	=	=	ij	ij	=	=	*	Ĭ	ij	ij	**	:	=	***
	9/8				2.2968			7206	.7101	<b>2009</b> .	.499	98.86	. 8776	4932		. 1711	7036	.1310	9190	.076	.0726	.0748	. 0382	.0783		•	. 0815	0000.0	1910	***	0000.0	.0912	.0469	0.00.0	8240	0913	00000	.0307
	9		9		N . 9 N		7 87		2.2	12.6	11.3	. <del>4</del>	14.9	B. +		9. 2	<b>1</b> .7	1.2	•	•	۲.	۸.	♥.	۲.	•	♥.	•	0.	•	₹.	0	<b>-</b>	♥.	•	♥.	•	0	s.
	r.6	9 1 1 2	8. 2			24.2		34.6		25.4	36.0	26.2		26.7		26.7	26.2	15.9	25.	23.7	23°.	25.4	25.3	22 . 2	23.1	23.	24.9	24.9	 	24.7	24.7	24.6	24.3	24.3	24.5	<b>54</b> . 3	24.1	24.3
	r.Ĝ	348 31	83.9			5	=	•	-	42.8	7	-		•	1.0860	7.7	13.1	<b>†</b> 1.5	=	:	7	7 62	2.0 2.0	39.	1. 1.	3 6	 =	=	37 7	37	37.4	37.0	7 92	7. 9.	3.6.5	9 9 8	9.0	33.8
	۲Ô											79.5														32.0	7.		1.	-	E .	0.		<b>.</b>	7. 01	. 4	*	2.5
	-3	COUNTRICE	•	19 10101		•	•	•	•	• •	•			11.0	VALVE FI		•	14.0	• 2	• .	17.	•	19.0	20.0	21.0		23 •	24.	23.0	26.						32.4		

Scaling Run 58, Test Configuration 6: Three 2.54-cm Nozzles ł 

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Table 35B — Inferred Pressurant Distribution, Scaling Run 58, Test Configuration 6: Three 2.54-cm Nozzles

*									Æ	CORUTAN	Pressurant Fractions (X) at Locations	(X) at 1	ocations	~				
.g :3	ĝ	ફ	•	B/e	124	_	7	~	•	٠,	•	7	•	۰	2	=	12	13
ICE VAL	_	1186																
29.9		69.2	•	•••••	• • •					100.	-	. 000.0	000.		0.00	000	000	
5.0		÷.	77.	.0061	. 629		1 . 102						. 220	•	- 11	000.0	000.0	000
7117																		
23		73.	200	9.0119	7		919	1 . 137	177	926	616		739	7	. 336	348	- 080	0.17
12.6		23.6	•	2.6611	16 a	. 147	123	200	6		7 7	165	~	202	•	=	157	. 228
16.1		34.6			380	. 361	442	. 42	196	443	442	7	291	356	292	318	. 161	.367
ICE VAL	=	388																
17.0		25.3	÷.~	£962.	. 443	£119	ij	439	Ť	Ţ	ij	. 412	414	426	403	415	421	877.
28.3		26.1	3518.5	. 6463	417	111	302	ij	. 347	505	. 526	. 471	29+	•	435	. 33	47	0.
FILLY	_																	
17.9		16.1	2155.3	. 4 6 23	988	100	304	204	3 6	200	346	<b>18</b>	200	20.	4.95	491	495	495
36.4		25.4	1117.3	. 2052	308.	. 521	. 321	425	321	521	321	303	499	503	490	4 9 3	499	503
33.6		24.9	717.5	. 1318	208	. 300	. 531	ij	133	531	333	+6+	503	198	4.9.4	489	489	484
34.9		24.6	628.3	1134	308	. 531	. 931	£1.	331	531	22	•	493	493	493	418	488	483
7.77		24.2	638.7	1210	206	. 521	. 521	.471	. 321	521	52.	496	496	436	96+	511	306	501
22.0		24.	411.1	. 67 33	908	. 520	. 520	. 469	120	524	320	187	495	300	500	200	910	520
23.5		23.9	211.3	. 0317	308	368	. 53.1	.479	331	531	363	479	490	202	505	193	202	\$15
32.9		33.6	516.3	1066	900	. 539	. 539	. 13	939	533	+ 13	480	<b>96</b> †	301	491	491	49.	. 301
32.6		23.5	299.8	.0331	900	. 529	329	£ 4.	. 529	529	329	<b>*</b>	303	205	186	497	486	.497
32.2		23.3	162.3	.0149	900	. 522	. 322	. 467	. 322	523	525	493	511	31	4.95	684	489	206
31.9		23.1	317.1	. 0583	300	. 515	919	439	313	.513	515	491	510	51.5	510	493	<b>\$</b>	313
31.6		33.1	324.9	.0597	900	315	. 531	<b>* * .</b>	. 302	531	505	492	508	200	308	. 502	505	\$1.
11.2		23.3	302.1	. 0922	905	. 527	937	473	. 473	. 537	517	473	499	133	499	493	6.8	518
31.9		23.3	348.4	. 0635	908	. 525	. 525	£ 2.	. 125	. 525	323	<b>1.</b>	100	115	49	498	492	518
7.6		<b>24</b> . <b>4</b>	134.4	. 0691	305	. 310	318	=	318	. 518	518	196	304	=	511	. 489	104	326
B. 0E		24.1	160.7	.0112	300	306	. 382	+10	206	305	306	. 43	. 521	# <b>.</b>	513	498	138	.521
10.2		24.3	160.7	. 0 6 7 7	908	. 596	326	. 473	512	336	3.3	<b>2</b>	490	6	4 90	7	. 473	4 9 8
20.0			278.2	~ · · ·	9	F 7 10 .	m T	9	*		r r	7.4	£ 4 .	P)	30	9	9 ~ V	305
9.6		7.	2.19.9	. 07 16	9	. 933	376		223	233	27	. 472	=	-	204	~	•	
29 . S		24.4	199.2	9960	905	305	396	808	201	598		472	=	430	499	•	472	481
19.2		24.1	8. 411	. 0749	908	980				210	4.5	<b>46</b> 2	9.4	476	476	137	43.7	924
23.1		24.1	2.8.2	. 0 3 8 3	900	364	364	<b>29</b> + .	364	.564	316	106	477	425	496	4 4	467	;
28.9		24.	211.0	. 0219	98.	48 S.	. 234	<b>*</b>	488		* S .	474		•	474	• •	44	¥
20.7		24.4	411.2	. 0796	900	14 th	966	416	263	543	543	479	•	4.3	500	434	•	200
78.4		<b>74</b> . •	1.4	. 0 8 2 2	900	. 5 20	3	£ .	25	25	. 528	=	55 T	<b>4</b>		<b>.</b>	=	306
7.		24.1	• •	0.00.0	906	613	£13	9	• 0,5	906	900	477	=	. 477	477	991	999	200
28.		34.	462.0		905	. 391	191	141	. 831	391	47	471	78	47.	7	•	434	313
7 7 7			237.4	.0436	900	90	F 9 P	419	. 463	R 9 B .	963	* * *	*	•	79.	439	. 477	513

Three 2.54-cm Nozzles 9: Configuration Test Scaling Run 59, ı Table 36A Change of the control 

Table 36B — Inferred Pressurant Distribution, Scaling Run 59, Test Configuration 6: Three 2.54-cm Nozzles

PRESENTANT Fractions (X) at Locational I (Fig. 1971) (C.) (C.) (F.) (C.) (C.) (C.) (C.) (C.) (C.) (C.) (C		11 12 13	000 0 000	170 133 049	į		327 . 322 . 353	•	0	684 394 924	-	. 493	492	767	493 493 498	4 6 4	006	605	\$ 0 ¢	505 499 511	. 495		300	•	484	. 483	<b>48</b>	<b>8 7</b>	473	124	485	. 486	_	9.4	474	•	705 697 FB4
HERE WALNE OPERHIEC  12. (**C) (**C)				.352		. 12/	311	:	420	2/4			₽ ∠ ▼ .	684	G 0		300	520	509	4 8 2	493	489	500	492	4 9 0	4 9 5	F 6 <b>T</b>	B. C.	488	667	964	500	504	264	484		
TE WALVE DEFENSE  28. 4 28. 4 28. 7 4 0.000  28. 4 28. 4 28. 7 7 4 0.000  28. 5 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 7 7 6 0.000  28. 6 29. 7 7 6 0.000  28. 7 7 6 0.000  28. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	ions I			1						•	3 490			·												•				•	٠	٠					
TE WALVE DEFENSE  28. 4 28. 4 28. 7 4 0.000  28. 4 28. 4 28. 7 7 4 0.000  28. 5 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 7 7 6 0.000  28. 6 29. 7 7 6 0.000  28. 7 7 6 0.000  28. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	(X) at Local		•	i		•	•		•	•	_	_	_	_				_								•	_	•			•	•			_	433	
TE WALVE DEFENSE  28. 4 28. 4 28. 7 4 0.000  28. 4 28. 4 28. 7 7 4 0.000  28. 5 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 28. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 6 29. 7 7 6 0.000  28. 6 29. 7 7 6 0.000  28. 6 29. 7 7 6 0.000  28. 7 7 6 0.000  28. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 6 0.000  28. 8 20. 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	nt Fractions	ø	•	377	į	7	664		٠	2.5	•	•	•	•			•	4.5		•	•		•	٠	•	•		•	•	٠	•	•	. 497	•	•		•
C	Pressura		•		i				•	•				•	•						•	•	٠		•	•		•		•		•		•			•
T			•	•		•	·		•	•	•	•	•					•	•	•	•	•	•	•	•	•	٠	٠	•	•	•	•	•	•	٠		٠
T. T		7							•	•	-	,	•	•	•	•	•	•		•	٠	٠	•	•	•	•	•	•	٠	•	•	•		•	•		•
T. T		-	•			•	•		•	•	•				•			•	•	•	•	•		•	•	٠			•	٠	•	•	•	٠	•		•
The control of the co		*	•	=	i	. 3	Ġ.			-	57	4.	₩,	•		,	•	•	<b>6 *</b> .	•	•	<b>.</b>	•	ŧ.	<b>F</b>	•	•	₹.	64	•	64.	<b>F</b>	6.	<b>5</b>	•	,	^ ·
THE TOTAL TO		9/8	•	6.6675			. 9547	:	7113	E 266.	2625	1 9 25	. 1372	6860.	.0743		0616	0559	***	0592	2090	.0622	0638	0325	1002	0343	0 2 0 1	0338	0731	0754	.0385	.0789	0404	0411	0418		.000
		<b>Q</b>	~	43.7	:	12.3	<b>9</b> . <b>k</b>		7.	~	7	•	•	₹.	Lė I	•	•		₹.	•	M	M	e.	<del>-</del>	e,	œ.	m	~	ĸ	€.	ď	₹.	~	~	N	•	•
SEGRADO COOKERS DE LE SEGRES LE SEGR	•	r.6	=	23		5.0	٠. ا	¥ .	•	5		2	6																								
SEGRADO COOKERS DE LE SEGRES LE SEGR			LVE 0P	29.0	Y OPEN	37.9	44.5	RIVE CL	= :	~ :			~	~	~ 1			-											9.7	37	36	36	3 6	36	33	*	•
	•	۲ô		2	=	2	2		Ë	-	1	*	2	2	ž			-	33	~	32	Ē	=	Ē	31	ŝ	÷	ê	å	29	2	23	3	3	2		;

Table 37A - Scaling Run 60, Test Configuration 6: Three 2.54-cm Nozzles

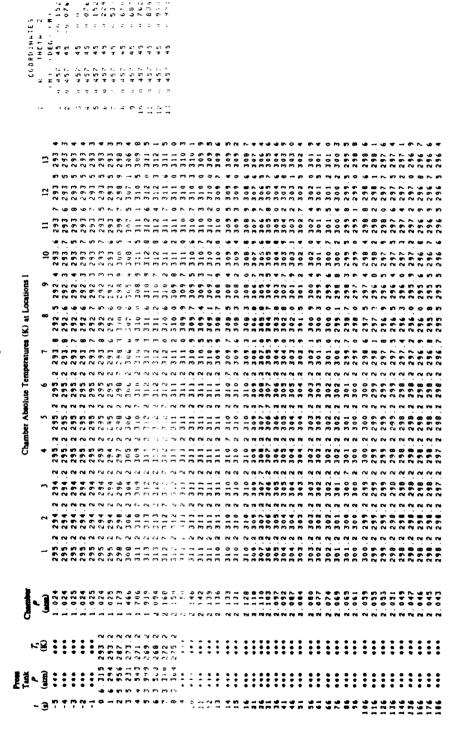


Table 37B — Inferred Pressurant Distribution, Scaling Run 60, Test Configuration 5: Three 2.54-cm Nozzles

	Ξ.		1.24		900	232	361	,		9	4 8 3	0.8	493	498	503	516	200	4 80	.0	205	518	. 525	520	215	20	5.2.4	208	510	215	4 4 6	498	4 9 9	** **	189	£ 8 3	9.6	•
	13	6	000		- 168	188	130	,			684	₩ ₩	8 6 4	4.93	505	496	200	191	501	513	230	400	531	206	503	2.0	208	215	499	964	492	499	4 7 8	489	483	486	***
	=	9	124		- 411	•	400	3.0%	9 1	437	8.8	4.83	4 9 4	4 2 9	492	4.9.1	0 6	÷	1.5	5 0 5	593	255	238	7.	497	4.93	4.95	4 & S	493	4.99	492	4 2 8	4 7 8	475	4.93	4 > 8	
	9	_	7		_	1.25	583		7		4 9 8	4.8.5	4.4	€ B 3	477	4.56	493	491	491	513	513	£ 9.3	205	206	£ 0 3	5 J	514	204	525	. 0 3	512	506	₩ 3 8	503	9 6 7	514	
_	6		000		_	227	331	;			498	485	0 - •	474	477	481	480	480	480	480	474	<b>48</b> 4	479	464	491	493	484	498	480	465	4 ? 5	485	47.1	489	<b>48</b> 3	47	
cations	∞		000		-	.079	303	3.00		2	434	68+	4 2 4	479	482	496	500	191	491	480	064	664	96+	200	503	206	201	4.9	499	# 83	492	4 8 5	485	4 8 3	4 90	500	,
Pressurant Fractions (X) at Locations	~	0	2.4		146	. 250	2.5	•			483	489	6 2 9	479	. 192	486	808	49.	483	491	490	64	¥ 8 3	~8	492	206	£ 80 ₹	6.5	£ 9 J	483	485	499	æ ∠ <b>•</b>	964	490	486	, ,
ractions	9	9	000		. 4 93	330	E .			5.	533	531	5 3 2	532	5.26	521	310	515	. 528	519	513	664	4 8 2	224	5	206	<b>E</b>	529	519	496	. 4.85	. 506	519	510	2 <b>6 9</b>	984	
surant F	~	ć	000		299	390	404			.533	514	551	533	. 532	.526	521	510	538	.528	519	.513	499	483	524	5.5	506	543	523	.519	529	. 552	540	519	510	533	558	
Ë	4	0	338		610	•••	A	768		. 23.	533	331	535	. 332	. 526	. 523	015	312	. 528	519	513	499	483	. 524	5.5	306	483	466	5 ·	496	. 485	206	513	.510	497	486	•
	~	000	000		.015	468	<b>#</b> 33	•			473	463	4 8 8	<b>+ 8 +</b>	477	471	439	486	475	194.	425	=	482	79	. 155	÷	12	994	455	463	.485	472	450	439	4 9 7	486	
	7	•	000		. 319	. 313	326	700		•	673	. 463	488	184	477	. 423	. 454	486	. 473	161	457	499	483	164	455	: :	.483	994	. 455	96	482	472	519	. 510	. 497	486	
	_	•	000		493	. 238		• • •		4 30	314	5.0	533	532	5.26	. 521	. 562	538	528	519	513	<b>6</b>	343	524	515	206	543	529	. 519	2 6 2	. 552	. 540	.500	240	3.68	258	
	ı×		1.24		. 113	. 272	.96.		6		133	499	4 9 9	489	4 9 9	664	199	499	.439	499	488	.499	664	499	664	664	664	4 9 9	488	494	664	499	488	499	449	499	
	9/8	0000	0436		9.2362	2.8234	1.1007			*EC/	37.00	1879	2032	0960	8660	9220	0.00	.0827	2950.	.0875	1090	.0929	.0317	0648	9990	0603	0702	.0358	0364	0744	0380	.1127	00000	.0816	0419	0426	****
	90	-	13.5		77.7	14.4	٠.	,		6.176	286 9	142.7	154.3	22.9	75.7	58.9	40.7	62.8	43.0	9.99	45 6	S. 0.	24.1	19.5	20.5	51.8	53	27.2	57.6	56 5	28 9	8.9	0 0	62.0	31.8	32 3	
16	<b>,</b> 0	N1NG	0.00		22.5	24.4	* * *			* .	26.6	9. 7.	25.3	25.1	24.	34.6	7.	24.2	24.1	23.0	23.7	23 23	33.4	23.1	23.2	23	<b>5</b> 5	22.9	22.8	12.7	35 · 6	25.5	22.5	25.3	22.3	22.2	
*	<b>:</b> 0	13 40 56	800	PER	23.7	36.	7	MEE WALVE CLUBURE		20.7	50.7	=	8 . 9 4	6 5	43.1	+ . +	43.7	43.1	42.6	42.0	41.5	6.9	9.0	40.7	39.7	6		38.6	30.4	37.9	37.7	37.0	32.0	36.6	36 3	- 9 E	
16	-ô	CE VAL			13.4	33.3				20.0		17.4	36.1	35.5	9.	34.5	7.	33.6	33.4	32.9	32.6	32.2	32.1	=	5.	~		8. 8.	9.0	30.3	30.5	8.62	8.62	29.5	<b>29</b>	23.5	•
	- 3						•						•	• . •	.1.	•	•	•		•		•	•	•	-			•	•	•		•	• .		•		

Table 38A - Scaling Run 61, Test Configuration 5: Two 2.54-cm Nozzles

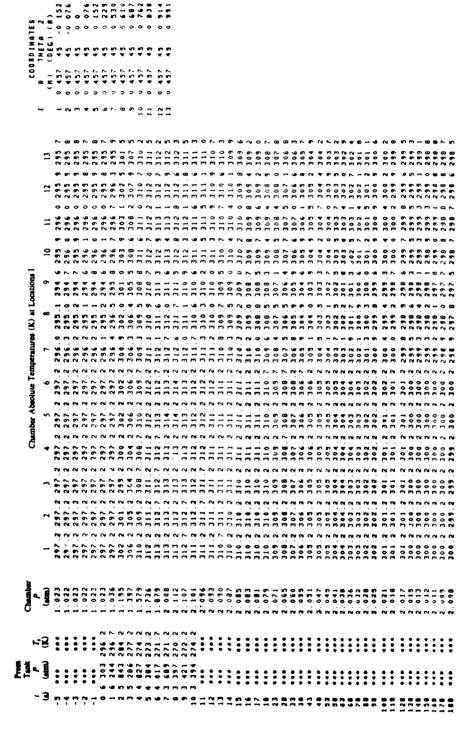


Table 38B — Inferred Pressurant Distribution, Scaling Run 61, Test Configuration 5: Two 2.54-cm Nozzles

	13			2 804	;	020	083	259	400	1:		4.52	A 60.		495	472	475	471	474	はいす	400	4.6%	503	205	<b>8</b> 8	505	205		<b>4</b>	.69	206	504	206	502	501	483	181	0 <b>0 7</b>	482	471
	12		000	38			0.55	234	33)	393		439	9.2		486	463	475	465	463	473	6 r 4	264	498	4.9.5	4 8 8	493	064	491	484	4 7 9	4 2 4	491	486	484	474	47.5	46.8	47.1	4 6 8	487
	=		0 000	8 38		284	046	228	337	362		4 3 9	476		4 . 0 	472	465	476	474	467	4 7 8	4.8.1	486	8 2 %	88	<b>₹8</b> 5	<b>8</b> 4 9	485	4 2 6	425	487	472	089	9. \$	454	445	454	4 6 4	4.5.4	<b>.</b>
	2		0 0 0 0	109-5		1	050	197	311	3.86		430	4 8 1		9 2 4	477	0 / 4	094	474	473	473	. 9 e	486	483	9 / *	487	064	4 8 5	. P	4 7 8	<b>4</b> 2 <b>4</b>	Q (- 4	084	469	481	244	8 8	471	6.8	;
	•		0 000	7.2		- 021	162	278	111	402		443	472		472	453	094	450	458	467	456	464	449	460	453	457	459	454	470	453	449	459	1.44	456	441	4 4 8	- 7 17	443	433	<b>449</b>
ations 1	<b>00</b>		000	21-12			135	271	358	415		452	9 6 4		064	482	485	483	479	473	878	181	486	683	88		<b>4</b> 7 8	-69	4.83	478	487	484	493	684	181	475	48;	8 2 4	475	478
Pressurant Fractions (X) at Locations			000 0 000 0 000	126-16		ı				53.5		462			064	472	180	465		8.1	. 291			472	459				483			824				. 5.	181	8.4	475	121
ctions ()	9		0 000	_						459			294				•				, 874				•				. 02	10.							475			
uant Fra	· ·		•	•						435			P		984	•	•	522					4 E 8 E		482	٠		•		484				509	•	_		533		
Presso	-,		000 0 00				٠	444																	•															
	*		000 0 0	٠			•		•	454			2 .512		•	1 501	•	•	•		•		463		•		•			•							3 475	•	\$24	
	•		000.0				•	444	•	459		•	512		•	•	•	•		•			250		•		•	•	•	•	•		•				543		524	٠
	7		-	•				413		454		•	. 512		•	•	•	•		•	•				541	•	•	•	•	•	٠		•				•			•
	-		0 0 0	. 261			331	352	394	435		489	. 512		509	. 550	. 540	. 322	. 532	543	533	525	520	501	. 541	. 534	. 526	. 516	301	. 347	538	533	. 519	509	562	3.50	5.43	5.53	524	. B
	Pre		000.0	. 0 12	;	1.29	243	323	380	426		.462	4.89		488	887	488	88.4	884	884	488	884	4.68	488	881	884	88 7	88.	488	488	488	887	468	4.8	4 88	884	4 8 8	4 98	88	•
	9/6		00000	13.6870		200	2.5624	1.1026	8028	6943		.6057	. 5162		. 0849	.1438	. 1262	.0789	0815	.0843	0.578	1650	9090	.0621	9690	0325	.0662	0190	0347	0332	0.357	0362	0740	0379	0385	0380	0397	0403	0410	9110
	<b>e</b> 0.		•	1199 7		9	18.2	6	•	-		9 3	65.0		<b>4</b> . <b>2</b>	12.5	11 0	9	7 1	7 3	0 10	89 193	ε. Θ.	¥.	10 10	8 2	& \$0	<b>6</b>	Ø M	 E	9	3 2	9	ED ED	<b>W</b>	÷ e	m	£. 5	9.6	*
*	<b>.</b> ©	3 1 1 1	6 9	23	;		24.7	25.7	<b>36.6</b>	27 4	BURE	28 0			28.1	37.6	27 3	27 . 1	3. 3.	3 9 2	36.3	<b>56</b> . <b>4</b>	<b>56</b> . 2	7,	3.6	25 9	23 8	25.6	256	25.5	53	25. 4	13	33.3	25.1	23 0	25.0	24.9	24.9	2 4
*	. <u>©</u>	VE 0PE1	23.2	5.5	*		33	-	45.7	46.2	VE CLOS	49.8	50.3	CLOSED	49 6	18 3	47.2	£.3	•	43.2	4.4	£ 4 3	43.9	43.4	<b>9</b> 0 .	12.7	42,3	8	Ç	-		ø. 6	<b>4</b>	49.5	0 0	3 %	39.5	7.5	39.1	
*	Ç	E VAL	23.5	23.2			33.5	3.91	38.4	19.3	E VAL	39.8				39.2	37.5	37.0	36.6	3. 3.	35.8	33.5	35.2	31.9	14.7	34.3	34.2	33.9	33.8	33.6	33.5	33.3	33.0	32.9	32.7	32.6	32.4	12.1	32.1	9. 8
	.3	CORNERCE VAL		•	•	~	-	•	•	6.6 39.3 46.2 27	CORRERC	7.0			•		11.	12.0				16.4	17.4	-	19.0	21.1	21.0	22.0	<b>3</b> 3.6	24.0	25.4	26.0	27.4	20.0	29	1.1		32.0	33.0	94.0

Scaling Run 62, Test Configuration 5: Two 2.54-cm Nozzles ļ Table 39A くんくくん くん くんくじょう こと こくさく ちんどうきかに はく の のくず にかに ひり おおらり とからり ことり とくり ちゅう ちょう ちゅうり ちょう ちょう ちょう ちょう

Table 39B — Inferred Pressurant Distribution, Scaling Run 62, Test Configuration 5: Two 2.54-cm Nozzles

•	•	•	#-							124	ressurant	Fraction	Pressurant Fractions (X) at Locations	ocations	_				
3	g	ç	Ş	<b>9</b> 0.	B/e	<b>6</b> 4	-	7	~	•	۸.	•	1	•	٥	90	=	12	13
	CE VAL	VE OP	2 N 1 N G																
:	21.2	21.2	98.	'	•	000.0	0.000	0.00.0	000.0	000.0	0000.0	0.000		0000	0000	0000.0	0 000 0	000	
1.0 21.3 21.3 24.0	21.3	21.3	24.	3843		000-	620	020	.020				. 017				0.54	050	0.17
141	FILLY	PEH																	
~	29.7	23.	24.	2	=	120	. 4.2		2.046	1.653	. 865		159-1	734-1	497-	2.206-	1.376-1		395
•	31.3	33.2	23		~	. 238	121	. 367	169	. 367	121	1.478	. 269	0.59		126	- 126 -	•	650
•	9.	310.3	24.	Ξ		319	. 268	306	380	380	268	1.268	291	508	202	860	135	150	=
•	35.7	1.9	23.		1 .9581	379	345	406	909	E 45	283	1 256	345	292	27.2	234	0.0	0.00	920
COMMER	CE VAL	VE CL	BSURE								•		!						
•.	36.3	44.0	26.	9	٠	.426	374	430	430	430	374	1.263	374	330	31.9	285	302	308	3.13
•·~	36.7	45.7	26	-4904	•	472	. 447	. 442	44	7		1.286	410	410	38			3 2 5	2 7 2
VALVE	FULLY	CL 0SE	6											:				•	
-	36.3	43.5	36.	6 -2486.7	4547	490	440	0 + +	110	0 7 7	0 0 0	1.287	. 419	430	6 -	604	393	0.0	209
•.	33.1	43.8	36.	-1108	9 .2028	490	. 442	. 442	. 442	=	.442	1.312	431	¥ 3	397	397	405	80	-
•	34.1	42.4	52	-1049	9 .1920	490	. 442	. 442	4 4 5	. 442	442	1.332	424	413	393	38.9	10 E	413	107
• · · ·	33.6	41.7	23		2 .0871	064	435	. 435	435	435	435	1.348	. 423	-	399	399	393	=	50.5
• .	13.1	•	20.	.661	7 .1210	064	4 P	. 421	4 2 4	42	421	1.366	. 427	E .	396	3.8		•	80
13.0	32.8	•	24.		3 .0628	480	434	434	+0.	434	404	1.333	60	403	383	383	383	390	0 6
• •	12.1	39	24.	- 531	٠	<b>0</b>	***	444	:	*		1.369	425		39.5	372	3 2 8	398	86.2
. <del>.</del>	32.0	39	3.	1 -366.4	0290.	064	491	. 424	434	424	. 691	1.367	101	417	377	390	377	797	390
• .	7.		**	-376	•	•	99.	994	•	432	*	1.339	-	405	786	370	363	191	391
17.	31.4	30.4	24	,	•	0.64	. 4 5 5	. 4 3 3	4 33	455	433	1.366	£0.4	412	384	384	. 377	191	377
• •	7.	0.	*	-398	62.20	06.7	. 445	. 443	4.13	. 443	. 4 4 5	1 376	0.1	424	386	E 0 +	₩.	388	381
	3.	37.	7	-203	5 .0372	4 30	. 491	. 491	5 T	. 419	4 3 3	1.360	4119	412	378	378	368	373	) h
30.0	30.7	37.3	23.	-416	2920. 2	490	475	475	475	÷.	475	1.363		416	372	372	372	387	372
	2	7.	P 1			7.	9	4.0	0	9	9.	1.358		000	370	378	363	37.	370
2.5		9	23		86.20	067	. 518	8	=		4.4	1 360	•	=	363	380	337	365	365
			9 6		6000		0 0	0 0	633	E F Y	433	363		0 !	6 / E	3.3	60 i	9 7 9	371
					00.00			7 2 3				700	7 6		2 1	9 9	,		367
. 52	2 2		7		00000			9					•						
37.0	7.62	72	23		0963	490	529	85.9	•	•	*	466				9		9	0.00
<b>31</b> . •	23.5	35.1	23.1	-242	8 0493	490	. 522	. 322	138	8 2	438	1.397	413		35.4	8	828	321	, C
83.0	29.1	34.9	23	-255	6 .0462	06.6	5.67	. 907	205	422	422	1.354		-	625	3 2 2	346	191	2 2 2
•		7.7	23	-257	3 0470	0.5	=		:	403	:	1 347	459	450	377	369	343	169	96
31.0	20.0	34.4	22.9	-262.	2 0479	4.90	477	. 477	477	477	477	1.347	9 7	425	372	372	346	3.55	5.5
72.	20.5	34.0	22.8	-539	2060. 8	060	463	763	. 463	. 463	£ 9 #	1.359	410	9.5	0.0	376	347	96.5	98.6
33.	<b>5.</b> 6.	B . R	22 7	-278	0269	•	. 443	936	443	4 4 3	4 4 3	1.334	457	457	39.1	391	348	364	335
34.0	2. 0.2	33	22.7	-284.0	0519	06.	528	523	433	433	433	355	423	433	387	377	350	330	350
														1	:				,

\*\*\*\*\*\*\*\*\*\* Test Configuration 5: Two 2.54-cm Nozzles Scaling Run 63, 1 Table 40A はちょうりょうしょう こくしょうりょう ちょうりょう しょう こくこい こくりゅう ララティス ちゅうりゅう りゅうしゅん ちゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう しゅうしゅう フェート こくしょう こくしょう こくしょう こくしょ こうしょ しゅうしゅう フェール こうしゅう フロース アンストン アンストンストン アンストン アンストンストン アンストン アンストンストン アンストン アンストン アンストン アンストン アンストンストン アンストンストンストンストン 

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Table 40B — Inferred Pressurant Distribution, Scaling Run 63, Test Configuration 5: Two 2.54-cm Nozzles

	•	•								Δ,	ressurant	Pressurant Fractions (X) at Locations	(X) at 1	ocations	_				
-3	-8	:0	r.Ô	90.	B/0	<b>~</b>	-	7	m	4	v,	٠	7	∞	•	01	=	13	=
2000	1784 23	HO HA	7 E G																
•	22.2	22.5	£3. 2	£. 2	000000	000.0	0.000	000.0	000.0	000.0	0000.0	0 000 0	0 000	0000	000	000.0	0000	000.0	
	23.1	23.1 23.1 2. Entry Defin	24.3	1.96.4	9.2872	. 021	1.320	1.320	124	. 754	320	114	E 67 .	M .	9 2 9	9 8 9 7	. 462	201	660'-
			24.4	4.44	6.1333	147	241	7.1	. 632	9	•	241	241 -		133	•	- 211	- 093	0
	33	9.0	2	4		254	274	4.28	306	306	351	331	228	1 20	166	0.50	680	960	1 43
•	36.7	4 24	25.0		. 9597	330	356	413	420	413	10	384	322	270	282	<b>P</b>	. 235	. 264	287
	7	7	56.0	<b>o</b>	.7405	98E	392	445	4 4 5	4 5	392	45	786	338	36.8	323	328		200
•	6.	-	2 5	•	6248	. 429	0.	476	<b>433</b>	476	<b>0</b>		¥	80	4.	<b>C</b> 0 <b>+</b>	0	0	3 9 8
~	1 M		27.2		5938	463	475	. 475	475	47.5	£ 4	475	47.1	462	458	4.36	67	453	466
•	2.6	000	27.5	6 E 2	4921	490	910	910	•	# .	=	488	181	493	48	•	4 8 0	•	475
VALVE	FULLY	CL 08ED																	
•		6.9		6.	1040	489	. 497	. 497	497	. 497	497	<b>49</b> 4	<b>78</b>	488	479	479	429	484	479
• .		47 7		7.7	. 1630	<b>61</b>	. 529	. 4 8 2	. 4 8 2	7 .	4 8 2	7	. 492	<b>.</b>	<b>7</b>	487	417	967	6
11.0		• •		•	9660	489	. 312	2 6	~ <b>8 7</b>	<b>~87</b>	<b>~ 8 4</b> .	-	497	305	485	4 8 2	. 468	477	477
12.4		46.2		w. M	.0772	694	161	18	4.04	194	164	464	214	304	6.4	479	439	<b>4</b> 8 <b>4</b>	479
13.0		5.5	23	<b>~</b> ∶ <b>6</b>	7620.	684	. 527	205	505	476	205	924	. 512	205	19	994	9 9 9	471	924
14.0		:		€ . B	.0823	489	. 303	203	303	303	503	303	200	200	474	6.2	4 53	4.38	463
13.4		4	23	0. <b>4</b>	.0832	<b>.</b>	. 497	497	1497	497	497	- 497	. 50B	503	492	.471	094	471	471
16.0		<b>~</b> E <b>†</b>	23	٧.	0.05.0	617	- + 3	. 491	164	164	491	=	205	205	403	485	4.4	480	400
17.0		£ .			. 0297	<b>68 7</b> .	. 533	478	4.4	<b>1</b> 2	478	4 2 8	203		•	4 9 4	m -	. 489	4 2 8
	n + r	-	25.1	<b>8</b> .	9090		. 323	133	493	. 467	<b>29</b> •	<b>29</b> • .	206	206	193	4 9 3	47	<b>78</b>	8.4
19.0	34.1	42.8	23.1	<b>₹</b> . <del>1</del>	8060.	604	205	305	. 502	305	205	9 + .	505	208	480	483	480	180	4.68
<b>5.</b>	33.8	<b>+</b> 2 <b>+</b>	24.9	6.	.0628	489	. 490	490	490	490	490	490	964	208	490	490	479	479	473
21.0	73.7	<b>4</b> 2	24.5	n	0350	489	537	473	479	47.9	479	479	305	208	<b>4</b>	205	897	479	474
<b>3</b> . <b>6</b>	1	-	24.7	3.1	.0633	684	. 527	. 327	894	468	894	B 9 .	510	210	492	492	4.4	480	-
23.0	11.2	-	<b>~</b> *	9. 1	.0333	489	. 519	. 31.9	4.59	459	459	459	525	301	201	501	424	495	483
24.0	73	41.2	<b>34</b> .6	9.	0337	684	200	300	300	200	200	<b>+</b>	500	200	488	500	4 20	485	485
25.0	32.6	• •	24.3	. A	6890.	489	489	489	4.89	489	4.0	458	205	513	489	501	4	485	485
36.4	32.7	1) 0 <b>4</b>	24 4	9.1	0352	684	481	481	181	18	- B	=	306	306	<b>†</b> 6 <b>†</b>	512	4 7 3	489	4 98
27.0	32.5	F .	<b>5 7</b>	۲.۷	. 0357	489	470	532	470	420	470	0.4	205	.503	493	.514	4.6	489	489
28.0	32.4	1.0	24.3	1.7	.0362	489	. 517	. 317	. 517	+2+	¥ 2 ¥	+2+	494	303	498	503	4 2 9	479	479
29.0	32.1	39 6	24.2	en m	.0740	489	. 511	. 511	511	9 .	9 + 1	¥	115	511	204	511	425	491	-6
36.0	12.1	39.6	24.2	0.0	0.0000	<b>68 7</b> .	498	498	498	. 463	100	<b>433</b>	204	511	491	511	. <del>1</del> 8 8	482	485
31.0	3	39.2	3 <b>+</b> 2	9. M	.0762	684	P # 1	. 483	£84	483	4 8 3	483	503	964	309	3c3	470	430	<b>4</b> 8 3
32.0	31.6	38.9	24.0	<b>8</b>	0380	489	478	478	478	478	47	478	498	511	2	510	4 8 4	<b>78</b>	¥.
33.4	31.5	38.7	23.9	6.1	9660.	611	530	530	£9 + .	£ 9 † .	463	<b>69</b>	. 496	496	503	517	469	483	4.83
7.	31.3	38	23.9	-	.0463	489	523	325	437	457	457	<b>25</b>	491	502	498	515	÷	491	•
XXX																			

Table 41A - Scaling Run 64, Test Configuration 4: One 2.54-cm Nozzle

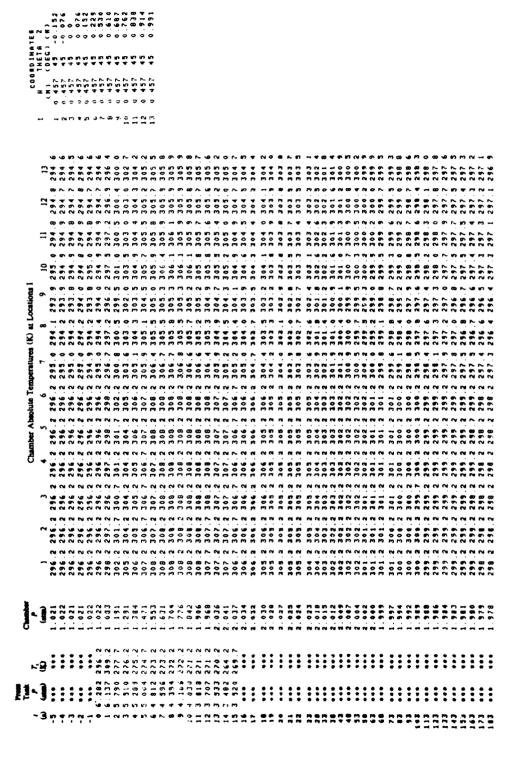


Table 41B — Inferred Pressurant Distribution, Scaling Run 64, Test Configuration 4: One 2.54-cm Nozzle

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Table 42A - Scaling Run 65, Test Configuration 4: One 2.54-cm Nozzle

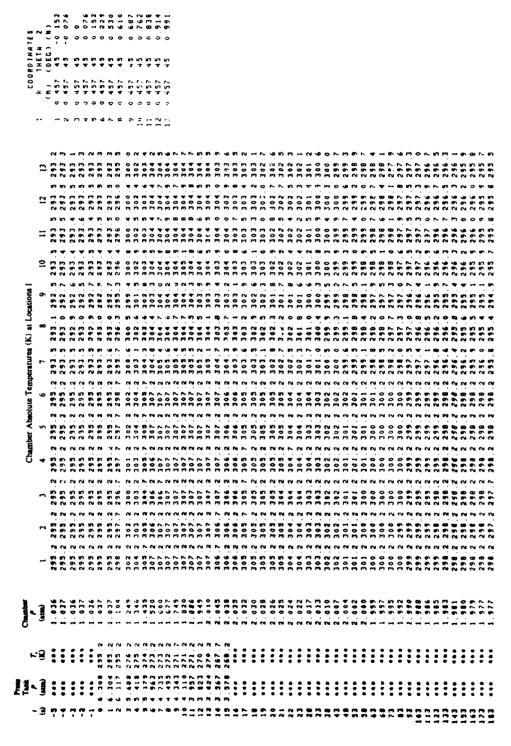


Table 42B — Inferred Pressurant Distribution, Scaling Run 65, Test Configuration 4: One 2.54-cm Nozzle

Test Configuration 4: One 2.54-cm Nozzle Scaling Run 66, ١ 

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Table 43B — Inferred Pressurant Distribution, Scaling Run 66, Test Configuration 4: One 2.54-cm Nozzle

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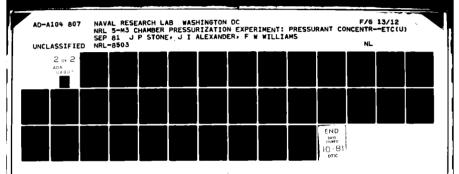
Set 1, Table C - Mean Values of All Quantities, Scaling Runs 23-31

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Set 2, Table C - Mean Values of All Quantities, Scaling Runs 32-34

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Set 3, Table C - Mean Values of All Quantities, Scaling Runs 35-37

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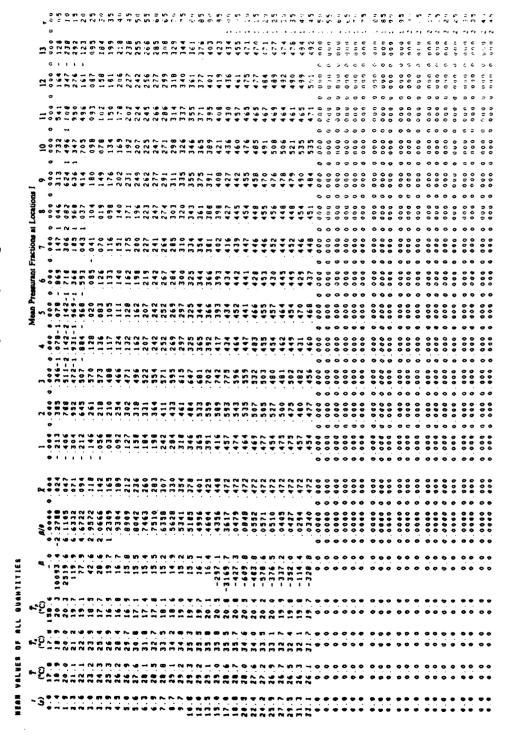
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Mean Values of All Quantities, Scaling Runs 39-41

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Set 4, Table C

Set 5, Table C - Mean Values of All Quantities, Scaling Runs 42-44



Set 6, Table C - Mean Values of All Quantities, Scaling Runs 45-47

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Set 8, Table C - Mean Values of All Quantities, Scaling Runs 51-53

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Set 9, Table C - Mean Values of All Quantities, Scaling Runs 54-56

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Set 10, Table C - Mean Values of All Quantities, Scaling Runs 58-60

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## STONE, CORLETT, ALEXANDER, AND WILLIAMS

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TO THE PROPERTY OF THE PROPERT  $\alpha$  control of the c OND TO BE ON TO THE ONE OF THE ON Mean Values of All Quantities, Scaling Runs 61-63 Set 11, Table C -\*\*\*\*  $\bigoplus_{i=0}^{k-1} \mathsf{w} + \mathsf{w} +$ 9 VALUES 

NRL REPORT 8503

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103

Set 1, Table D — Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 23-31

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Set 2, Table D — Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 32-34

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018	127	056	. 053	032	045	.013	. 01	.009	027	. 019	012	0	24	1	45
. 411	0.49	065	061	032	030	008	0 11	013	039	016	019	0	30	1	50
634	<b>9</b> 3 ن	0 6 9	060	032	934	002	0 1 5	.016	. 0 4 7	023	024	0	32	1	55
0 + 3	041	054	041	016	. 043	013	0 1 1	015	.045	. 024	024	Ú	24	ı	60
436	0.40	0.47	049	006	036	010	0 1 5	5 .014	044	019	018	Ú	14	i	€5
0 ! 5	049	047	. 690	039	015	010	0 1	2 016	045	017	014	0	11	1	70
u 2 3	037	0.18	690	043	003	011	01:	2 .015	035	.019	016	C	0 4	ì	7.5
051	3 4 7	0 0 3	V 8 4	046	002	012	0 1	012	.031	016	019	0 0	ψÜ	1	80
046	.014	0.28	956	033	. 022	.011	. 0 0 6	013	033	008	022	0	01	ł	85
436	J 2 9	044	047	016	034	009	0 1	3 016	031	005	018	U	0.7	1	90
037	44.8	0.47	051	003	038	018	. 62	016	029	010	015	0	16	ı	95
446	534	0.46	466	017	03€	.021	Q 2 1	. 023	.030	008	015	ú	14	2	00
040	0.21	046	050	026	021	027	. 0 3	. 027	038	. 014	023	0	14	2	05
. 0 4 5	012	055	056	015	. 041	034	044	. 434	047	017	030	. 0	20	2	10
067	013	058	064	017	042	040	. 0 4			018	027			2	15
084	032	962	080	. 032	032	052	. 05	. 044	. 0 3 3	. 026	028	0	18	5	20
063	033	063	. 0 8 1	033	015		0 3		050	023	029				25
.038	036	057	084	036	012		0.4		0.18	020	027				10
.043	031	052	166 447	030	026		041		010	023	023				35 40
. 0 3 4	012	044	046	017	434		04			027	029				45

Set 3, Table D — Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 35-37

					Locati	ons I						
1	2	3	4	5	6	7	8	9	10	11	12	13 +
		0.000				0.000				4.000		0.000 0 00
1.682	1.535	2.419			1 694	1 040		2.102		1 760	2 320	.165 05
1.921	1.409	2.297	2 032 2		1.895	. 8 6 6	4.245	2.054	2.258	1.706	2.119	523 10
2 234	1 285	2 170	1 804 2	635		.764	3.957	2.009	2.279	1.683	1.919	.868 15
2.593	1.161	2.065	1.577 2	. 826	2.472	.756	3.687	1.970	2.325	1.692	1.721	1.215 20
2.904	1.040	1.910	1 352 1	.061	2.014	. 447	3.441	1.933	2.393	1.733	1.525	1.562 25
3.437	. 755	1.775	. 958 3	.379	3.232	1.035	3.195	1.032	2.517	1.025	1.265	1.934 .30
3.923	. 5 2 7	1.743	623	.763	3.697	1.260	3.498	1.874	2.747	2.004	1.080	2.306 35
4.083	. 342	1 701	390 3	. 850	3.845	1.381	2.831	1.829	2.746	2 022	. 904	2.446 .40
3.528	200	1.296	249 3	.317	3.310	1.204	2.316	1.547	2.251	1.684	.751	2.058 45
2.984	.078	. 917	. 145 2	. 803	2.790	1.024	1.019	1.287	1.779	1.361	. 623	1.673 .50
2.440	.083	. 543	. 147 2	. 269	2.269	.844	1.323	1.430	1.307	1.041	.498	1.286 55
1.860	. 233	. 119	251 1	.741	1.712	.647	. 8 0 1	. 709	.797	. 670	.330	.886 60
1.464	. 332	. 150	. 355	373	1.340	. 515	. 470	. 502	.491	. 413	224	.608 65
1.361	314	. 119	330	. 2 6 8	1.260	.483	. 440	. 487	. 5 1 0	. 347	. 222	.524 .70
1.259	. 298	. 091	. 322 1	203	1.192	. 451	. 413	. 475	. 531	. 282	. 2 2 1	.439 75
1.165	. 294	068	. 309 1	. 126	1.110	. 432	. 362	. 439	. 522	. 229	. 229	.378 80
1.120	276	063	. 326	. 097	1.070	. 436	. 364	. 401	.450	. 230	. 221	. 367 65
1.074	253	065	344	.062	1.025	.440	. 367	. 363	.379	. 231	.207	.351 .50
1 030	. 251	069	347	.024	. 991	. 4 0 0	. 361	. 341	. 351	. 235	. 186	. 328 95
986	. 288	. 214	. 363	.977	. 977	.311	. 293	. 274	. 293	. 245	. 229	272 1 00
977	.274	. 164	. 371	970	970	.324	. 311	287	300	. 224	204	. 246 1 05
983	.287	169	. 363	. 9 8 1	. 981	. 324	. 314	. 294	. 296	. 231	. 209	285 1 10
. 593	. 300	. 176	. 355	. 991	. 991	. 322	. 318	. 302	. 292	. 236	. 215	. 202 1.15
. 999	. 297	. 172	363	. 999	. 999	. 329	317	. 302	. 294	. 235	. 221	. 290 1 20
1.006	.294	175			1.006	.337	313	. 300	. 2 5 5	231	. 224	298 1.25
1.013	292	178	377 1	013	1.013	346	. 311	. 299	. 297	. 228	. 229	.365 1 30
1 023	. 292	185	. 378 1	.022	1.023	349	. 317	. 299	298	233	. 234	.304 1 35
1.037	. 290	. 193	. 380 1	.029	1.037	.349	. 327	. 300	. 299	. 243	239	.302 1 40
1.047	. 289	. 201	392 1	. 033	1.050	.346	335	. 300	.301	. 251	. 244	300 1 45
1.053	. 294	. 207	. 393 1	. 032	1.064	. 342	. 327	. 299	. 295	. 256	. 250	304 1 50
1.059	.301	. 211	.401 1	.036	1.072	. 342	. 318	. 299	. 289	260	. 256	.311 1 55
1.068	307	. 217	.409 1	. 0 4 5	1.074	343	. 308	. 301	280	. 264	264	.318 1 60
1.077	312	. 227	399 1	054	1.069	342	. 312	. 303	. 201	. 266	. 266	316 1 65
1.083	. 317	2 3 8	. 305 1	.062	1.066	. 341	. 318	. 304	. 285	267	. 264	.312 1 70
1.083	. 325	. 245	366 1	.065	1.073	. 342	. 327	. 104	. 291	268	. 263	.310 1 75
1.081	. 336	. 250	. 344 1	.066	1.081	.344	. 329	312	296	265	. 260	. 313 1.80
1.079	. 345	. 255	. 322 1	.068	1.090	. 3 4 5	. 331	. 321	. 300	. 264	. 250	.316 1 85
1.084	. 355	. 260	314 1	.069	1.092	343	327	. 128	.302	. 265	257	319 1 90
1.089	. 342	. 265	. 328 1	.071	1.094	. 341	. 327	. 327	. 302	266	257	. 325 1 95
1.096	. 323	. 269	350 1	.074	1.096	.330	. 326	. 126	.304	265	. 256	331 2 00
1.091	303	. 280	360	.081	1.100	. 334	. 326	. 324	. 305	. 266	. 263	.335 2 05
1.081	. 307	. 291	344 1	. 088	1.099	. 331	. 328	. 319	302	. 271	.267	.334 2 10
1.071	.316	. 301	320 1	.091	1 098	332	. 332	312	297	. 279	269	330 2.15
1.071	335	313	. 3 0 3 1	088	1.100	. 332	. 334	304	. 250	283	268	323 2 20
1.080	. 352	. 322	. 306 1	.087	1.109	. 331	. 330	. 304	285	282	. 271	.320 2.25
1.088	. 366	. 329	. 315 1	089	1.118	. 330	. 323	307	.279	. 291	274	.318 2.30
1.091	.372	. 333	. 318 1	.097	1.122	.330	. 317	. 315	.271	. 281	. 291	. 319 2 . 35
1.088	.357	. 329	. 319 1	. 097	1.119	.320	. 317	. 317	. 269	. 286	. 286	322 2 40
1.084	. 332	. 319	. 121 1	. 095	1.116	. 325	322	. 315	.272	. 293	290	330 2 45

Set 4, Table D — Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 39-41

					Lo	catio	ns I													
ì	2	3	4	5	6		7	8		9	1	0		11		12		13		7
0.000	0 000	0 000	0 000	0 000	9 00	0	000	0 000	0	000	0 0	00	0	000	0	000	0	000	0	0.0
1 042	1 132	897	856	940	98	6 1	.078	. 510		267	5	30	4	297	3	158		629		u S
679	729	956	82	896	. 58	6	.792	. 495		470	8	90	2	719	1	960		657		10
486	375	1 091	59	986	44	9	492	611		497	9	33	1	560	1	201		574		15
. 309	104	992	920	022	46	6	148	. 5 9 1		364	6	90		748		857		346		20
2:8	058	644	654	567	42	3	073	451		227	4	96		580		671		193		25
139	.076	; 008	222		36		115	382		130	5	38		153		3 0 8		215		30
151	1 U 9	1 274	281		41		131	514		165		94		106		366		300		35
930	052	910	179		. 24		969	. 329		119		38		067		223		179		40
v32	032	309	01		09		010	109		056		52		436		064		047		45
911	035	051	051		06		032	024		024		13		028		030		023		50
033	0.23	443	64		04		029	034		023		14		026		035		018		55
447	039	432	626		ů3		027	035		021		14		020		039		016		é u
037	024	J 2 1	02		0.4		025	030		021		17		006		046		015		65
031	.026	022	43:		02		018	022		018		22		005		051		006		70
. 046	021	027	43.		υJ		013	J 18		416		23		009		047		001		15
. 030	006	017	. 61		02		009	017		007		06		016		023		010		80
926	047	010	. 404		.00		009	. 008		005		05		. 025		012		012		85
. 043	.027	910	00		.00	-	013	700		015		111		012		008		013		90
. 043	. 051	006	01		01		027	014		015		06		015		024		040		95
. 025	019	054	.06		03		032	021		015		21		065		042			1	90
. 014	014	. 018	011		01		010	016		001		10		030		023		015	1	V 5
. 428	029		04													024			ì	
. 035	036	044	. 030		03		022	937		.028		34		016		.031		023	i	10
047	043	042	010		01		010	.017		. 02 r		19		008		.031		009	1	15 20
036	042	024	42		. 03		019	. 416		. 028		24		016		039		016	i	25
059	040	053	000		01		.009	018		015		18		014		034		025	i	30
. 066	. e 3 o	047	03		0.1		.021	. 925		029	. 0	31		017		044		038	1	35
. 050	017	049	02		. 05		025	024		035		26		013		043		044	í	40
048	. 050	. 0 6 1	01		. 03		.018	. 024		. 029		32		003		040		0.38	ı.	
. 037	. 675	035	01		. 0 1		. 023	. 023		. 925		30		. 005		034		. 0 4 0	1	50
. 056	070	.049	45		0 2		027	0 1 4		039		49		007		047		048	1	3 5
. 070	071	. 0 # 0	0.4		0.5		.018	. 030		938		52		021		033		9 2 0	ı	60
.052	.077	.063	06		. 04		014	028		936		67		035		066		036	1	20
. 076	076	038	936		. 04		.009	013		435		52		033		076		057	i	25
.079	075	024	. 01		. 05		.007	0 3 5		019		38		032		078		0 6 3	i	80
. 081	.084	072	934	034	. 00	6	.013	029		021	0	39		045		081		070	ı	65
. 070	. c ? 2	065	. 96		. 04		.016	. 0 3 8		.027		34		044		086		0 4 2	ı	90
. 095	v 5 7	057	05(		03		025	. 042		030		40		034		077		056	1	95
. 071	065	v <b>6</b> 5	031		. 04		059	. 036		031		19		031		072		059	2	ų o
462	462	462	463		46		496	424		. 340		65		413		426		430	2	0.5
. 453	455	435	451		45	-	. 500	. 486		356		71		420		421		437	2	10
0 000	0 000	0 000	0 000		0 00			9.000	0	000		00	0	000	0	000	0	000	2	15
0.000	0 000	0 0 0 0	0 000		0 00			0 000	٥	900		00	0	000	0	000	0	000	2	50
0.000	0 000	0 0 0 0	0.000		0.00			0 000	0	000		00	0	000	0	000	0	000	2	25
9.000	0 000	9.090	0.000		9 90			9.990	¢	. 000		90	0	000	0	000	0	000	2	30
0 000	0 000	0.000	0 000		0 00			0.000	6	000		00	ø	000	0	000	0	000	2	35
1.000	0 000	0.000	0 000		0.00			0.000		000		00	¢	000	0	000	0	000	5	4 (1
0 000	0 000	0 000	0 000	0 0 0 0	0 00	0	000	0 000	٥	000	0 0	0.0	đ	400	٥	000	a	080	٠.	45

Set 5, Table D - Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 42-44

				Locations 1				
i	2	3	4 5	6 7	8 9	10 11	12 13	7
4.400	0.000		0.000 0 000	4.400 0 000	0.000 0.000	0 000 0 000	0 000 0.00	
. 565	2 834	776	4 261 4.261	1.602 994	3.660 1.007	1.950 .999	.739 1.36	6 .05
1.157	5.687	1.576	8 490 8.480	3 176 1.985	7.255 2.037	3.999 2.111	1.480 2 66	i <b>a</b> 10
.770	4.408	1.102	7.060 7 074	2.777 1.677	5.891 1.609	3.363 1 849	1.271 1.97	8 15
. 330	2.012		3.250 3 312	1.244 964	2.677 .727	1.508 .820	.720 .90	6 20
. 961	277	. 0 8 4	143 .035	206 341	370 .134	101 136	.220 .23	
. 036	.163	162	.052 .067 028 .025	123 121	.116 943 975 938	092 102	048 .01	
. 073	.062	090	028 025	961 051	026 026	.040 .054	027 01	
. 065	. 052	. 056	462 469	025 039	010 011	039 039	040 02	
. 053	.048	. 030	069 .069	.033 011	.015 006	.026 025	037 .02	
. 042	.046	046	.059 059	.060 .012	019 .008	.021 .010	.029 .01	
. 028	. 0 6 6	043	. 657 . 657	.057 012	.015 005	014 .012	.036 .01	
	062	. 0 0 7	016 .016	.061 .016	.013 015	.024 016	.033 .01	
. 010	. 0 3 3	. 0 2 5	.433 .033	.036 .015	017 .001	.016 018		
. 021	.067	. 051	.050 .050	.041 .007	.010 015	.019 .015		
020	.054	038	.448 .048	048 .009	009 014	.017 .015		
. 616	.075	. 011	016 049	.049 .014	.014 000	.017 .025		
. 036	.055	. 004	.030 .042	.042 016	.013 009	.024 .021		
. 071	.011	. 038	.967 .014	.014 .014	023 014	.020 .024		
. 024	.019	065	949 949	.049 012	.005 .014	018 003		
048	.049	. 068	.041 .049	.056 .009	.021 .012	023 016		
. 026	.022	. 059	.026 .044	.044 .008	.023 .030	.024 .003	.020 00	
. 981	.020	. 071	.052 .048	053 .007	.013 .009	.019 .004	015 .00	
. 030	.096	. 057	.041 041	045 011	.002 .010	.007 .006	017 .01	
. 024	.031	. 061	.024 .024	.053 .009	,004 .010	.018 .003	.010 ,00	
. 058	.028	098	045 .051	.069 .017	.013 .427	.016 .010	.004 .00	
. 039	039	062	040 .026	.040 .010	016 014	.018 022	017 .02	
042	110	.063	.040 .051 .038 .062	043 019	.029 .027	.023 .031		
. 101		.068		.037 .028	.035 .037	026 014	0.008 0.00	
4.000	0.000		0 000 0 000	0.000 0.004	0.040 0.000	0.000 0.000		
0.000	0.000		0 000 0 000	4 400 4 004	0.000 0.000	0.000 0.000		
4.000	0.000		0 400 0 000	0 000 0 000	0.000 0.000	0.000 0.000		
4.000	0.000		0.000 0.000	0 000 0 000	0.000 0.000	0.000 0.000		
4.000	0.000		0.000 0.000	0.000 0.000	0 000 0 000	0.000 0.000		
0 000	0 000		0 400 0 000	0 000 0 000	0 000 0 000	0 000 0 000		
0.000	0.001		0.000 0.000	0 000 0 000	0.000 0 000	0 000 0 000	0.000 0.00	
0.000	0 000		9.000 0.000	4 400 0 000	0.000 0.000	0.000 0 000		
0.000	0.000		0 000 0 000	0 000 0 000	0 000 0 000	0.000 0 000	0 000 0 00	
4 400	0 000		0 000 0 000	0 000 0.000	9 999 9 999	0.000 0 000	9 000 0 0	
9.000	0 000		0 000 0 000	4 000 0 000	0.000 0 000	0.000 0 000	0 000 0 0	
4 600	0 000		0 000 0 000	0 000 0 000	0 000 0 000	0 000 0 000	0 000 0 00	
0 000	0 000		0 000 0 000	0 000 0 000	U UOO O UOU	0.000 0 000	0.000 0.00	
0.000	0.000		0 000 0 000	9 000 0 000	9.000 0.000	4.000 4 400	0 000 0 0	
0 000	0 009		0 000 0 000	0.000 0.000	0.000 0.000	0 000 0 000	0.000 0.00	
0 000	0 009	,	0 000 0 000	0 000 0 000	0 000 0 000	0 000 0 000		
0.000	0.009		0.000 0.000	0 000 0 000	0.000 0.009			
0.000	0 600	1 000	v 040 0 000	0 000 0 000	0 000 0 000			
0.000	0 . 0 0 9		0 000 0 000	0 000 0 600	0 000 0 000			

Set 6, Table D — Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 45-47

											L	оси	tions 1														
1			2		3		4		5		6		7		8		9		10		11		12		13		Ť
9.00	0	٥	000	0	000	0	000	ij	000	ď	000	0	000	¢	dgi	v	000	U	u դ ե	0	000	O	000	0	000	0	0.0
. 50	3		873	4	540	1	693	1	842	:	624		508		759		30.7		5.52		5:3		4 . 6		7 e :		a 5
1.16	0	4	212	7	852		444	1	261		408	1	293	1	4 8 9	1	4 v 3	1	625	ı,	J06		930		290		10
1.35	?	5 .	141	8	461		100	1	\$57		166	1	4 6 9		4.77	1	8 .	2	4 10,	:	752	1	091		414		15
. 64	3		045		172		042		103		++ 3 G		620		600		#33		v 35		010		0 0 8		639		20
. 00	9		036		076		042		689		1149		018		416		019		014		016		032		030		25
02			032		0 6 4		030		0.85		0.3.2		018		U 2 1		U Q 4		025		010		032		043		30
. 04	1		085		038		056		929		045		023		008		. 009		013		004		004		014		35
. 01	5		026		095		042		076		034		005		011		016		015		011		012		. 022		40
. 01			063		089		054		107		1148		017		014		G 1 9		012		026		013		044		4 5
. 02			013		. 480		. G & 5		0 6 6		48.		039		435		. 913		024		005		.017		025		. 50
. 03			074		. 0 ? 8		037		0 # 1		037		006		0 1 8		004		013		011		022		030		55
. 05			084		078		037		079		031		013		011		014		013		009		015		015		60
. 01			048		056		u 3 7		083		0-7		6		0.23		11		014		010		010		027		70
. 01			055		090		033		080		#33		012		0.27		007		027		021		020		034		7.5
. 01	1		053		047		013		093		046		004		021		021		021		024		023		. 028		60
. 60	7		973		105		946		. 996		. 946		005		. 028		.008		021		013		024		. 0 2 4		6.5
. 01	5		011		108		. 096		.089		037		019		016		006		032		018		025		021		90
. 65	,		065		124		958		002		. 055		012		. 0 0 8		917		.012		.007		. 0 1 1		. 0 2 0		. 95
. 06	8		068		183		948		.093		. 956		023		. 025		. 011		014		013		025		032	i	0.0
0.00	0	0	000	0	000	0	000	ı)	000	0	000	0	000	0	.000	٥	000	0	000	0	000	0	000	0	000	1	95
0.00	0	4	0 4	0	000	0	000	0	000	0	.000	0	000	0	000	0	000	0	000	0	000	٥	000	0	. 444	ì	10
0.00	٥	0 .	000	9	040	0	400	0	000	ø	000	0	900	11	000	٥	000	0	000	Q	000	0	000	0	. 000	1	15
9.00	0	٥.	000	0	000	Ü	000	ó	000	a	060	Ò	0.60	e	000	6	000	Ó	000	0	000	0	000	0	000	i	20
0.00	0	0	000	0	0 0	0	000	0	0.00	0	000	0	000	o	a a u	61	0.00	0	000	0	000	0	000	0	046	1	25
4.60	0	q	000	0	. 0 0 0	ø	404	a	0.00	u	000	u	000	ø	400	U	400	U	000	U	000	U	000	0	000	1	30
0.00	0	9	000	0	000	0	000	G	6 11 6	r)	600	0	0.60	6	6 9 6	Ģ	0.00	n	000	17	000	0	000	0	000	1	. 35
9.00	0	٥	000	0	000	ø	000	0	000	a	Sec.		000		1.00	ı	48.45	6	6.00	4)	0.00	ø	0 11 0	0	000	1	40
0.00	0	0	004	1	000	0	000	a	0 0 0	ø	grid	ø	6 0 3	đ	000	v	000	0	000	0	000	0	000	0	. 000	i	45
4.00	0	0	000	0	000	0	000	0	000	tì	069	a	0.6.0	t	0.00	Ġ	400	ô	000	0	000	0	000	0	000	ı	50
0.00	0	٥	000	0	000	ø	000	13	000	4)	060	6	to il tr	0	0.00	۲,	996	0	. 0 0 0	Q	.000	0	000	0	000	i	55
0.00	0	0	000	0	0 0 0	0	000	t)	0.00	0	0.014	Ó	640	**	000	ø	800	ø	000	¢	000	0	000	0	000	ł	60
0.00	0	0	000	ŋ	600	0	006	11	600	0	0.6 0	6	0.60	Ð		4.	466	U	606	ų	000	0	000	Ú	0 4 6	1	• 5
0.00	٥	٥.	000	0	000	Ú	000	11	0.06	()	666	ř.	0.00	0	000	6	000	0	000	0	000	0	000	0	. 0 0 0	1	70
C . 00	0	٥.	000	0	600	Ģ	0 0 0	a	440	đ	0.50	ø	ó a d	.,	200	Ġ	4.		0.96	9	000	a	000	a	000	1	75
0.00	0	0	000	9	000	0	000	a	0.00	0	ge o	0	000	91	0.00		0			ij	0.00	v	600	0	000	i	60
0.00	0	0	000	9	000	0	000	ı)	000	41	000	0	000	11	2.00	¢.	12.00				006	6	000	0	000	1	95
4.00	0	0	000	9	000	9	900	ø	0.00	tj	000	į,	Q13. 11	.4	4 (15)	ţ.	11.45		, (	ti	0.00	v	000	ø	6 9 9	ı	50
0.00	0	0	000	0	000	ú	000	a	000	0	000	0	000	41	000		44.11	vi.	0.00	0	060	v	000	0	000	1	95
9.60	ò	0	000	Ó	000	٥	000	0	0.00	a	000	6	000	()	000	(1	000	0	000	0	000	0	000	0	000	2	00
0.00	٥	0	000	0	000	0	000	a	0.00	0	000	ó	000	0	000	ú	400	ø	000	4	600	0	000	0	000	2	. 05
0.00	ò	0	000	0	0.00	6	600	-	0.00	0	000	6	0.00	0	000	0	000	n	000	0	000	Ó	000	0	000	2	10
0.00		Ó.	000	ó	900	ú	000	4	000	ò	000	ė	000	0	000	Ü	000	0	000	0	000	ò	000	o	000	2	15
0.00		ò	000	ě	000	ò	000	ñ	0.00	4	000	ò	600	0	0.00	ó	000	o	000	đ	000	ò	000	à	000	ž	20
0.00		ó	000	0	000	ò	000	ó	000	0	000	ò	000	0	000	ö	000	ŏ	000	ò	000	ŏ	000	ő	000	2	25
0.00	-	o.	000	0	000	ŏ	000	ň	000	0	000	ő	000	0	000	ŏ	000	ŏ	000	ō	000	ō	004	ŏ	000	2	30
0.00		ŏ	000	0	040	ō	000	0	000	9	000	o	000	ü	0.00	ō	Ond	n	000	a	000	0	000	a	000	2	35
0.00			000	ű	040	Ü	900	0	000	4	000	ò	0 0 0	ü	000	v	000	u	000	ú	000	ō	000		040	ž	40
0.00			000	0	000	ŏ	000	ò	0.00	1)	000	ě	000		600	Ü	000	ų	600	ō	000	ò	000	ō	000	2	45

Set 7, Table D — Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 48-50

					Loc	ations I							
l	2	3	4	5	6	7	8	9	10	11	12	13	7
4.400	0.000	4.040	0 000	0.000	0 000	0 000	0.000	0.000	0.000	0 000	0.000	0 000	0 00
1.019	. 920	962	1.149	1.134	1.019		1 151	. 486	. 373	. 793	834	. 432	0 5
. 583	. 629	692	839	832	. 743	.301	696	352	. 360	584	621	329	10
. 094	.032	. 228	163	163	126	219	370	491	140	104	123	097	15
. 266	.019	. 019	. 107	.111	. 064		1.120	. 984	.152	080	.110	. 0 5 7	20
. 110	.028	038	. 043	111	. 105	.091	852	. 084	.075	084	.077	. 0 6 1	. 25
. 173	.022	.072	.090	.055	068 089	117	.789	.078	036	057 044	059	048	. 30
. 129	.031	031	036	.116	129	077	793	081	693	045	055	049	40
. 139	.054	0 4 5	. 060	.136	144	006	807	078	073	057	060	054	. 45
. 096	.059	059	125	122	128	.075	510	07.	0.52	043	033	015	50
. 099	.059	065	100	.080	. 103	094	. 842	.063	.049	. 054	.048	054	. 55
. 499	.074	.071	106	071	099	067	858	070	.056	U46	.086	074	60
. 104	.086	.060	114	.114	. 104	.088	. 873	.084	069	. 042	057	057	65
110	. 066	079	100	.079	. 110	. 0 8 1	899	073	074	. 051	.054	049	70
. 108	.059	059	. 137	137	122	.089	932	079	066	046	.052	029	75
. 110	.061	061	145	. 145	126	090	950	087	.062	. 027	. 959	049	. 80
. 150	.063	. 063	. 142	. 142	. 150	.097	. 970	068	.043	. 039	053	. 044	65
. 162	.078	. 020	. 154	. 154	. 162	. 1 0 0	. 985	. 483	. 053	. 032	. 0 4 3	. 054	. 50
. 069	. 0 4 2	. 042	. 091	. 130	. 223		1.003	. 499	. 093	. 117	. 111	. 090	95
. 491	.026	. 131	. 116	. 116	. 157		1.036	. 124	. 120	. 104	.113	. 103	
0.00		0.000	0.000	0.000	0.000			0.000	0.000			0.000	1.05
0.000		0.000	0.000	0.000	0.000				0.000			0.000	1 10
0.000		0.000	0 000	0.000	4 000			0.464					1 15
0.000			0.000	0.000	9.000		0.000		0 000			0.000	1 20
4.000		9.000	0 000	0.000	9.000		0.000		0.000		0.000		1.25
4.400			0 000	0.000		0.000	0 639						1 15
	0.000			0.000	0 000	0 000		0.000			0 900	0 000	
0.000		0.000	0.000	0.000	9 900	U.000		0.000	0.000		0.000	9.000	1 45
0.000	0.000	0.000	0.000	0.000	0 000		0.000	0 800	0.000		0.000	9.000	1 50
			0.000		0.00		9.000					0.000	1 35
4.600	0.008	0.000	0.000	0.000	9 000	0.000	9.000	0.000	0.000		0 000	0.000	1 60
6.000	0.000	9 999	0.000	0.000	0 000	0.004	0.000	0.000	0.000	0 000	0.000	0,000	1 65
		9 0 9 0	0 000	0.000	0 000			<b>0</b> 000		0 000	0 000		1 70
• . • • •		0.000	0.000	0.000		4.000		0.000		0.000	0.000	0.000	1.75
	4.000	4.000	0.000	0.000	0.000	0 000	9.000	0.000	0.000	0.000	0.000	0.000	1 00
0.000		9 000	0.000	0.000	0.000		0.000	0.000	0 000	4.000	0.000	0.000	1 85
												9.900	
4.400			0.000	0.000	0 000		0.000	0 000	0.000	0 000	0.000	0.000	1 95
	0.000		0.000		0.000			0.000	0 000			0.000	
0.000		0 040	0 000		0 000	0.000	0.000		0 000		0 000	0.000	
1.000		0 000	0.400	6.000	4 400		0.040		0 000	0 000	0 000	0 000	2.15
		0.000	0.000		0.000			0.000	9.000		0.000		
		0.000	0.000	0.000	0.000			0.000	0.000	0 000	0.000	0.000	2 25
		0.000	0.000	0.000	0 000	0.000		0 000	0.000	0 000	0 000	0 000	2 30
0.000	0.004	9 9 9 9	0.000	0 000	0 000	0 000	0 000	0 000	0 000	0 000	0 000		2 35
4.600	0.000			0.000							0 000	0.000	
	0 000	0 000	0 000	0 000	0 000	0 0 4 0	0 0 0 0	0 000	0 000	0 000	0 000	0 0 0 0	3 45

Set 8, Table D - Standard Deviation of Mean Local Pressurant Fractions. Scaling Runs 51-53

						Locations	1						
1	2	3	4	5	6	7	8	9	10	11	12	13	7
4.000	0.000	0.000	0.000	0 000	0 000	0 000	0 000	<b>0</b> .000	0 000	0 000	0 000		0 00
. 502	.718	1.026	686	642	. 502	.316	. 9 8 8	435	518	306	239	399	0.5
. 272	. 375	1.376	. 521	700	272	.306	7 4 5	292	930	484	444	5 " :	10
. 202	.047	. 736	. 121	. 466	. 184	306	223	967	455	240	349	44.	: 5
. 390	. 410	. 157	. 347	256	357 392	355	430	233	163	237 361	257	. 298	2 0 2 5
.411	.545	462	. 545	.160	. 226	173	294	157	207	193	171	107	10
. 028	.066	. 117	068	055	. 109	.047	048	068	043	067	084	055	35
. 459	.044	.062	040	040	098	018	028	937	033	947	053	026	40
	036	. 033	. 036	036	081	005	. 023	012	018	029	032	014	45
. 045	.006	014	. 039	036	044	.009	. 024	045	010	024	017	010	30
	.016	. 014	. 031	.040	. 051		. 019	. 023	.004	. 020	015	. 010	3 5
	. 0 2 1	. 021	035	.026	. 051	. 014	. 0 2 5	. 609	.004	.012	.017	017	60
. 423	.012	. 0 1 2	. 012	.012	022	.022	. 0 0 9	. 012	.020	. 012	.006	009	6.5
. 006	.006	. 022	. 025	.025	. 014	.001	. 0 0 4	. 021	.011	. 003	.017	. 0 0 6	70
. 011	.022	. 036	.076	023	. 005	.009	. 015	024	. 022	. 009	.027	. 0 1 5	7.5
. 418	. 015	. 0 2 6	. 014	015	. 438	.007	. 9 9 5	. 023	.014	. 008	.017	. 015	. 8 0
. 014	. 019	. 019	. 019	.019	. 002	. 015	. 010	014	. 011	001	.004	. 0 2 0	8 5
. 416	.017	. 017	. 017	.017	. 444	.014	. 015	025	.048	. 016	.036	. 0 2 1	90
. 015	.024	.062	. 043	.062	. 015	017	017	02:	.004	022	.022	040	95
. 010	.026	.028	. 028	. 0 2 8	. 010	. 0 2 2	. 017	. 029	.004	.008	027		1 00
.005	.045	. 033	. 036	. 033	.007	.016	. 007	017	016	.018	.009		1 95
. 011	.032	. 032	. 032	.032	. 912	020	. 001	. 016	. 020	. 013	031		1 10
.031	.014	. 014	.051	.009	. 042	.013	.035	.004	.011	.015	.016		1.15
. 003	.039	.039	. 036	.039	. 005	020	013	.016	.020	013	.012		1 25
. 015	.033	.033	. 036	033	. 009	.029	030	.010	030	. 619	045		1.30
. 061	.017	. 0 2 6	. 062	.074	. 063	011	. 034	012	.018	.021	. 035		1.35
. 021	.031	. 031	.061	.031	. 021	.006	. 018	016	024	.030	.041		1.40
. 479	.429	429	. 429	. 429	479	500	. 481	. 488	508	. 484	501		1.45
4.000	0.000	0 000	0.000	0.000	0.000	0.000	0.000	0.040	0.000	0.000	0.000		1 50
	0.000	0 000	0.000	0 000	0.000	0.000	0 000	0.000	0.000	0.000	0 000	0.000	1 55
0.000	0.004	8.000	0.000	0.000	0.000	0 000	0 000	0 000	0.000	0.000	0 000	0.000	1.60
0.000	0.000	0.000	0.000	0.000	0.000	0 000	0.000	0.000	0 0 0 0	4.000	0 000	0.440	1.65
0.000	0.000	0.000	0.000	0 000	0.000	0.000	0.000	0.000	0.000	4.000	0.000	0.000	1 70
9.000	0.000	0.000	0.000	0.000	0 000	0 000	0.000	0.000	0.000	8.000	0 000		1.75
0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0 000	0.000	0 000	0 000		1.80
6.600	0.000	9.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0 300		1 45
0.000	0.004	0.000	0.000	0.000	0.000	0 000	0 000	0.000	0 036	0.000	<b>0 600</b>		1.90
0.000	0.004	0.000	0.000	0 000	0.000	0.000	0.000	0.000	0.000	0.000	0 000		1.95
0.000	0.000	0.000	0.000	0.000	0.000	0 000	0.000	0.000	0.000	0.000	0 000		2.00
6.000	0.004	0 000	0.000	0.040	0 000	0 000	0 0 0 0	0.000	0 000	0 000	0 000		2.85 2.10
6.800	0.004	0 000	0 000	0 000	0.000	0 040	0 600	0 000	0.000	0 000	0 000		2.10
0.000	0.004	0.000	0.808	0 000	0.000	0 000	W. UUU	0 900	0.000	0 000	6 600		2 20
4.400	0.000	4 440	0.000	0 000	0 000	0 000	0 000	0 000	0.000	0 000	0 000		2.25
0.000	0.004	0 000	0.000	0 000	0 000	0 000	0 000	0 000	0 000	0 000	0 000		2.30
9 900	0 004	0 000	0.000	u 000	0.000	0 000	0 000	0 000	0 000	4 400	0 000		2.35
0.000	0.004	0.000	0.000	0.000	0.000	0 000	0.600	0 000	0 000	0 000	0 000		2 40
0.000	0.004	0 0 0 0	0.000	0 000	6 000	0 000	0 000	0 000	0 900	0 000	0 000		2 45

Set 9, Table D — Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 54-56

1						Location	ıs i						
18	ı	2	3	4	5	6	7	8	9	10	11	12	13 +
491   1.597 2.446 2 432   1.588	0.000	0.004	0.000	0.006	0.000	0.000	0.000	0.000	0 000	0.000	0 000	0 000 0	000 0 90
800   2   228   3   446   3   438   2   171   720   1   588   2   346   1   633   1   712   2   081   1   894   1   346   15   1   1093   2   22   117   3   379   3   343   2   046   7   31   1   602   2   218   1   727   1   610   2   2   12   1861   1   300   25   3282   1   231   1   356   1   888   1   133   34	. 221	1.017	1.444	1.454	1 038			1.364	809	1 (16			482 45
1.813   2.921   4.684   4.661   2.876   568   2.207   3 071   2.426   2.238   2.818   2.573   1.812   20	. 491	1.597	2.446		1.588	452	. 976	1.818	1.310	1 389	1 373	1.279	. 913 10
1932   2   117   3   379   3   342   2   046   713   1   602   2   218   727   6   10   2   0   12   1   86   1   300   25   302   1   213   1   916   1   808   1   133   403   207   167   274   319   100   167   232   273   168   35   368   1   134   162   802   022   690   125   009   020   022   043   030   046   40   404   075   099   043   011   025   022   033   030   046   40   404   075   099   043   011   025   022   033   030   046   40   404   035   015   023   028   048   029   020   036   014   022   032   032   048   029   020   036   014   022   032   032   048   029   020   036   014   022   031   010   55   042   049   042   034   048   037   049   042   034   048   037   039   048   029   020   036   014   022   031   010   55   042   049   042   034   048   037   049   042   034   048   037   049   042   031   010   055   042   031   048   048   032   042   042   042   043   044   045   022   022   023   013   017   028   015   027   027   028   028   038   038   018   011   010   028   028   038	09	2.220	3.466	3 436	2 171	. 720 1	586	2.346	1 635	1.732	2 081	1 894 1	1.346 15
1	1.093	2.921	4.684	4.661	2.876	. 968 2	2.207	3 071	2.426	2.259	2 818	2.573 1	.812 .20
048					2.046	. 713 1			1.727				
													_
0.00	. 619	. 346	. 493	. 403	. 207	. 167	276	. 319	186	.167	232	273	. 168 . 35
0.27	. 048	.134	. 162	. 992	.022	. 090	. 125	.089	. 020	.022	. 043	.090	.046 .40
0.028	. 640	.075	109	. 644	.014	. 057	. 089	.043	011	.025	. 022	. 053	. 027 45
642   0.44	. 027	.041	. 055	. 015	023	028	.048	. 0 2 9	. 020	036	. 014	.029	.012 50
038	. 028	.049	. 042	. 034	028	. 037	. 030	u 2 8	426	031	024	. 631	.010 .55
Reg	. 042	.045	. 044	. 016	. 032	. 0 4 2	021	. 020	432	.032	. 025	030	. 011 60
021	. 036	.043	. 058	. 034	. 0 3 2	. 026	.036	. 013	020	.039	010	.025	.027 65
0.25	. 022	.016	044	. 045	.022	. 422	029	013	917	028	015	027	.022 70
	. 021	. 034	. 030	. 926	.023	. 023	024	647	. 017	002	034	027	. 009 . 75
0.25	. 025	.064	. 024	. 036	012	. Q i 2	017	007	006	023	.039	.018	.011 .80
Region   R	. 022	. 039	040	019	.020	020	024	007	. 011	009	023	.011	.014 85
	. 025	.064	. 0 6 8	. 024	. 0 2 4	024	.003	. 0 0 1	020	.011	041	026	006 90
Color	. 027	.076	053	. 044	.044	. 044	.024	. 025	. #21	004	. 024	.029	016 95
0.45	. 422	.042	. 042	. 022	. 035	.035	.020	. 017	018	038	022	.009	.015 1 00
0.29	. 019	.067	. 066	025	. 0 2 5	. 031	.032	017	.017	.009	037	014	025 1 05
0.27	. 445	.073	. 0 5 1	. 016	.016	. 916	.036	.004	. 407	.029	. 029	.007	446 1 10
	029	.047	. 047	. 010	.013	458	034	# 43	AVA	029	023	011	010 1 15
013	. #27	.065	. 065	. 027	.031	. 025	.037	. 017	. 018	.014	. 040	.023	.029 1.20
	. 408	.075	. 075	. 042	.008	. 042	039	. 010	006	.017	. 035	.028	.033 1.25
836	013	. 059	. 056	. 014	. 023	. 044	.020	921	919	022	.015	027	.037 1 30
0.30	. 442	.074		. 053	. 054	. 030	042	. u 2 9	v 2 5	032	031	016	u24 t 35
		. 081	. 055		047		009	032	0 2 v	027	040	014	017 1.40
.634													
041				. 029	. 011	. 018	.012	. 047	. 030	. 0 2 9	044	.027	053 1 30
0.24													
834													
1													
1													
1													
494 407 407 494 494 494 433 503 466 479 486 470 465 1 95  8.000 8.000 8.000 8.000 8.000 8.000 0.000 8.0000 8.000 8.000 8.000 8.000 8.000 8.000 8.0000 8.0000 8.000 8.000 8.000 8.0000 8.0000 8.0													
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1													
• •00 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0													
0   0   0   0   0   0   0   0   0   0													
0.000   0.00													
4.400 0.000 0.000 0 000 0 000 0 000 0 000 0 000 0 000 0													
4.400 0.000													
4,400 4.004 4.006 0.000													

Set 10. Table D — Standard Deviation of Mean Local Pressuran: Fractions, Scaling Runs 58-60

					Lo	cations I									
1	2	3	4	5	6	7	8	9	10	11	12		13		7
4.400	0.000	0 000	•	0.000	0.000	0.000	0.000	0.000	0 000	0 000		ø	000	o	00
. 025	.418	131	203	.037	049	.041	.077	003	0 6 8	023	017	•	021	٠	05
. 051	836	263	407	074	. 498	083	154	007	137	046	035		042		10
. 068	.867	. 342	475	097	135	.111	2 4 9	043	239	004	046		061		15
. 087	713	. 518	. 510	.161	262	.135	402	. 112	365	. 076	060		079		20
. 249	. 360	245	. 333	.387	. 224	069	488	420	294	209	059		016		25
. 201	. 2 4 2	225	179	304	. 238	066	. 380	306	195	150	034		023		30
. 210	.206	177	. 005	. 236	170	067	207	202	063	062	093		019		35
. 137	. 1 8 3	. 209	. 961	. 177	. 128	.069	125	. 126	.066	051	105		. 045		40
. 464	. 159	. 214	. 089	124	095	071	083	. 061	088	064	097		043		45
9	.134	. 218	. 119	074	. 064	072	062	018	113	0 B 2	091		0 4 1		50
. 076	. 110	. 217	. 141	. 046	.041	076	.070	963	.130	. 097	086		039		55
. 065	.087	. 160	. 092	. 036	. 023	.070	0.39	044	087	071	.069		034		60
. 041	.079	121	.060	.031	030	051	031	034	0 9 9 0 4 1	052 938	057 058		036		65
. 025	066	. 0 8 5	017	026	. 039	015	025	018	033	031	063		039		75
. 015	061	. 057	. 011	029	.041	013	011	. 004	020	. 019	050		043		3.0
. 012	069	. 958	. 029	032	. 035	.011	.012	008	015	015	043		078		85
. 020	.062	. 047	. 024	. 036	. 026	.006	020	013	.007	.007	035		. 107		90
. 604	.051	. 021	. 031	.034	. 004	.008	. 012	. 011	010	. 004	021		047		95
. 016	. 0 2 5	. 029	. 025	.010	. 009	. 0 1 2	.007	. 011	.010	012	.005		011	1	00
. 009	033	. 0 2 1	. 029	.016	008	.014	. 0 7 8	. 011	006	010	007		014	1	05
. 604	. 039	. 018	. 036	. 029	017	016	.009	. 011	004	. 0 0 8	.008		016	1	10
. 010	046	. 0 2 4	. 046	.044	. 028	.019	.010	. 014	.003	.007	011		050	1	15
. 007	.046	. 028	. 051	. 038	022	.018	014	.016	.007	.009	.008		. 016	1	20
. 014	.046	031	. 053	. 026	.014	.017	.018	. 018	.011	011	.003		010	1	25
. 026	.049	. 036	. 058	.015	.013	015	. 024	. 022	.015	. 014	003		097	1	30
. 034	. 052	. 029	. 045	.015	.008	015	027	023	016	. 014	007		.003	1	35
. 030	. 056	. 026	. 034	019	. 005	015	. 026	021	012	015	.006		005	1	40
. 043	. 059	. 024	. 022	.022	002	.015	.026	. 017	.007	.015	.006		.009	1.	. 45
634	. 051	. 020	025	.025	003	.016	. 020	016	004	015	.004		012	1	50
. 021	. 042	. 018	. 428	.028	. 006	.014	. 015	017	007	013	.002		008	1	55
. 010	. 037	. 015	032	.032	. 009	012	010	019	011	015	G () 🐞		004	i	60
. 008	.036	. 017	. 031	.031	.008	011	010	. 018	014	018	009		003	1	65
. 008	.038	. 017	031	.031	.008	.008	.012	017	.014	. 013	008			ı	7.0
. 008	.034	015	.032	.032	.008	.006	. 015	. 016	011	011	008		011	1	75
. 008	.044	. 014	. 033	.033	. 008	.006	. 0 17	. 017	.009	013	012			1	80
. 010	.043	. 013	. 034	.034	.008	.006	. 020	. 017	007	016	.012		011	1	85
. 023	.050	. 013	037	. 037	. 006	012	024	918	0 9 8	020	011		000	1	90
. 037	.056	. 015	. 040	. 0 4 0	. 006	.016	.023	. 021	.008	. 019	.006		.008	1.	. 95
. 048	.061	. 019	. 043	. 0 4 3	. 007	.021	. 021	. 023	.007	. 019	0 C 4		010	2	00
. 044	.061	014	. 047	. 047	. 012	.019	.019	026	0 0 5	010	002		013	2	05
. 038	.055	. 0 0 8	. 050	. 053	. 017	.015	. 018	. 026	.011	017	006		019	2	10
. #37	. 057	. 0 0 8	052	058	. 020	014	0 1 9	027	020	017	010		056	2	15
. 036	. 055	. 012	. 053	.061	. 014	015	019	. 028	027	016	.012		035	2	50
. 036	. 056	004	. 056	. 046	. 021	. 012	.020	026	026	020	012		029		25
. 037	.056	. 005	060	.029	. 033	009	022	024	023	025	015		027	2	36
. 030	.054	. 011	063	014	. 038	.002	. 024	023	018	030	.015		024	2	35
. 040	.050	. 019	.067	.014	. 024	.002	. 027	025	.008	025	015		0 2 0	2	40
. 043	.046	. 025	. 071	017	. 009	.004	031	027	010	019	016		014	2	45

Set 11, Table D - Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 61-63

					Location								
1	2	3	4	5	6	7	8	9	10	11	12	13	7
4.400		0.000			0.000 0		.000 0		0.000	0.000			. 00
3.335	5.453	5.714	5.721	5.500	5.037 1	.08214	. 32211	. 193	3.765	5.175	2.073	2.478	. 05
4.220	4.082	4.333	4.337	1.155	3 599	.87910	. 853 8	. 452	2.839	3.877	1.550	1.951	10
2.906	2.752	3 000			2.507	686 7	. 400 5	. 733	2.053	2.634	1.107	1.432	15
1 600	1 577	1.020	1.750		2.319	.515 4	. 0 35 3	. 101	1.625	1.577	.876	. 931	20
. 392	1.128	1.247	1 055	604	3.083	.385 1	. 472 1	. 246	1.741	1.238	.974	. 492	25
. 152	. 8 8 8	. 8 2 1	. 692	.445	2.793	. 295 1	. 099	. 998	1.319	. 986	.773	. 316	30
. 965	633	. 314	. 464	. 271	2.339	. 205	. 811	. 745	. 994	.762	. 593	. 243	35
929	379	. 350	236	098	1.086	. 1 1 5	525	. 493	.669	. 539	.413	. 171	. 40
. 114	. 1 2 5	118	912		1.432	.025	. 241	. 242	. 345	. 316	. 233	102	. 45
. 169	.061	. 045	140	. 195	1.083	. 0 4 2	. 056	. 469	. 121	. 153	.101	. 056	50
. 137	.076	. 045	. 112	161	1.006	.026	. 051	. 070	. 115	. 132	. 091	.049	55
. 106	.090	.063	. 085	. 122	. 933	.015	. 048	. 467	. 104	. 104	. 085	053	60
.077	. 1 6 5	082	. 459	.083	858	.033	. 046	066	.093	.078	.076	. 058	65
. 064	.073	. 0 6 4	. 067	.087	. 840	.037	. 0 4 9	.069	.092	. 084	.083	.063	. 70
. 050	.047	. 0 4 7	. 465	. 0 3 6	. #21	.040	. 051	.071	.084	. 089	.081	.064	. 75
. 046	.034	. 033	. 076	.087	. 803	.048	. 0 6 0	. 076	.087	. 089	.080	.071	
. 052	. 035	. 027	046	.063	. 786	.054	071	. 080	. 100	. 086	0 6 1	.082	6.5
. 050	. 0 <b>3 6</b>	. 029	036	058	.776	.057	. 0 6 9	.079	. 099	. 084	.080	.088	90
. 045	.038	. 038	.038	.070	.773	.061	057	.074	. 084	. 083	.076	096	95
. 468	.068	060	060	. 039	. 781	.065	. 058	. 059	.07.	081	068	074 1	00
.083	. 055	049	. 062	. 049	778	.057	. 054	. 065	.075	.077	.072	073 1	05
. 493	054	053	. 074	049	. 791	.053	. 054	.075	.001	. 069	.071	.065 1	10
. 086	.066	059	. 060	. 0 4 6	802	. 0 5 9	. 0 6 8	. 075	.082	. 066	.064		. 15
. 977	067	. 0 6 4	. 054	. 035	. 014	.069	.078	. 073	.082	. 069	.061	071 L	30
. 071	074	070	. 069	. 070	826	.075	. 077	. 069	.074	. 073	061	. 970 L	23
086	.069	069	064	069	. 930	.074	.074	.070	.068	. 074	.037	.068 T	10
0.8.3	.077	070	064	.070	. 63 t	.069	. 066	. 970	.075	. 066	.054	965 L	35
. 077	. 0 9 9	. 974	. 074	.074	. 633	.062	. 057	. 672	.083	. 053	. 0 5 6	061 1	40
. 071	. 0 8 4	. 0 6 8	. 057	. 057	. 036	.072	.067	.082	.083	. 063	.067	072 1	45
. 066	.069	069	. 038	038	. 836	.080	. 079	. 494	.087	. 083	.081	064 1	30
.065	.063	065	.035	.035	. 845 . 859	074	.082	.087	.111	.092	.087	050 1	55 60
. 064	070	. 070	. 034	014	865	073	070	093	108	102	091	054	65
035	.073	. 073	048	012	866	084	076	101	100	. 100	091	098 1	70
.027	.061	. 058	. 462	017	166	. 083	. 0 6 2	. 095	. 100	. 103	.090	056 1	75
041	.060	0.38	.063	026	. 866	,077	089	. 484	. 104	. 112	. 099	.068 L	. 60
. 064	.064	. 026	.046	.026	. 652	.073	. 089	.087	. 106	. 113	.091	093 L	65
. 465	.066	. 025	. 032	.025	852	.078	. 0 2 4	. 091	. 105	. 104	.092	107 1	90
. 476	. 0 6 6	041	. 424	. 0 2 4	. 662	. 0 8 2	. 073	. 091	103	. 097	. 0 9 2	. 109 1	95
. 079	. 967	966	. 422	.025	. 872	.063	. 075	. 489	. 091	. 097	. 093		. 0 0
063	063	061	. 025	046	. 477	064	. 976	. 491	. 0 9 0	. 103	.091		. 45
. 436	.036	052	. 940	052	. 971	.087	. 075	. 103	. 1 0 6	. 106	108		. 10
. 021	. 0 2 1	016	. 972	036	161	002	. 078	107	. 1 1 3	103	107		. 15
. 439	.035	. 026	. 087	.026	. 471	.071	. 974	. 100	. 113	. 497	. 093	112 2	20
. 664	.056	918	. 072	.018	. 863	. 975	080	. 100	.114	. 102	.091	115 2	25
. 965	.049	031	. 038	.019	957	.081	. 0 8 8	. 101	. 112	. 111	. 0 9 5	120 2	30
. 957	.045	049	. 022	022	. 852	.082	. 0 8 6	106	. 115	113	. 1 0 3	. 123 2	32
045	019	0 6 9	024	. 924	857	083	. 0 5 5	. 110	.116	. 111	.116		. 40
043	011	069	.024	047	. 866	086	. 0 85	. 109	. 115	. 115	.117	. 127 2	. 45

Set 12, Table D — Standard Deviation of Mean Local Pressurant Fractions, Scaling Runs 64-66

		Locations	ı			
1 2	3 4	5 6	7 8	9 10	11 12	13 ,
0.000 0.000 0	000 0 000 0	000 0 000 0	000 0 000 0		0 000 0 000	0 000 0 00
.486 175 1	447 179	185 1 118	545 911	108 521	120 122	411 05
961 379 2	904 3/4	379 2 224 1	054 1 810	251 1 030	250 255	.786 10
#20 304 2	510 289	359 1 945	927 1 574	. 237 874	. 223 . 231	679 13
347 182 1	724 166	232 1 356	654 1.079	181 .577	163 173	466 20
286 063	973 111	107 .780	380 599	130 .305	103 117	259 25
088 033	372 064	033 257	098 204	079 110	037 037	079 30
965 032	128 032	054 108	018 048	049 .034	.031 002	041 35
042 033	U95 050	048 066	025 063	038 036	931 009	026 40
028 051	640 928	033 038	028 .049	028 .030	.020 009	021 45
011 035	V46 U33	033 .011	012 040	019 035	011 016	.015 50
011 019	015 034	.022 .011	009 026	150. 600	.010 007	008 55
.037 .012	017 011	017 037	024 020	013 004	008 005	002 60
043 023		013 .043	024 020	.010 .013	007 013	009 65
.030 .020	010 029	010 .030	021 .027	012 011	010 017	013 70
026 .004	-		.023 .018	019 .011	.017 .009	010 75
028 004			.027 .028	017 015	008 005	009 60
.025 .009			.022 .027	018 021	013 005	009 85
.423 .013			.023 029	.028 .015	.011 .008	.015 90
023 021	309 009	009 032	006 .028	018 010	015 .009	012 95
069 032	.031 031		.037 .023	006 019	007 019	014 1 00
031 .013			004 021	010 009	003 004	012 1 05
435 016	018 015		.024 .026	029 027	010 .005	014 1 10
	.016 .016			.033 .011	020 010	
	. 632 632	032 .033	019 .018	.001 .015	010 027	.033 1 20
.067 .038	014 040	040 .036	041 .008	.017 .009	012 018	025 1 25
	027 032	.018 028	046 .036	.036 032	015 005	009 1 30
			034 .028	030 023	012 008	006 1 35
.041 .031			.021 .021	.005 .011	.020 .030	029 1.40
.067 .035			.029 .013	011 016	.035 .028	012 1 45
.095 .035			.038 .026	.026 .028	.034 .034	.032 1.50
041 035	012 044	012 079	037 .017	030 .029	025 035	.016 1.55
.951 050	050 040	.050 .083	.023 .025	.011 .017	.024 .047	022 1 60
050 047			022 028	.010 .034	.027 .049	.017 1 65
.057 039	.039 .043		.028 .019	.020 .022	.036 .041	.027 1 70
.308 .464			.470 501	472 478	.472 .486	.484 1 75
337 .489	489 439	489 .487	441 498	451 452	441 461	461 1 80
0 000 0 000 0		000 0 000 0			0 000 0 000	0 0 0 0 1 85
0.000 0 000 0		000 0 000 0	000 0 000 0		0 000 0 000	0 000 1 90
4.000 0.004 0		000 0 000 0	000 0.000 (		0 000 0 000	9.000 1 95
4.900 0.000 0	000 0 000 0	000 0 000 0	.000 0.000 (	0.000	0.000 0.004	0 000 2.00
4.400 0.004 0	.000 0 000 0	.000 0.000 0	.000 0.000 0	000 0 000	0 000 0 000	0 000 2 45
0.000 0.000 0	.000 0.000 0	000 0.000 0	.000 0.000 0	.000 0 000	0 000 0 000	0 000 2 10
4.406 0.006 0	000 0 000 0	000 0 000 0	000 0.000 0	000 0 000	0 000 0 000	0 000 2 15
0.000 0.000 0	000 0.000 0	000 0 000 0	000 0.040 0	.000 0.000	0.000 0 000	0 000 2 20
0.000 0.000 0	000 0 000 0	010 0 000 0	000 0.000 0	100 0 000	0 000 0 000	0 000 2 25
	000 0.000 0	000 0 000 0	000 0 000 0		0 000 0 000	0 000 2 30
4.400 4 004 0	000 0 000 0	000 0.000 0	000 0.000	. 400 0 . 000		0 000 2 35
0.000 0 000 0	000 0 000 c	000 0 000 0	000 0.000 0	000 0 000	000 0 000	0 000 2 40
	000 0 000 (	000 0 000 0	000 0 000 0	. 000 0 000	• ••• • •••	0.000 2.45

Set 1, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 23-31

											Locatio	ons	I														
	ì		2		3		4		5		6		7		8		9		10		11		12		13		7
4	000	0 1	0.0	0	000	Ü	000	0	000	4	000	0	000	0	000	Ģ	000	O	000	Q	0.00	o	600	g	000	Û	g G
- !	933	. :	3.3	2	452		170	٠	415		796	-	722	•	120		190	•	. 45 i	-	524	•	319	-	810		05
- 2	9a n	2 3	: 12	Ł	11:	:	691		654		879	•	803-	1	944		487-	1	722-	1	637	-	512	-	899		10
- 3	794	2 8	931	9	197	2	712		485		941	-	89u-	3	466-	1	101-	2	.786-	2	536	-	666	-	966		15
~ 3	235	2	131	a	905	2	. : 3		460		5 4 3	-	732-	3	134-	1	634-	2	.522-	2	207	-	519	-	767		20
- 2	442	1.	769	6	758		988		117		251	-	574-	2	043	-	611-	1	634-	1	362	~	304	-	512		25
- 1	445	:	546	3	965	•	107	-	228	~	038	-	386	-	746	•-	147	••	629	-	452	-	085	-	245		30
- 1	000	;	350	2	555	-	282	•-	281	-	100	-	260	-	349	-	0.26	**	295	•	191	~	016	-	109		35
-	761	:	307	1.	813	-	274		238	~	104		197	-	235		9 6 1		191	-	145		605	-	069		40
-	660		544	1	436		275	•	222	-	118		250		160		009	-	130	-	105		006	-	053		45
-	529		3 : 3	:	3.0		294	-	245		130		139	-	117		004		093	-	063	•.	003	-	035		50
	487		321	1	204	••	270	-	249		140		128	-	104	-	809		069	-	048	•.	061	-	019		55
-	445		323	1	152	-	277	-	263	-	154	-	127		099	•-	002	•	060	-	041		C 1 2	-	018		60
-	379		326	i	192	-	290		287	-					034				075	-	029		608	-	031		65
-	321		336	•	147		299		286	-	179	-	148	-	076		628		077	-	023		005	-	040		7.0
-	294	:	356	ì	ili	-	269	-	269		208		153	-	089	~	046	-	061	-	036		016	_	027		75
-	249		352	1	0 8 8	-	246	_	246	-	226		161	-	077	_		-	061		040	_	026	-	044		80
•	230		375	1	068	-	228	-	246	-	232		156	-	104	-	055	-	056	-	058		034	-	039		85
_	224		413	1	0 6 1		208		258	_	522		177	-	094	_	978	_	.080	_	050		039	_	047		10
	238		4 11 2	1	0.75		165			-	244		165	-		_		-	103	-	053	-	037	-	048		95
-	236		342	1	936	**	151	-	235	-	235	٠.	168	-	083	-	077	-	.060	-	043	-	056	-	034	1	00
_	100		197		576		099	-	. 132	_	136	-	117	_	064		034	-	.007	-	045	_	020	-	010	ı	05
-	071	:	154		4 1 1	-	083	-	.092		112	-	096	-	041		026		.004	-	021		008	-	019	1	10
-	079		160		347	-	053	-	071		114	٠.	101	<b>-</b> .			916		. 0 4 6	•	049		001	-	008	١.	15
	13 🚊 🥫		123		3 2 5	-	069		. 058	-			104	-	037		007		.048	-	029	-	006	-	022	ı	20
	05.		0 9 4		213	-	063	•	042	-	099	-		-	036		014		100	:	037		011	-	028	ı	25 30
-	047		067		190	-	051		020	-	005	-	086	Ξ.	036	•	036		.114	Ξ,			023		025	i	35
-	941		063		142	_	018		400	_	082	-	083		065		044		108		068		023	_ `	025	ì	40
			5,74		107	••	025	-	011	-	064	-	084	-	064		063			-	063		021	-	020	ı	45
	028		. 44		177		e2.8		.003		063		085	-	050		059		.120	-	059		025	_	028	ı	50
-	004	- (	016		112	-	041	-	021	_	062	-	090		015		063		. 138	-	046		021	-	026	Ł	5 5
-	037	- (	024		990	-	a 5 9		. 0 J 8		069	-	081	-	038		465		. 151	• .	058		033	-	008	1	60
-	461	٠, ٠					0.58		. 056		079	•	064	-	051		073		161	• .			041	-		ı	65
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-	007				0.15	-	907		.015		007		012		042		014		.012				005	-	012	1	80
	0!3	- 1			014		.013		.014	-	013	-	016		046		012		.019	-		-	005	-	013	1	85
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7			000	е.	000		.000		.000	0	000	٥	000		000	0	000		.000	0	000	0	000	0	000	1	95
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Set 2, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 32-34

			1	ocations 1					
1	2	3 4	5 6	7	8	9 10	11	12 13 :	7
4.000	0.000	0 000 0 000	0.000 0.000	0.000	0.000 0	004 9.000	9 900 6	000 0 000 0	90
- 323	330			- 100	1.016	.112016	. 121	014 045	05
			- 973 - 323		2.114	.348 .090	300		10
- 502			- 595 - 013			139 - 537			15
- 122						. 531 ~ . 980			20
- 239		3 424 - 061	034 350			662-1 . 087			25
- 253		3 273 162	.129 323			649-1.032			30
- 268		1 122 184				- 635 - 976			35
- 3+8		2 570 256				406 - 687			40
- 421						. 168 403			45
- 366 - 334		1.623 - 047 1.296 - 120	- 121 - 036			· 495 - 277 · .044169			50
- 301						. 016 - 169 - 016 - 089			55
- 276			- 184 - 08			016089 006059			60 65
- 255	234	939 - 151				.010060			70
- 238	244					.024 - 075			75
- 205	266		- 138 - 10						80
- 164	.279		- 132 - 10						85
- 132	275		- 116 - 09						90
113	304		11048						95
693	247	.786 - 107						- 081 - 090 1	00
- 064	.199	588096	07907	3117	081 -	061 051	- 047	054066 1	05
047	. 1 6 0	.436089	051050	095	066 -	049027	028 -	- 034 - 050 1	10
055	. 140	.386 GBO	02905	080	062 -	038 016	025	031051 1.	15
049	.136	351081	022049	066	060 -	03E 010	929	033053 1	20
041	132	328 - 473				043006		037056 1.:	
- 035	. 116	331 - 053	.01104	5 072	060 -	037005	043	040062 1	30
- 039	.039	.339038				034003			35
034	.092			080				041072 L.	
- 027	. 1 1 2		017044		057 -			036079 1.	
025	105	280 - 053		069		- 019 .038		031079 1.	
040	.084	.236045				0.00 E10		029079 1 ! 021073 1.6	
	066	.221 - 033		082	031		033 -		
- 040	062	.186035		7 - 079	049	.014 .084		019069 1.4 025071 1.5	
- 021	045	167 - 037	022 - 03		- 033	.025 .096		- 022 - 073 1	
018	. 0 4 9	.168047	.02004	7077	049	.035 .095	042 -	017073 1.	
038	.048	171 - 047	.00503		033	.036 .105		009068 1	
044	.042	165 - 057	003037 010039	7 - 066	010	.035 .117		001062 1.5 .005062 1	-
- 049	.03 <b>6</b> 02 <b>3</b>	149 - 059 127 - 032	.00706		-,040 -,034	.042 .125		010 - 062 1	
- 045	027	. 121 021			- 018	050 124		.010049 2	
041	032	.115 - 024			031	.059 .121		.010 - 071 2.	
- 042	036	. 103 011	029 06	070	055	.060 .132		.008074 2 .	15
035	.036	.094004	036 - 07	7068	052	.052 .145	064	.006075 2.	20
- 019	017	096 - 023	017 - 07	2 - 060	042		057	.006073 2	25
- 003	001	.097041	00105	- 053	043		- 056	001 - 072 2	30
019	002	.091 - 038	00206	047	042	.083 .135	055 -	002072 2.	35
039	017	.081 - 040	01705	044	040	. 481 . 161	- 060	005076 2.	40
043	032	.065056	023 - 04	- 039	042	.003 .162	065	00 <b>1 -</b> .073 2.	45

J CASES

MEAN VALUES OF ALL QUANTITIES

Set 3, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 35-37

			Lauriana			
1	2	3 4	Locations 1 5 6 7	8 9	10 11	12 13 г
		000 0 000	0 000 0 000 0 000			0 0 000 0 000 0 00
- 764	- 934-1	189-1 449-	1 242 - 726-1.066	2 799 . 595 1	091 1 19	3 1 649 - 364 05
- 169	- 5J <b>6</b> -	354 - 979	~ 514 - 071-1.132	1.834 336	359 67	6 1.205 - 654 10
424	- (4)	480 - 510	213 583-1 199	866 - 323 -		
1 019	.257 1			- 101 - 982-1		
1 612	654 2		1 669 1 093-1 332			
2 108	866 2		2 255 2.407-1.375			
2 604				2 524-2.373-2		
2 654	1 211 3	\$95 1 151	3 181 3 187-1 376-	7 030-2 500-3	148-1 86	1 - 956-2 142 40
2 367				2 552-2 113-2		
1 909				2.030-1 617-2		
1.429	. 322 1			1 507-1.123-1		
1.001				1 023 - 715 -		
	076	864 - 298	854 900 - 424		642 - 10	
	074	778 - 321		- 595 ~ 414 ~		
. 612		.693 - 344	.690 719 - 430			
555		633 - 371	610 632 - 424			
527		694 - 406	560 .598 - 437		-	
. 500	. 0 9 3	584 - 441		- 411 - 314 -		
. 496		580 - 453		- 390 - 316 -		
. 520		365 - 414	533 533 - 363			
	- 092	230 - 386		- 279 - 246 -		
	- 12 <b>2</b>	181 - 381		- 277 - 241 -		
596		112 - 375		- 275 - 238 -		
	158	149 - 366		- 273 - 238 -		
621		096 - 358		- 272 - 240 -		
	- 157	084 - 352				4 ~ .064 ~ 261 1 30
	153	.076 ~ 351		- 273 - 236 -		
	- 148	071 - 349	647 635 - 295			3 - 080 - 261 1 40
639		.066348		277 - 229 -		
.647		.039 ~ .353		271 228 -		
	156	048 ~ 367				2 - 104 - 274 1 55
. 659		044 - 376	690 .650 - 297			9 - 111 - 279 1 60
653		042 - 366	684 663 - 294			1 - 110 - 279 1 65
. 649		v19 - J53			191 - 13	
. 655		029 - 147		- 270 - 197 -		1 - 112 - 278 1 75
662		015 - 345			.17114	
.670		· 001 - 343 · 017 - 323	.687 655 - 273 .689 .656 - 273	- 258 - 196 - - 237 - 199 -	.159 - 15	
		032 - 316		260199 -		
663		049 - 314	694 663 - 272		.13616	
. 676		056326 062326			129 - 15	
704		- 069 - 321 - 075 - 304		277192 -	113 - 16	
		078 - 299			.95 - 18	
		083 - 302			.08419	
		093 - 312			.075 - 19	
		- 099113	.646 .657 - 283		.07519	
. 702	- 511	- 105 - 306	.686 .657282	- 290 - 162 -	.97819	7128265 2 45

Set 4, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 39-41

				1.	ocations	: 1												
1	2	3	4		6	7	8	9		10		11		12		13		
0 000	_	.000 0		00 0 0	•		0.000	2 00	0 0	000		000		000		000		00
-1.188	- 912-1	249-1	314-1 3	28-1 1	48 -	808	. 767	13	1	150	4	141	3	087	-	347		45
-: 252	- 686-1	326-1		20-1 1	59 -	551	. 851	31	4	449	3	603	2	862	- ,	115		10
-1 137	- 392 -	939-1	288-1.3	67 9	174	309	711	. 36	7	505	2	649	2	211		917		15
824	- 008	101 -	.514 - 7	48 4	127 -	135	. 143	21	4	067	1	280		957	-	097		20
625	.221 1	034	.075 - 2	79 (	0) -	091	- 316	05	9 -	378		465		107	-	261		25
- 327	.316 1				173 -	148	649	- 08				131		369		443		30
476	298 1				152 -	161	- 690	- 10		8 6 9		062		456		4 5 5		35
- 394 - 308	072	732	205 - 0		92 -	473	- 425	- 03				102		236		260		40
- 273	042	527	014 - 0				- 115	03		181		139		045		069		50
273	067	517 -					107	. 02		164		163		077		074		55
270	.105	513 -				088	- 107	. 0 1		148		187		114		063		60
253	. 135	495			77 -		• • •	- 00		137		199				082		65
- 238	145	465 -	119 - 1				- 111	- 02		130		221		191				70
217 175	111	.470 -	150 - 1		) 91   10 -		- 123 - 131	- 05 - 07		125		266 280				061		25 80
- 169	148	468 -	1291			134	- 127	- 09		142		277		232		066		85
- 193	145	490 -	1121				- 127	- 11	-	148		294						90
- 153	153	474 -			31 -	162	- 142	. 11		138		312		240		071		55
123	096	467 -					114	- 10		094		224		216		054	1	00
- 092	-	279 -		53 - 0			- 069	- 05		034		168		155		040	1	0.5
071	059	207 -			91 -	082	- 069	- 04		022		148		123		035	í	10
- 087		.180 -					- 063	- 01		018		130		111			i	15
- 103	019	149 -		28 - 0			- 055	0.0	4	028		115		093		020	1	20
055	.020	.145 -	.048 - 0	28 (	65 -	072	0 5 8	- 00	2	040		085		069	- ,	0 3 4	1	25
073	.020	153 -	0260	15	36 -	075	064	. 00	3	.039		061		052	<b>-</b> .	037	1	30
- 069		. 125 -		19 - 1	42 -	048	- 064	02		054		047		041			1	35
056	037	091 -			36 -		- 053	03		067		025					1	40
070		. 054		05 - (			050	0 4		075		010		021		023	1	45
458	028	.056 -			23 -		- 046	04		085		001		012			1	50
- 015		048 -		15 - (			- 042	04								017	1	55
036	018 048	079 -					- 043	. 05		110	-	022		003	-	015	1	60
- 009 027		.067			)75 - 364 -		- 052 - 048	03 05		.100	-	044		022	-	031	1	65 70
- 012				32 - (			- 015	06	-	142	-	072		053	-	046	ì	75
- 042		. 045		37 - (			- 038	. 07		.153	_			061		037	1	80
- 074		085			301 -		- 042	0.8		143		087		058		049	i	85
- 032	.016	044		44 - 0			- 050	. 06		136						058	i	90
037	019	019		21 - (			629	97		164	_	099		069	~	045	i	9.5
035	- 011 -	011	_	47 0		007	- 025	. 08		161		099		067	-		2	0.0
006	- 006 -	006 -	006 - 0	06 - 0	06	018	003	0.5	0	067	-	040	_	031	-	028	2	0.5
011	011 -	.011 -	011 - 0	11	11	021	. 011	. 06	1	072	-	ú35	-	034	-	023	2	10
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Set 5, Table E - Deviations of Mean Local Pressurant Fractions, Scaling Runs 42-44

					Locat	ions	i													
1	2	3	4	5	6		7	8		9		10		11		12		13		7
0 000	0 000	9 999	9 901	0 000 0	000	0 0	000	0 000	0	990	0	000	0	000	0	000	0	000	0	• 0
- 503	2.6.5	602-	2 339-	2 235-1	893	2	260	2 166		617	1 .	500	1	096		297	-	323		05
- 960	1 2/4	9 # 1 .	4 638-	4 638-3	723	:	549	4 311	2	223	3	070	2	248		636	•	6 4 5		15
- 794	1 20'	850	- ۾ پيار ه	9-72-6-3	0 - 4		1	4 036	1	1.97	2	7 9 4	ı	362		614	-	143		15
- 648	1 10'	6 4	rate in a fire	2 249 1	456	2	11.3	. 491		▶ ? ?	i	234		852			•	4 6 0		20
- 360	3 4 4	937	u. 2	508 ~	071	- 4	<b>د</b> د د	- 029		131	-	043	-	054	-	066	-	049		2.5
- 420	169	912	- 013	- 124 -	034	- 1	1 5 3	- 260		015	-	175	-	094		034		689		30
- 268	093	644	- 162	- 126 -	60.	~ 1	0.4	- 143		0.2.3	••	066	-	652		035		0 7 2		35
- 205	1.37	5. 44,			1 . 4	. (	14	- 103		0.23	••	042	•	c 2.4		035		0 4 1		4 :-
179	1.4.1	149		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	107	e 1	ં ડ	) ย		(49	•	e 13	-	77.2		CJZ		じなち		4 %
- 165	173				. U & 1			~ 085		0.5%		962				013		040		50
162	151					. (		- 078			-				-			018		55
- 179	1 7 2	5 ? 3		.087 -				~ 0?b		. 6 ! 3				405		_		0 ( 4		60
- 136	221	559		- 117 -			-	- 069				076	-		•			0.62		65
- 098	219				. 098			058					•		-		•	002		70
~ .077	.227			- 121				-					-		-		-	021		75
- 069	. 225			- 112 -				- 073				067	-	048	-		-	035		80
077	.280			- 121 -								• • •	-				-	054		85
071	.263							v 7 d				0.17		1164	•		-	1140		7 /
- 068	.293			117 -				- 105	-			. 957 . 976	-	084	-		- -	053		95
. 005				- 080 -									-				-	037	1	05
- 016	150	263		- Ung -				- 056		061	-	025		032	_			003	;	10
- 006	074	134		613 -		(		- 030		43a		¢27		016		-		605	:	15
. 011	074	066	_	- 037 -				- 036	-			041		011						20
037	.117			- 032 -		0		- 033	_	008		077		006		037		011		25
. 006	.053	020					559	- 052		013		073		018		042		004	i	30
. 006	006	0 4 4		. 039 -				- 051		016		134		023		038	•	012		35
- 032	617						فادد	- 039		038		1 3 3		014		036		047	:	4.0
039	.011	- 035				- 6		045		925		. 133	-	002		062		042	i.	45
4.400	0.004	0.000	0.000	0.000 0	.000	0.0	000	0.000	٥		0	000	0	004	0	000	٥	000	1	50
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Set 6, Table E - Deviations of Mean Local Pressurant Fractions, Scaling Runs 45-47

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	ł		2		3		4		5		6		7		8		9	10		11		12		13		•
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-	251	1	270	-	170	1	254	ı	027	1	343	-	160-	1	197	-	632-1	995	~	895	-	178	-	448		05
- 1	. 093	3	601	5	120		739	-	245		276	-	901-	1	832 -	. 1	278-1	987	- 1	202		851	-	5 2 1		10
- 1	296	4	065	6	742		203-	- 1	013		203-	٠1	124-	1	695-	1	353-1	972.	- 1	4 7 4		917	-	425		15
-	. 273		256		791	-	021	-	076		005	-	081	-	1 1 1	*	062	164	-	104	-	072	•	076		20
-	. 233		204		624	-	692		0.95	-	032	•	0 4, 4	-	477	-	001 -	127	-	0 & 1	-	041	-	036		25
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Set 7, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 48-50

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Set 8, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 51-53

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Set 9, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 54-56

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- 635		064	-	062		026	_	031	-	031	-	057		028		045	032		976	080	062		
054	-	061	-	941	-	938	-	038	-	938	-	072		039		043	057		079	065	. 057		90
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006	-	062	-	076	-	031	-	019	-	053	-	019		064		014	050		052	054		ı	65
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J CASES

Set 10, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 58-60

						Locat	ions	ı														
1	2	3		4	5	6		7		8		9		10		11		12		i3		٢
4.000	0 000				0.000			.000				000				000				000		00
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- 096	. 539		_	1 968	027	149	_	011		40		292				447				105		20
. 206	. 643			1.260	. 506		_	040	-	34		744-				764	_			203		25
. 170	569			1.318	459	620			-1.3			719-				758	_			213		30
. 140	544			( 254	454	572		074		45				084			-			210		35
. 111	.473			1.109	.399			091				528				656	_			194		40
. 083	. 391			931	342			109		-		410					_	381				45
. 056	310			754	265	354		126	_	_		292					_					50
. 034	. 231			584	.231	281		141										274				55
. 445	.169		15	475	203	235						136						227				66
. 030	.121			. 387	169	206						105						179				65
. 424	.091		90	316	130			119														70
.006	064	-	16	246	097	156		101										094				75
. 000	.037			. 195	.083	143		079										078				80
. 611	.024			. 154	.075			053				030					-			050		65
.021	.007			. 122	.063			.034		-		_				063						90
010	001			095	054			032											-			95
. 007	- 035			. 063	021			038										019			1	
. 013	- 029			.056	.027			033									_				i	
	- 023			. 049	033			027													i	
028	- 017			042	.039			021										017			i	
	017			037	.047			023		-								017			i	-
	014			.031	052	. 068						021		_							1	
	012		-	.026	.058			.032													1	
	009			.033	. 054	070														019	i	
	013			. 040	.051			.030												017	1	
	017			. 447	047			.028										017			ì	
	011			. 043	043			027										017			i.	
	007			. 036	036	. 052														011	i	
	004			029	.029			024										007		006	i.	-
	008			. 025	025			022								003				001	1	-
	010			. 423	023	939						021					•	002		005		70
	013			. 020	.020	.037						021				001		003			i.	
. 035	015			.017	.017	. 035			0			919				005		002		020		80
	016			. 617	017	031		035				017						001		025	-	85
. 037	017			. 014	016	025								006		001	_	001		024	-	90
441	019	- 0	14	. 015	.015	. 019			0			913	_	005		002		001		020	1	95
. 449	- 026			. 014	014	012								004	<u>.</u>	004	_	001		015	-	60
. 457				414	.018	. 006	-	021	۵	06		006	_	006	-	006	_	003		049	2	43
. 053	011			. 013	.024	.001		.021						005		006	_	007		004	2	
. 053	006	0	12	. 013	029	001	-	022	•	0.3	_ `	005	_	004	_	007	_	011	_	001	2 .	
. 645	0 0 7			. 012	. 027	. 007		. 623						002		006	-			0 9 1	5	
. 039	615			. 411	. 032	. 017					-					001		011		0 9 3	2 .	
. 033	421				. 038	. 027		.029						000		004	-			043	\$ .	
. 027	027				.044	.027		.031				909		009		900	-			100	2.	
. 024	023			003	.033	. 031		021				006		800				003		047	2.	
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3 CARES

Set 11, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 61-63

			Locations 1			
ı	2 3	4 5	6 7	8 9	10 11	12 13 r
	D.000 0 000			.040 0.400 0		
	3.813 3.621			3.525-7 588-2		
	3.269 3.397			7.707-6.160-2		
	2 725 2 995			.063-4 733-2		
	2 190 2 691		3.192 075-4			
	l 594 2 316 1 223 1 996			2.188-1.033-2 1.454-1.217-1		
. 208	987 1 619		1.834 - 003-1			.096449 .30 .927410 .35
132	751 1 240			.844 - 700-1		
. 036	513 860					573 - 333 45
. 001	326 . 519			. 296 239 -		
001	258 429			247 - 202 -		
. 003	.192 334	288 .028	.807014	.204174 -	.394342 -	.202219 .60
.005	124 241	207 .013	.732014	162146 -	.321 - 268 -	.236174 .65
001	.110 .165	138 - 015	.695010 -	. 133 133 -	.269228 -	201 - 145 .70
- 004	.108 .136	.489037	.662006 -	.106121 -	.222 ~.192 ~	.177 ~ .123 .75
014	.093 .091	463043	.639010	-,090 -,112 -	.183163 -	.155110 80
425	.067 .057	. 659033	.615021	009106 -	.151142 -	.133149 05
016	.042 .031			075094 -	.130120 -	.110098 .90
. 0 0 5	.011 .011		.58103?			.091 - 078 - 55
005				038 061 -		
	023029			044078 -		.064062 1 05
	021026			042089 -		
	003018			041088 -		.072072 1 15
	00 <b>0</b> 008	021 020 1 019 - 008		- 046093 - 046096 -		.074 - 078 1.20 .074 - 078 1.25
	014014			046090 -		
		- 434 - 023		044 089 -		
		- 033 - 033		- 042 - 099 -		.089081 1 40
016		433033		046000 -		.085080 1 45
010	-	- 030 - 030		050093 -		.084080 1 50
.002		035 035		046091 -		
		- 948048		- 046 - 082 -		
. 032	020020	061044	574 - 052	046080 -	.074083 -	.057063 1.65
. 036	026 - 026	061022	571057	042487 -	.068088 -	.060065 1 70
. 025	018 - 022	042003	. 365 059	044095 -	.076093 -	.065070 1.75
. 424	.015013	031004	.558063	045102 -	.089093 -	.072079 1.60
. 420		- 037020			086091 -	
. 018		437 032		045093 -		
	003 - 023			044091 -		.073076 1 95
. 025	005 - 015			019089 -		
. 024		- 072 - 034		034 091 -		
. 031	031 - 029			- 042 - 089 -		
.023		) - 054020   - 047003		- 047 - 087 -		
. 030		- 047 - 043 052 - 013		049099 - 045105 -		
.016		042 027		· .042106 -		
. 014	.035010			- 044 - 104 -		085 - 072 2 15
425		- 455 - 055	567049			
. 933		- 069 - 043		- 041 - 104 -		085 - 074 2 45
						· · · · · · - · •

Set 12, Table E — Deviations of Mean Local Pressurant Fractions, Scaling Runs 64-66

					Locatio	ns I							
i	2	3	4	5	6	7	8	9	10	11	12	13 +	
0.000	0.000	0.000			. 000		0.000				0 0 0 0		0
359	. 059	. 953	. 0 5 5		.807		- 567		315	. 133	. 127		5
712		1.914	126	. 1 26 - 1					- 622	273	262		0
- 682		1 881	. 197	. 089-1			-1.080			. 233	217		5
- 541		1.540	. 264	. 073-1			976	- 034		. 144	.126		0
398		1.200	. 332	.059 -			- 672		479	. 058	.037	253 2	
205	.031	653	. 285				350				022		0
108	.029	313				084	- 158				022	.025 3	-
077	.964	. 157	. 124			087	- 068		093		001		10
059 047	.087	106	053	- 069		- 077	- 061	037	- 066	014	.010	.011 .4	15
045	.068	059				- 057	014	.036	- 015	.033	.022		5
054	.024	. 030				- 041	- 002	.048	.003	.034	.036		0
059	.002	029				039	. 010	046	.017	. 046	. 037		5
	043					039	. 0 3 4	041	.017	.061	.042	.040 7	
				- 045 -			. 037	038	033	. 053	.050	044 7	-
024				- 047 -		- 039	. 040	.038	042	. 061	.060	035 8	-
026	- 048					- 037	. 041	043	038	.070	.059	038 6	
				- 057 -			. 053	. 938	054	.082	.064	037 9	
030				- 072 -			. 059	. 053	059	. 078	068		15
				- 097 -		.015	. 081	057	.072	091	076	.052 1.0	
017					024	0.000	. 051	022	033	045	041	.030 1.4	
. 603	040			- 032 -	006	006	054	018	021	036	031	.008 1 1	
. 029	042	042	042	.003 -	. 015	013	. 046	.008	.032	030	.015	013 1.1	5
010	036	036	036	036 -	.010	.003	. 057	. 023	. 0 2 6	034	.022	.006 1 2	0
010	038	- 012	- 068	- 068 -	. 041	- 001	. 057	943	. 055	040	. 032	.004 1.2	5
. 041	015	010	050	022 -	. 043	026	. 050	0.000	. 038	.025	010	~.001 1.3	0
. 036	- 001	027	- 054	~ .027	001	- 012	. 049	003	008	026	011	~.006 1.3	5
. 006		024		024		011	034	.016	.025	. 009		0.000 1.4	
. 005	023	025	048	048 -	. 019	021	. 064	003	.038	. 040	.013	.020 1.4	5
. 008	.032	023	- 092	023 -	. 064	013	059	027	029	.019	027	015 1 5	
. 043	.029		~ . 054	.012 -		047		004		~ 002	005	. 9 0 5 1 . 5	
. 038	.006		- 001	-		049		020		0 000	-	0.000 1 6	
. 020	013			013 -		029		007	022	.002	.016	.010 1.6	
. 010						- 012		007	.020	. 009	015	.024 1.7	
. 449			- 067			001	. 0 4 5	. 003	. 010	. 002	021	.020 1.7	
. 946	F10.	.013	023	013		- 022	.019	~ .019				008 1 6	
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0.000			0.000	0.000 0		0.000	0.000		0.000			0.000 2.0	2
4.400		0.000	0.000		. 000	0.000		0.000	0.000		000		0
6.000		0.000			. 000	0 000	0.000		0 000	8 900			3
0.000			0.000		. 000	0.000	0.000		0.000		000		0
0.000		0.000	0.000			0.000		0.000	0.000	0 000			5
		0.000	0.000		. 000	0.000		0.000	0.000		000		10
6 600		9.000	0 606		. 000	0.000		0.000	0.000		0 0 0 0		15
4.400				0.000 0		0.000			0.000			0.000 2.4	-
4.000	0.000	0.000	0 000	0 000 0		0 000		0.000			000	0.010 2 4	

## LIST OF SYMBOLS

$c_p$	Molar specific heat at constant pressure
$c_{\nu}$	Molar specific heat at constant volume
h <sub>s</sub>	Specific enthalpy of pressurant at $T_s$
i	Index referring to spatial points (subscript)
N	Number of moles
P	Absolute pressure
P <sub>0</sub> Q R	Initial absolute pressure
Q	Heat-removal rate
R	Universal gas constant
$\frac{T}{T}$	Absolute temperature
	Mean absolute temperature
$T_a$	Resident air temperature
$T_0$	Initial absolute temperature
$T_{p}$	Pressurant absolute temperature
Ü	Total internal energy of chamber contents
и	Local specific internal energy
$\bar{u}$	Mean specific internal energy
$\overline{u}_a$	Mean specific internal energy of resident air
$u_0$	Local specific internal energy at $T_0$
V	Chamber volume
X	Pressurant mole fraction
β	Dimensionless parameter characterizing molar heat-transfer coefficient
γ	Ratio of specific heats: $c_p/c_v$
$\boldsymbol{\theta}$	Characteristic time
$\theta_{c}$	$\theta$ evaluated at time just prior to $t = t_c$
ξ	Dimensionless pressurant deviation
au	Dimensionless time

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